

2023 Q1 convection

Monday, 22 May 2023

17:40

$$(a) \quad \underline{u} \cdot \nabla (\rho c_p T) = \nabla \cdot (\lambda \nabla T)$$

$$\underline{u} = u \underline{e}_x = u_c \left(1 - \left(\frac{y}{\delta}\right)^2\right) \underline{e}_x$$

$$\underline{u} \cdot \nabla = u_x \frac{\partial}{\partial x}$$

$$\nabla \cdot (\lambda \nabla T) = \lambda \left(\underbrace{\frac{\partial^2 T}{\partial x^2}}_{\text{neglect}} + \frac{\partial^2 T}{\partial y^2} \right)$$

$$\therefore \boxed{u_c \left(1 - \left(\frac{y}{\delta}\right)^2\right) \frac{\partial T}{\partial x} = \frac{\lambda}{\rho c_p} \frac{\partial^2 T}{\partial y^2}} \quad \text{QED}$$

$$(b) \quad \frac{\partial^2 T}{\partial y^2} = \frac{u_c}{\alpha} \left(1 - \left(\frac{y}{\delta}\right)^2\right) \frac{\partial T}{\partial x}$$

$$\frac{\partial T}{\partial y} = \frac{u_c}{\alpha} \frac{\partial T}{\partial x} \left(y - \frac{1}{\delta^2} \frac{y^3}{3} \right) + C_1(x)$$

$$\left. \frac{\partial T}{\partial y} \right|_{y=+\delta} = \frac{2}{3} \frac{u_c \delta}{\alpha} \frac{\partial T}{\partial x} + C_1(x)$$

$$\left. \frac{\partial T}{\partial y} \right|_{y=-\delta} = -\frac{2}{3} \frac{u_c \delta}{\alpha} \frac{\partial T}{\partial x} + C_1(x)$$

$$q_+ = -\lambda \left. \frac{\partial T}{\partial y} \right|_{y=+\delta} = -\lambda \left[\frac{2}{3} \frac{u_c \delta}{\alpha} \frac{\partial T}{\partial x} + C_1 \right]$$

$$q_- = -\lambda \left. \frac{\partial T}{\partial y} \right|_{y=-\delta} = -\lambda \left[-\frac{2}{3} \frac{u_c \delta}{\alpha} \frac{\partial T}{\partial x} + C_1 \right]$$

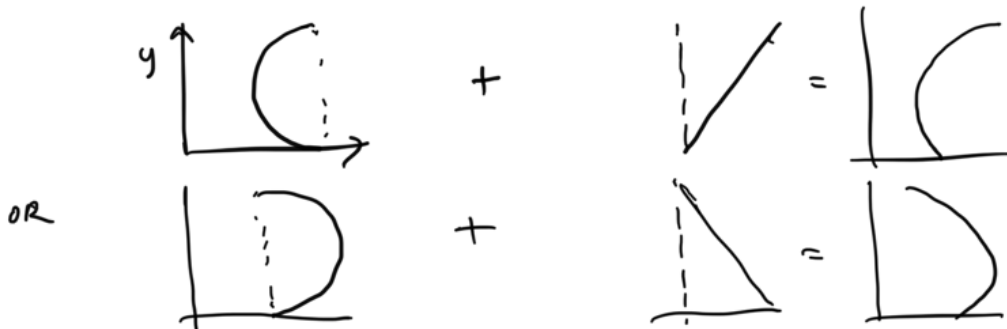
$$C_1 = - \frac{(q_+ + q_-)}{2\lambda}$$

$$\boxed{\frac{\partial T}{\partial y} = \frac{u_c}{\alpha} \frac{\partial T}{\partial x} y \left(1 - \frac{1}{3} \left(\frac{y}{\delta} \right)^2 \right) - \left(\frac{q_+ + q_-}{2\lambda} \right)}$$

$$(c) \quad T = \frac{u_c}{\alpha} \frac{\partial T}{\partial x} \left[\frac{y^2}{2} - \frac{1}{3} \frac{1}{\delta^2} \frac{y^4}{4} \right] - \left(\frac{q_+ + q_-}{2\lambda} \right) y + C_2(x)$$

$$T = \frac{u_c}{\alpha} \frac{\partial T}{\partial x} \frac{y^2}{2} \left[1 - \frac{1}{6} \left(\frac{y}{\delta} \right)^2 \right] - \left(\frac{q_+ + q_-}{2\lambda} \right) y + C_2(x)$$

SYMMETRIC ABOUT $y = 0$
LINEAR



$$T(\delta) = \frac{u_c}{\alpha} \frac{\partial T}{\partial x} \frac{\delta^2}{2} \frac{5}{6} - \left(\frac{q_+ + q_-}{2\lambda} \right) \delta + C_2(x)$$

$$T(-\delta) = \frac{u_c}{\alpha} \frac{\partial T}{\partial x} \frac{\delta^2}{2} \frac{5}{6} - \left(\frac{q_+ + q_-}{2\lambda} \right) (-\delta) + C_2(x)$$

$$\boxed{\Delta T = T(\delta) - T(-\delta) = - \left(\frac{q_+ + q_-}{\lambda} \right) \frac{\delta}{\lambda}}$$

(d) ONE CAN INTEGRATE THE EQUATIONS FOR u AND T TO OBTAIN THE MEAN, BUT A SIMPLER WAY TO SHOW HOW \bar{T} VARIES COMES FROM USING THE ORIGINAL 1D CONSERVATION EQUATION:

$$\frac{u \partial T}{\partial x} = \alpha \frac{\partial^2 T}{\partial y^2}$$

$$\int_{-\delta}^{+\delta} u \frac{\partial T}{\partial x} dy = \frac{d}{dx} \int_{-\delta}^{+\delta} u T dy = \int_{-\delta}^{+\delta} \alpha \frac{\partial^2 T}{\partial y^2} dy =$$

$$= \alpha \left[\frac{\partial T}{\partial y} \Big|_{-\delta} - \frac{\partial T}{\partial y} \Big|_{+\delta} \right]$$

$$\downarrow = \frac{\alpha}{\lambda} \left[-q_+ - (-q_-) \right] = -\frac{\alpha}{\lambda} [q_+ - q_-]$$

$$2\delta \bar{u} \frac{dT}{dx} = \frac{\alpha}{\lambda} (q_- - q_+) = \frac{\lambda}{\rho c_p} (q_- - q_+)$$

$$\dot{m} c_p \frac{dT}{dx} = q_- - q_+$$

So we show both that the mean temperature rise is constant, and equal to the net heat flux, as it should be.

Conduction in r via diffusion

2ai) $-\frac{1}{r} \frac{d}{dr} \left(r \frac{d\Theta}{dr} \right) = 0$ where $\Theta = \frac{T - T_\infty}{T_s - T_\infty}$

$\int d \left(r \frac{d\Theta}{dr} \right) = \int 0 dr \Rightarrow r \frac{d\Theta}{dr} = a$

$\int d\Theta = \int \frac{a}{r} dr \Rightarrow \Theta = a \ln r + b$

2aii)

Dimensional

B.C.1 $T(r=r_1) = T_s$

B.C.2 $-\lambda \frac{dT}{dr} \Big|_{r=r_2} = h(T(r_2) - T_\infty)$

B.C.2 $\frac{\lambda}{h} \frac{a}{r_2} = -a \ln r_2 - b$

B.C.1 $1 = a \ln r_1 + b$

$\frac{\lambda}{h} \frac{a}{r_2} + 1 = a \ln r_1 / r_2$

$1 = a \left(\ln r_1 / r_2 - \frac{\lambda}{h} \frac{1}{r_2} \right)$

$a = \left(\ln r_1 / r_2 - \frac{\lambda}{h r_2} \right)^{-1}$

Non-D

$\Theta(r_1) = 1 = a \ln r_1 + b$

$\frac{d\Theta}{dr} \Big|_{r=r_2} = \frac{a}{r_2} = -\frac{h}{\lambda} (a \ln r_2 + b)$

$b = 1 - \left(\ln r_1 / r_2 - \frac{\lambda}{h} \frac{1}{r_2} \right)^{-1} \ln r_1$
 $= \frac{\ln(r_1 / r_2) - \frac{\lambda}{h} \frac{1}{r_2} - \ln r_1}{\ln r_1 / r_2 - \frac{\lambda}{h} \frac{1}{r_2}}$

$b = -\frac{\lambda + h r_2 \ln r_2}{-\lambda + h r_2 \ln r_1 / r_2}$

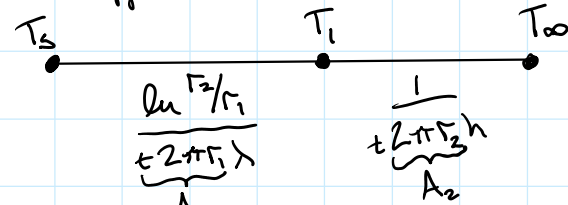
$Q_w = -\lambda \frac{\partial T}{\partial r} \Big|_{r=r_1} 2\pi r_1 t$

$= -\lambda (T_s - T_\infty) \frac{d\Theta}{dr} \Big|_{r=r_1} 2\pi r_1 t$

$= -\lambda (T_s - T_\infty) \left[\left(\ln r_1 / r_2 - \frac{\lambda}{h r_2} \right)^{-1} \right] 2\pi r_1 t$

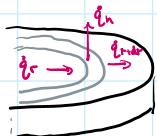
$Q = \frac{2\pi \lambda t (T_s - T_\infty)}{\frac{\lambda}{h r_2} + \ln(r_2 / r_1)}$

Alt. Approach



$Q = \frac{T_s - T_\infty}{\frac{\ln r_2 / r_1}{2\pi r_1 \lambda} + \frac{1}{2\pi r_2 h}}$

2bi) Conservation of Energy Cylinder



ODE for dimensional \dot{q}

$\dot{q}_r 2\pi r t - \left(\dot{q}_r + \frac{d\dot{q}_r}{dr} \delta r \right) 2\pi (r+\delta r) t - \dot{q}_c 2\pi r t \delta r = 0$

$-\dot{q}_r 2\pi r t \delta r - \frac{d\dot{q}_r}{dr} 2\pi r t \delta r - 2\dot{q}_c 2\pi r t \delta r = 0$

$\frac{dT}{dr} = (T_s - T_\infty) \frac{d\Theta}{dr} \quad \frac{d\dot{q}_r}{dr} = (T_s - T_\infty) \frac{d^2\Theta}{dr^2}$

$\frac{t\lambda}{r} \frac{d\Theta}{dr} (T_s - T_\infty) + t\lambda \frac{d^2\Theta}{dr^2} (T_s - T_\infty) - 2h\Theta (T_s - T_\infty) = 0$

$\Theta = \frac{T - T_\infty}{T_s - T_\infty}$

$\therefore T = (T_s - T_\infty)\Theta + T_\infty$

Collecting terms

$= \frac{1}{r} \frac{d}{dr} \left(r \frac{d\Theta}{dr} \right) - \frac{2h\Theta}{\lambda t} = 0$

$\frac{1}{r} \frac{d}{dr} \left(r \frac{d\Theta}{dr} \right) - \frac{\Theta}{\delta^2} = 0$

$\delta^2 = \frac{\lambda t}{2h}$

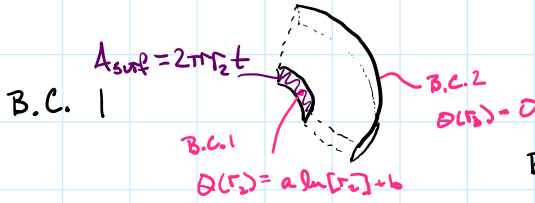
The non-dimensional temperature function in part b is not the same as in part a, as evidenced by the different function given in the problem. Thus, the non-dimension denominator can be defined in terms of T_2 rather than T_s .

the problem. Thus, the non-dimension denominator can be defined in terms of T_2 rather than T_s .

$$\frac{1}{r} \frac{d}{dr} \left(r \frac{d\theta}{dr} \right) - \frac{\theta}{\delta^2} = 0$$

$$\delta^2 = \frac{\lambda t}{2h}$$

2bii)



$$\theta = \frac{T - T_\infty}{T_2 - T_\infty}$$

$$T_2 = \theta(r_2) (T_{in} - T_\infty)$$

$$T_2 = (a \ln r_2 + b) (T_{in} - T_\infty)$$

$$\text{BC1 } \theta(r=r_2) = c e^{r_2/\delta} + d e^{-r_2/\delta} = \theta(r_2) = \theta_2$$

$$\text{BC2 } \theta(r=r_3) = c e^{r_3/\delta} + d e^{-r_3/\delta} = 0$$

$$\text{From BC2 } c = -d e^{-r_3/\delta} e^{-r_2/\delta} = -d e^{-2r_3/\delta}$$

$$\text{into BC1 } -d e^{-2r_3/\delta} e^{r_2/\delta} + d e^{-r_2/\delta} = \theta(r_2)$$

$$d = \theta(r_2) \left\{ e^{-r_2/\delta} - e^{(r_2-2r_3)/\delta} \right\}^{-1}$$

$$c = -\theta(r_2) \left\{ e^{-r_2/\delta} - e^{(r_2-2r_3)/\delta} \right\}^{-1} e^{-2r_3/\delta}$$

$$c = \theta(r_2) \left\{ e^{r_2/\delta} - e^{(2r_3-r_2)/\delta} \right\}^{-1}$$

2biii)

$$\eta = \frac{\dot{Q}_{fin}}{h A_{fin} (T(r_2) - T_\infty)}$$

$$\dot{Q}_{fin} = - \underbrace{2\pi r_2 t \lambda}_{A_{surf}} \left. \frac{dT}{dr} \right|_{r=r_2}$$

$$\theta = \frac{T - T_\infty}{T_2 - T_\infty}$$

$$\frac{d\theta}{dr} = (T_2 - T_\infty)^{-1} \frac{dT}{dr}$$

$$\therefore \frac{dT}{dr} = (T_2 - T_\infty) \frac{d\theta}{dr} = (T_2 - T_\infty) \left(\frac{c}{\delta} e^{r/\delta} - \frac{d}{\delta} e^{-r/\delta} \right)$$

$$\eta = - \frac{2 \cdot 2\pi r_2 t \lambda (T_2 - T_\infty) \left. \frac{d\theta}{dr} \right|_{r_2}}{2h (2\pi (r_3^2 - r_2^2)) (T_2 - T_\infty)} = \frac{-2\delta^2}{(r_3^2 - r_2^2)} r_2 \left. \frac{d\theta}{dr} \right|_{r_2}$$

fin top & bottom

$$\eta = \frac{-2\delta^2}{100\delta^2 - 25\delta^2} r_2 \left(\frac{c}{\delta} e^{r/\delta} - \frac{d}{\delta} e^{-r/\delta} \right) \Big|_{r_2=5\delta}$$

$$= -\frac{2 \cdot 5\delta}{75} \left(\frac{c}{\delta} e^5 - \frac{d}{\delta} e^{-5} \right) = -\frac{10}{75} \left(-\frac{e^{-15}}{e^5} e^5 - e^5 e^{-5} \right)$$

$$\eta = \frac{10}{75} = 13\%$$

3ai)

At steady state there is no \dot{Q}_{in} , Heat Flow is only out

All external view factors = 1

per unit length

$$R'_i = \frac{2(1-\epsilon)}{\epsilon A_i} + \frac{1}{A_i} = \left(\frac{1-\epsilon}{\epsilon \pi r_i} + \frac{1}{2\pi r_i} \right) = \frac{2(1-\epsilon) + \epsilon}{2\pi r_i \epsilon} = \frac{2-\epsilon}{2\pi r_i \epsilon} = R'_i$$

$$R'_{eq} = \frac{1-\epsilon}{\epsilon 2\pi r_2} + \frac{1-\epsilon}{2\pi r_2 \epsilon} + \sum_{i=3}^N \frac{2-\epsilon}{2\pi r_i \epsilon}$$

$$R'_{eq} = \frac{1}{\epsilon 2\pi r_2} + \frac{2-\epsilon}{2\pi \epsilon} \sum_{i=3}^N \frac{1}{r_i}$$

3aii)

$$R'_{N+2} = \frac{1}{\epsilon 2\pi r_2} + \frac{2-\epsilon}{2\pi \epsilon} \sum_{i=3}^{N+2} (2r_i)^{-1} = \frac{1}{\epsilon 2\pi r_2} + \frac{2-\epsilon}{2\pi \epsilon} \left(\frac{1}{2r_2} + \frac{1}{4r_2} + \frac{1}{8r_2} + \dots + \frac{1}{2^N r_2} \right)$$

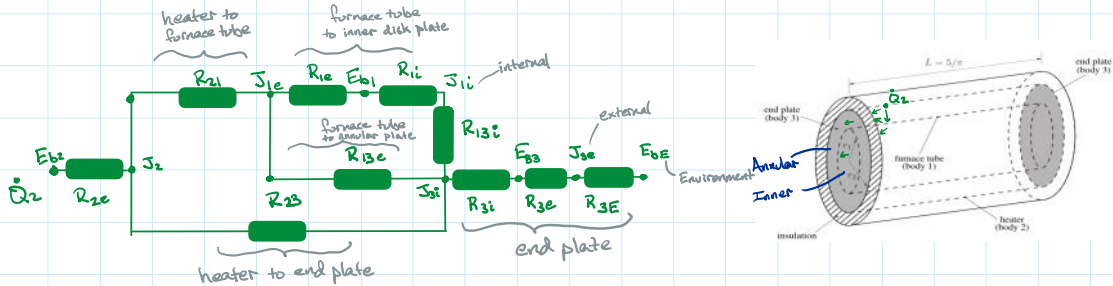
$$R'_{N+2} = \frac{1}{\epsilon 2\pi r_2} + \frac{2-\epsilon}{2\pi \epsilon} \left(\frac{1}{2} + \frac{1}{4} + \dots + \frac{1}{2^N} \right)$$

As $N \rightarrow \infty \left(\frac{1}{2} + \frac{1}{4} + \dots + \frac{1}{2^N} \right) \Rightarrow 1$

convergent series powers of 2

$$R'_{N \rightarrow \infty} = \frac{3-\epsilon}{2\pi \epsilon r_2}$$

3bi)



3bii)

$$R_{eq} = \frac{1-\epsilon_2}{\epsilon_2 A_2} + \left[R_{23}^{-1} + \left\{ R_{21} + \left(R_{13e}^{-1} + (R_{1e} + R_{1i} + R_{14i})^{-1} \right)^{-1} \right\}^{-1} \right] + R_{3i} + R_{3e} + R_{3\infty}$$

$$A_2 = 2\pi(1m)\left(\frac{5}{10}m\right) = 10m^2 \quad A_1 = 2\pi\left(\frac{1}{2}m\right)\left(\frac{5}{10}m\right) = 5m^2$$

$$R_{23} = \frac{1}{A_2 2\epsilon_{23}} = \frac{1}{10 \cdot 0.3} = \frac{1}{3} \quad [m^{-2}]$$

$$R_{21} = \frac{1}{A_2 F_{21}} = \frac{1}{A_1 F_{12}} = \frac{1}{5 \cdot 4/5} = \frac{1}{4}$$

$$R_{13e} = \frac{1}{A_1 F_{13}} = \frac{1}{5 \cdot 3/10} = 1$$

$$R_{13i} = \frac{1}{A_1 F_{13}} = \frac{1}{5 \cdot 3/10} = 2$$

$$R_{1e} = R_{1i} = \frac{1-\epsilon_1}{A_1 \epsilon_1} = \frac{1-1/2}{5 \cdot 1/2} = 1/5$$

$$R_{3i} = R_{3e} = \frac{1-\epsilon_3}{A_3 \epsilon_3} = \frac{1-3/10}{\pi(1/2)^2 \cdot 3/10} = \frac{8/10}{\pi/20} = \frac{16}{\pi}$$

$$R_{3\infty} = \frac{1}{A_3 \epsilon_3} = \frac{1}{\pi/4} = \frac{4}{\pi}$$

$$R_{eq} = \left[\frac{1-\epsilon_2}{\epsilon_2 A_2} + \left\{ R_{21} + \left(R_{13e}^{-1} + (R_{1e} + R_{1i} + R_{14i})^{-1} \right)^{-1} \right\}^{-1} \right] + R_{3i} + R_{3e} + R_{3\infty} = 11.7m^{-2}$$

$$\left[3 + \left\{ \frac{1}{4} + \left(1 + \left(\frac{1}{5} + \frac{1}{5} + 2 \right)^{-1} \right)^{-1} \right\}^{-1} \right] + \frac{16}{\pi} + \frac{16}{\pi} + \frac{4}{\pi}$$

$\frac{16}{\pi} \sim 5.1$, $\frac{16}{\pi} \sim 5.1$, $\frac{4}{\pi} \sim 1.27$

$3 + 5.1 + 5.1 + 1.27 \sim 14.47$

$$\dot{Q}_2 = \frac{\sigma(T_2^4 - T_E^4)}{R_{eq}} = \frac{5.67 \cdot 10^{-8} \frac{W}{m^2 K^4} (10^{0.4} - (3 \cdot 10^3)^4) K^4}{11.7 m^{-2}} = 4804 W \approx 4.8 kW = \dot{Q}_2$$

3biii)

Film with specular performance

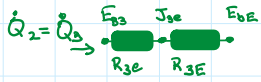
Wien's Law

$$\lambda^* T = C_3 \quad C = 2,897.8 \text{ } \mu\text{m K}$$

↑
Max of radiation

$$F(0 \rightarrow \lambda_{\text{max}}) = 0.25$$

Determine T_3 to find λ_3^*



$$\dot{Q}_3 = \frac{\sigma(T_3^4 - T_E^4)}{R_{B3E}}$$

$$R_{B3E} = R_{3e} + R_{3e} = \frac{16}{\pi} + \frac{4}{\pi} = \frac{20}{\pi}$$

$$T_3^4 = T_E^4 + \frac{\dot{Q}_3 R_{B3E}}{\sigma}$$

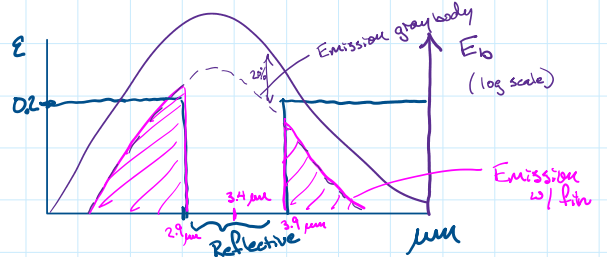
$$T_3^4 = 81 \cdot 10^8 + \frac{4.8 \cdot 10^3 \cdot \frac{20}{\pi}}{5.67 \cdot 10^{-8}} \text{ K}^4$$

can neglect

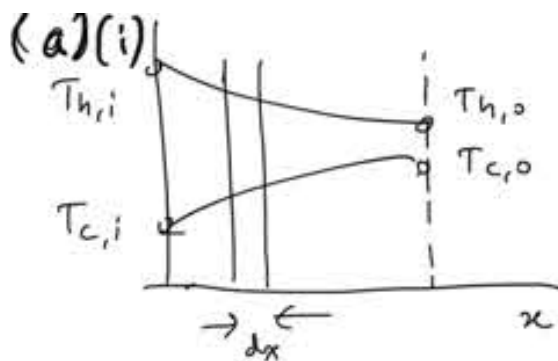
$5 \cdot 10^{11} \text{ K}^4$

$$T_3 = 860 \text{ K}$$

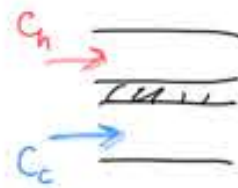
$$\lambda_{\text{max}, T_3} = \frac{C_3}{T_3} = \frac{2898 \text{ K } \mu\text{m}}{860 \text{ K}} = 3.4 \text{ } \mu\text{m} = \lambda_{\text{mid}}$$



2023 Q4 HX



co-flow HX



$$\delta \dot{Q} = U dA (T_h - T_c) = -\overbrace{\dot{m}_h c_h}^{C_h} dT_h = \overbrace{\dot{m}_c c_c}^{C_c} dT_c$$

$$d(T_h - T_c) = -\frac{\delta \dot{Q}}{C_h} = \frac{\delta \dot{Q}}{C_c} = -\delta \dot{Q} \left(\frac{1}{C_c} + \frac{1}{C_h} \right)$$

$$= -U (T_h - T_c) dA \left(\frac{1}{C_c} + \frac{1}{C_h} \right)$$

$$d \ln (T_h - T_c) = -UA \left(\frac{1}{C_c} + \frac{1}{C_h} \right)$$

$$\ln \frac{(T_h - T_c)_o}{(T_h - T_c)_i} = -UA \left(\frac{1}{C_h} + \frac{1}{C_c} \right) \frac{1}{C_{||}}$$

$$\boxed{\frac{\Delta T_o}{\Delta T_i} = \exp \left(-\frac{UA}{C_{||}} \right)}$$

QED

(a)(ii)

$$\begin{aligned}
\dot{Q} &= \int_0^A u (T_h - T_c) dA = \\
&= \int_0^A u \Delta T_i \exp\left(-\frac{uA}{c_{11}}\right) dA = \\
&= -c_{11} \Delta T_i \exp\left(-\frac{uA}{c_{11}}\right) \Big|_0^A \\
&= -c_{11} \Delta T_i \left[\exp\left(-\frac{uA}{c_{11}}\right) - 1 \right] \left\{ A(0) = 0 \right\} \\
\dot{Q}_{11} &= c_{11} \Delta T_i \left[1 - \exp\left(-\frac{uA}{c_{11}}\right) \right]
\end{aligned}$$

$$\boxed{\frac{\dot{Q}}{uA \Delta T_i} = \frac{c_{11}}{uA} \left[1 - \exp\left(-\frac{uA}{c_{11}}\right) \right]} \quad \text{QED}$$

ALTERNATIVELY:

$$\begin{aligned}
(T_h - T_c)_0 &= \overbrace{(T_{h,0} - T_{h,i})}^{-\dot{Q}/c_{11}} + \overbrace{(T_{h,i} - T_{c,i})}^{\Delta T_i} + \overbrace{(T_{c,i} - T_{c,0})}^{-\dot{Q}/c_c} \\
&= \Delta T_i \exp\left(-\frac{uA}{c_{11}}\right)
\end{aligned}$$

$$\therefore -\frac{\dot{Q}_{11}}{c_{11}} = -\Delta T_i + \Delta T_i \exp\left(-\frac{uA}{c_{11}}\right)$$

$$\dot{Q}_{11} = c_{11} \Delta T_i \left(1 - \exp\left(-\frac{uA}{c_{11}}\right) \right) \quad \dots \text{etc.}$$

(b) COUNTERFLOW HX





NOTE THE SIGN \neq

$$(i) \delta \dot{Q} = -C_h dT_h = -C_c dT_c$$

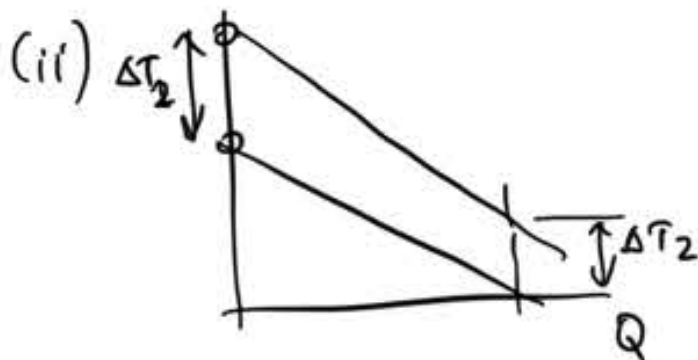
$$d(T_h - T_c) = -\delta \dot{Q} \left(\frac{1}{C_h} - \frac{1}{C_c} \right) = -\frac{U}{C_x} (T_h - T_c) dA$$

where $C_x^{-1} = C_h^{-1} - C_c^{-1}$

$$d \ln(T_h - T_c) = -UA / C_x$$

$$\ln \frac{(T_h - T_c)_2}{(T_h - T_c)_1} = -UA / C_x$$

$$\Delta T_2 = \Delta T_1 \exp(-UA / C_x) \quad \text{QED}$$



$$d\Delta T = -\frac{\delta Q}{C_x}$$

$$(T_h - T_c)_2 = (T_{h,o} - T_{c,i}) = (T_{h,o} - T_{h,i}) + (T_{h,i} - T_{c,i})$$

$$= -\frac{\dot{Q}_x}{C_h} + \Delta T_i$$

$$(T_h - T_c)_1 = (T_{h,i} - T_{c,o}) = (T_{h,i} - T_{c,i}) + (T_{c,i} - T_{c,o})$$

$$= \Delta T_i - \frac{\dot{Q}_x}{C_c}$$

$$\Delta T_i - \frac{\dot{Q}_x}{C_h} = \left(\Delta T_i - \frac{\dot{Q}_x}{C_c} \right) \exp\left(-\frac{UA}{C_x}\right)$$

$$\dot{Q}_x \left[\frac{1}{C_h} - \frac{1}{C_c} \exp\left(-\frac{UA}{C_x}\right) \right] = \Delta T_i \left(1 - \exp\left(-\frac{UA}{C_x}\right) \right)$$

$$\frac{\dot{Q}_x}{UA \Delta T_i} = \left(\frac{C_x}{UA} \right) \left[\frac{1 - \exp\left(-\frac{UA}{C_x}\right)}{\frac{C_x}{C_h} - \frac{C_x}{C_c} \exp\left(-\frac{UA}{C_x}\right)} \right]$$

Q. 11

(c) For $C_h \ll C_c$: $C_{11} = C_h$; $C_x = C_h$

$$\frac{1}{C_{11}} = \frac{1}{C_c} + \frac{1}{C_h} \quad \frac{1}{C_x} = \frac{1}{C_h} - \frac{1}{C_c}$$

$$\dot{Q}_{11} = C_h \Delta T_i \left(1 - \exp\left(-\frac{UA}{C_h}\right) \right)$$

$$\dot{Q}_x = C_h \Delta T_i \left(1 - \exp\left(-\frac{UA}{C_h}\right) \right)$$

$$\hat{Q}_{11} \approx \hat{Q}_x$$

