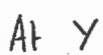


1.

$$K_p = \frac{1 + \sin 23}{1 - \sin 23} = \underline{\underline{2.28}}$$

$$\sigma_{H_0} = 102 \text{ kPa.}$$

$$\sigma'_{H_0} = 72 \text{ kPa}$$



$$\sigma_v' + \sigma_H' = 132 \text{ kPa}$$

$$\sigma_H' = 40.2 \text{ kPa} \quad \sigma_V' = 91.7 \text{ kPa}$$

$$\frac{(91.7 + u) - 90}{5} = (40.2 + u) - 102$$

$$U = \underline{77.7 \text{ kPa}}$$

$$H = \underline{\underline{4.97\text{m}}}$$

$$\sigma_v = \underline{169.5 \text{ kPa}}$$

$$b) \quad \sigma_v = 169.5 + 79.5 = 249 \text{ kPa}$$

$$\sigma_H = \cancel{60} + 0.2 \times \cancel{159} = \cancel{91.8} \text{ kPa}$$

$$\frac{249 - u}{133 \cancel{91.8} - u} = 2.28$$

$$c) \quad 2c_u \geq \cancel{157.2} \text{ kPa}$$

$$c_u > \underline{\underline{\cancel{78.6} \text{ kPa}}}$$

$$249 - u = \frac{305.1}{\cancel{209.3}} - 2.28 u$$

$$1.28 u = \cancel{-39.7} \text{ 56}$$

$$u = \underline{\underline{\cancel{-31} \text{ kPa}}}$$

c) Plot height vs pore pressure. Kink in graph seen
d) at yield.

d) Half of excess p.p dissipated
e) $u_{ex} = \cancel{77.7} - 30 = \cancel{47.7} \text{ kPa}$

$$u_e \quad u \text{ @ restart} = \frac{30}{\cancel{77.7}} + \frac{6.9}{\cancel{23.85}}$$

$$= \cancel{53.85} \text{ kPa } 36.9$$

$$\sigma_v' = \frac{169.5 - 36.9}{\cancel{91.7} - \cancel{23.85}} = \frac{132.6}{\cancel{115.5}} \text{ kPa}$$

$$\sigma_H' = \frac{117.9 - 36.9}{\cancel{40.2} + \cancel{23.85}} = \frac{81}{\cancel{64}} \text{ kPa}$$

$$\sigma_v' + \sigma_H' = \frac{213.6}{\cancel{179.5}} \text{ kPa}$$

$$\sigma_v' = 2.28 \sigma_H'$$

$$3.28 \sigma_H' = \frac{213.6}{\cancel{179.5}}$$

$$\sigma_H' = \frac{65.1}{\cancel{54.72}} \text{ kPa}$$

$$\sigma_v' = \frac{148.5}{\cancel{124.8}} \text{ kPa}$$

$$\frac{148.5 + u - 169.5}{5} = \frac{65.1 + u - 117.9}{5}$$

$$4u = 199.3 - 31.8$$

$$u = \frac{49.8}{4} \text{ kPa} = 12.45 \text{ kPa}$$

$$\sigma_v = 174.6 \text{ kPa}$$

$$H = 5.3 \text{ m}$$

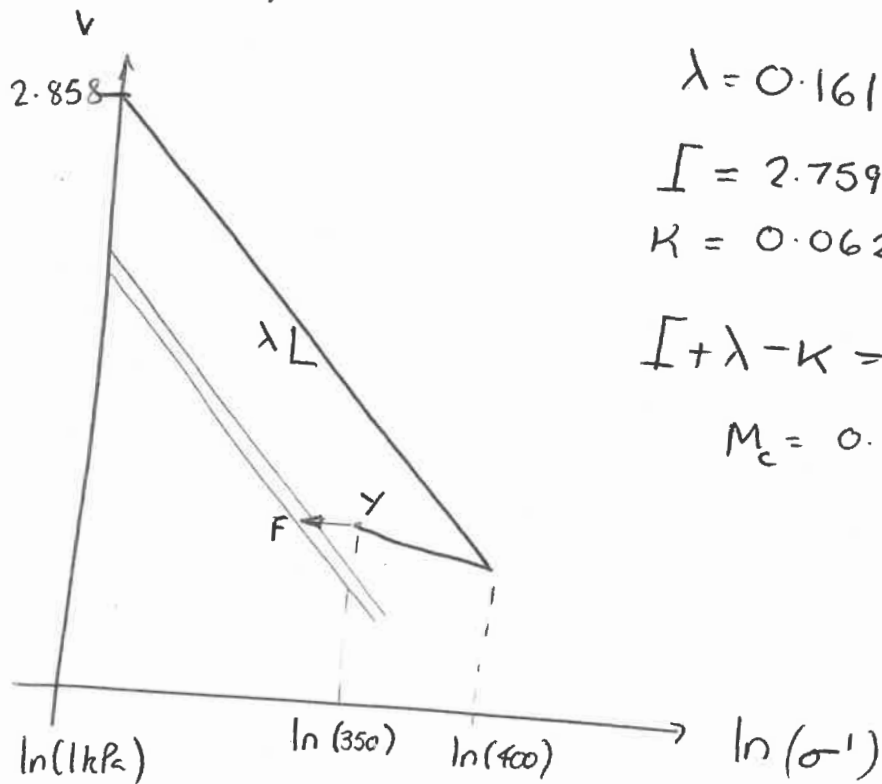
$$2C_u = 70.1$$

$$C_u = 35.05 \text{ kPa}$$

3D2.

Q2)

a)



$$\lambda = 0.161$$

$$\Gamma = 2.759$$

$$K = 0.062$$

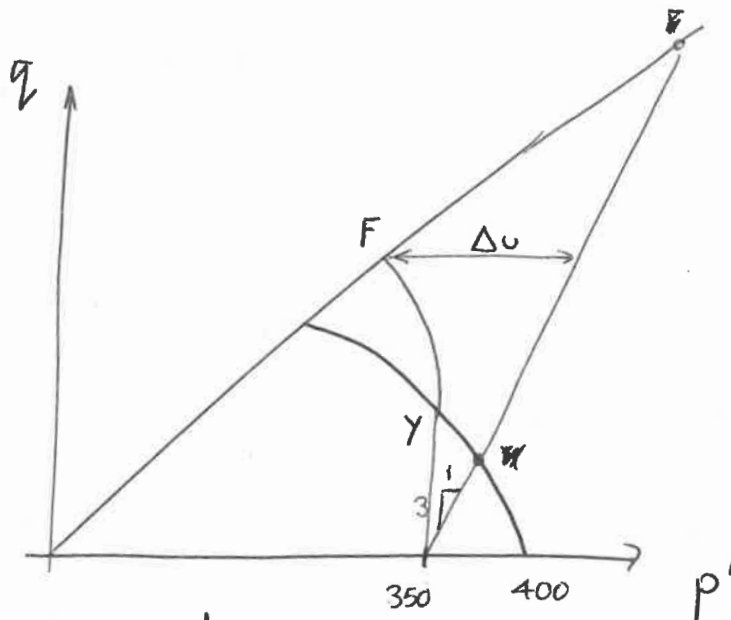
$$\Gamma + \lambda - K = 2.858$$

$$M_c = 0.89$$

$$V_{400} = 2.858 - 0.161 \ln(400) = 1.893$$

$$V_{350} = V_{400} + 0.062 \ln\left(\frac{400}{350}\right) = \underline{\underline{1.902}}$$

b)



At yield $\frac{q}{p'} = M \ln \frac{p'_c}{p'}$

$$q_y = 0.89 \times 350 \times \ln\left(\frac{400}{350}\right) = \underline{\underline{41.6 \text{ kPa}}}$$

$$u_{ex} = \frac{41.6}{3} = \underline{\underline{13.87 \text{ kPa}}}$$

$$p' = 350$$

$$p'_c = 400$$

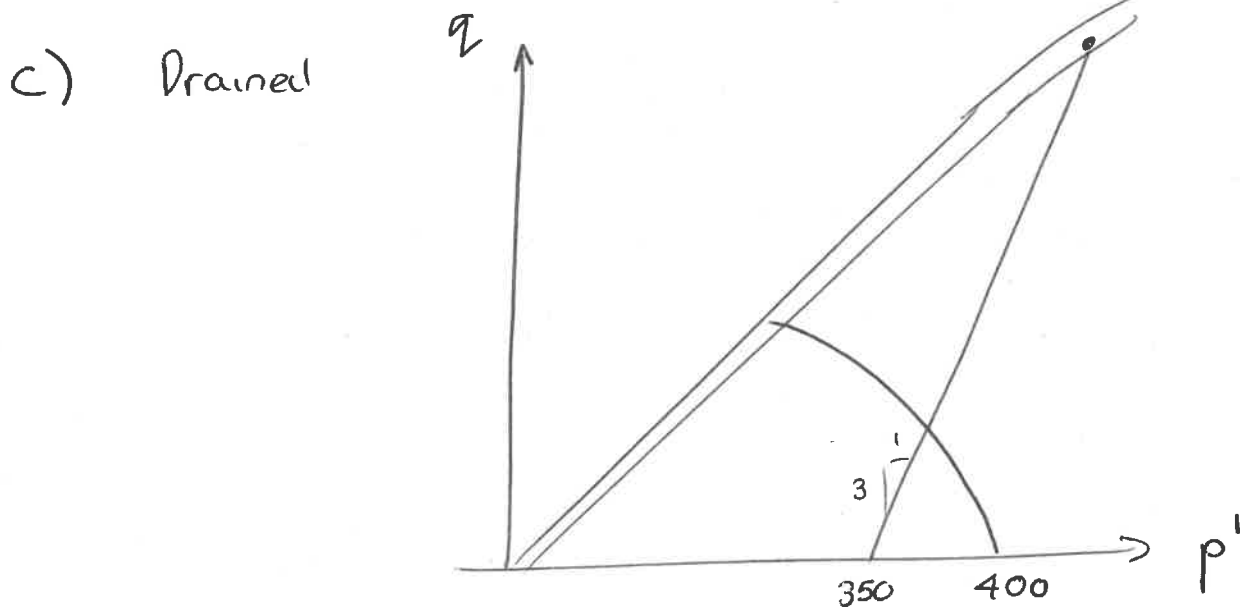
q_f

$$1.902 = 2.759 - 0.161 \ln p'$$

$$p' = 205 \text{ kPa}$$

$$q = Mp' = \underline{\underline{182.4 \text{ kPa}}}$$

$$u_{ex} = 350 + \frac{182.4}{3} - 205 = \underline{\underline{206 \text{ kPa}}}$$



$$q = Mp' \ln \left(\frac{p'_c}{p'} \right) = 3(p' - 350)$$

Guess $p' = 380$

~~RHS~~ LHS = 17.35

LHS = 36.9

LHS = 32.16

LHS = 32.96

RHS $\rightarrow p' = 356$

RHS $p' = 362$

RHS $p' = 361$

RHS $p' = 361$

$p' = 361 \text{ kPa}$ $q = \underline{\underline{33 \text{ kPa}}}$

On same $K \rightarrow \Delta v = K \ln \left(\frac{361}{350} \right) = 0.0019$

$e_v = \underline{\underline{0.1\%}}$

contraction

At failure on CSL

$$q = M p' = 3(p' - 350)$$

$$(M-3)p' + (3-M)p' = 1050$$

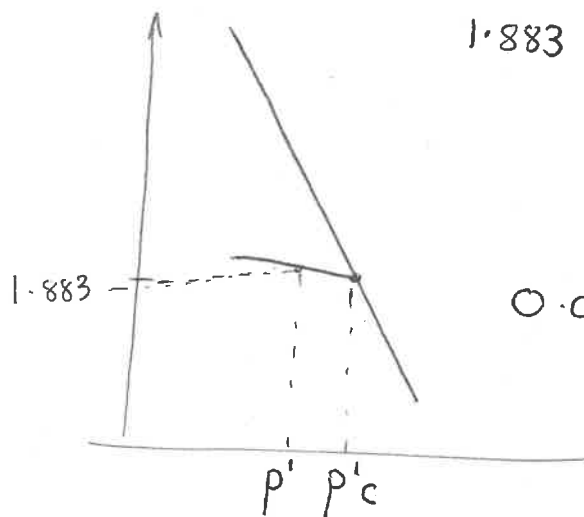
$$p' = \underline{497.6 \text{ kPa}}$$

$$q = \underline{442.9 \text{ kPa}}$$

$$V = 2.759 - 0.161 \ln(497.6) = 1.759$$

$$e_v = \frac{\Delta v}{v} = \frac{0.143}{1.902} = \underline{\underline{7.5\%}}$$

d) If $e_v = 1\%$ $v = 0.99 \times 1.902 = 1.883$



$$1.883 = \Gamma + \lambda - K - \lambda \ln p'_c + K \ln \frac{p'_c}{p'}$$

$$= 2.858 - 0.161 \ln p'_c + 0.062 \ln \frac{p'_c}{p'}$$

$$0.062 \ln p'_c - 0.062 \ln p' - 0.161 \ln p'_c = -0.975$$

$$0.099 \ln p'_c + 0.062 \ln p' = 0.975$$

Yield surface $q = M p' \ln \frac{p'_c}{p'}$

Load path $q = 3(p' - 350)$

$$3p' - 1050 = 0.89 p' \ln \left(\frac{p'_c}{p'} \right)$$

$$0.099 \ln(p'_c) + 0.062 \ln p' = 0.975$$

$$\ln(p'_c) = 9.848 - 0.626 \ln(p')$$

$$3p' - 1050 = 0.89 p' \ln(p'_c) - 0.89 p' \ln(p')$$

$$3p' - 1050 = 8.765 p' - 0.557 p' \ln p' - 0.89 p' \ln p'$$

$$5.765 p' + 1050 = 1.447 p' \ln p'$$

~~Try LHS~~ $p' = 400$ ~~-~~ ~~LHS~~ $p' = 419.4$
~~LHS = 453.6~~
~~LHS = 514.3~~
~~LHS = 623.7~~

Try values to approximate solution.

$$p' = \underline{\underline{374 \text{ kPa}}}$$

$$\Rightarrow q = 72 \text{ kPa}$$

$$p'_c = 464 \text{ kPa}$$

~~Try~~ ~~RHS~~ $p' = 375$

3D2

Problem 3

Part (a)

1. Sliding along base
2. Overturning about toe
3. Exceeding bearing capacity (sinking)
4. Sliding along blocks (above base)
5. Overturning within blocks (above toe)

Part (b)

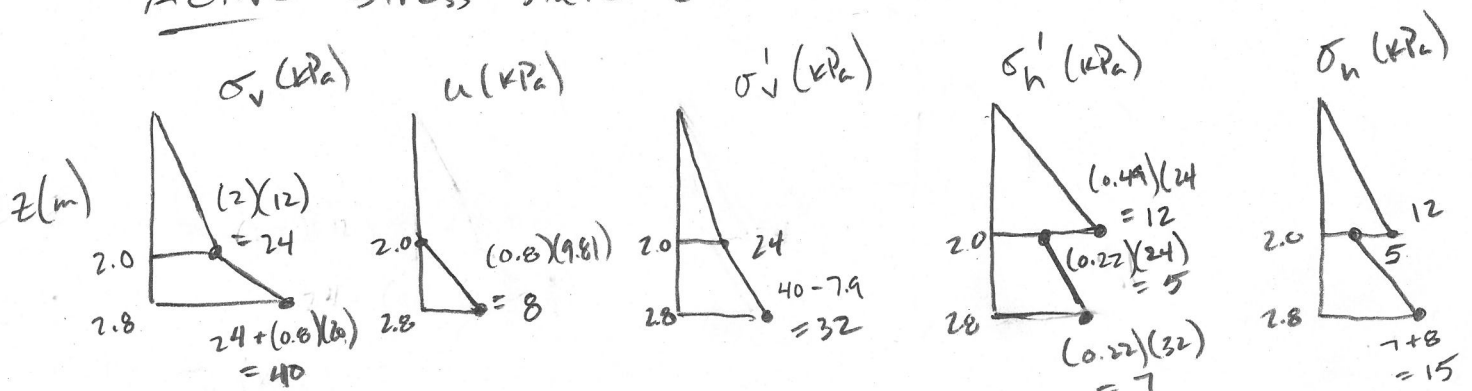
$$K_a = \frac{1 - \sin \phi'}{1 + \sin \phi'} \quad , \quad K_p = \frac{1}{K_a}$$

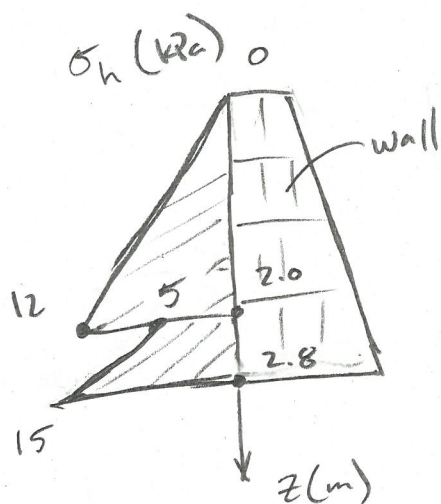
clay : $K_a = \frac{1 - \sin 20^\circ}{1 + \sin 20^\circ} = 0.490$

$$K_p = \frac{1}{0.490} = 2.04$$

silty sand : $K_a = 0.22$, $K_p = 4.60$

Active stress state behind wall :

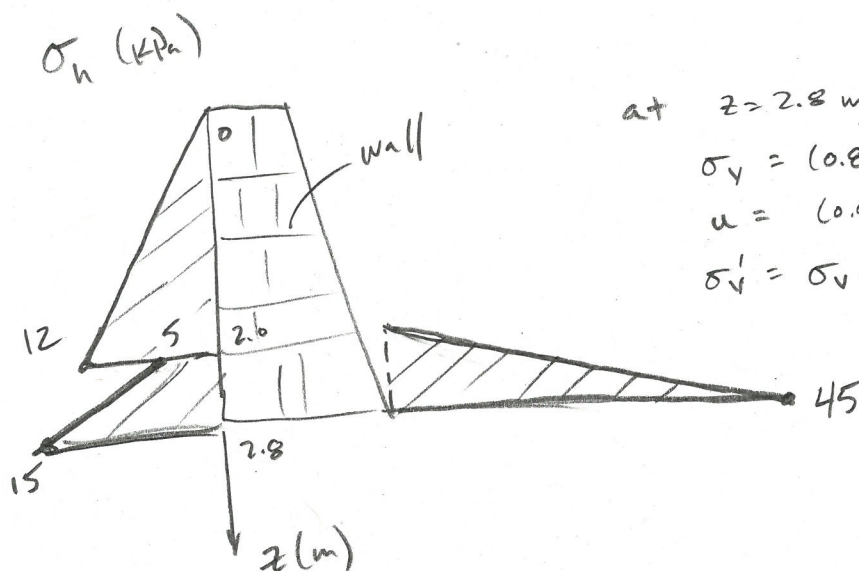




Part (c)

Neglect influence of wall inclination

Assume failure along base - not given
friction angle of blocks



at $z = 2.8 \text{ m}$ on front:

$$\sigma_v = (0.8)(20) = 16$$

$$u = (0.8)(10) = 8$$

$$\sigma'_v = \sigma_v - u = 8, \quad \sigma'_h = k_p \sigma'_v = (4.6)(8) = 37.5$$

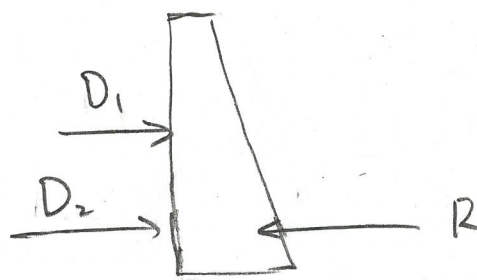
$$\sigma_h = \sigma'_h + u = 37.5 + 8 = 45$$

$$SF = \frac{F_{\text{resisting}}}{F_{\text{driving}}}$$

$$= \frac{R}{D_1 + D_2}$$

$$= \frac{\frac{1}{2}(0.8 \text{ m})(45.3 \text{ kPa})}{\frac{1}{2}(2.0 \text{ m})(11.8 \text{ kPa}) + \frac{1}{2}(0.8 \text{ m})(5.22 \text{ kPa} + 14.8 \text{ kPa})} = 0.91$$

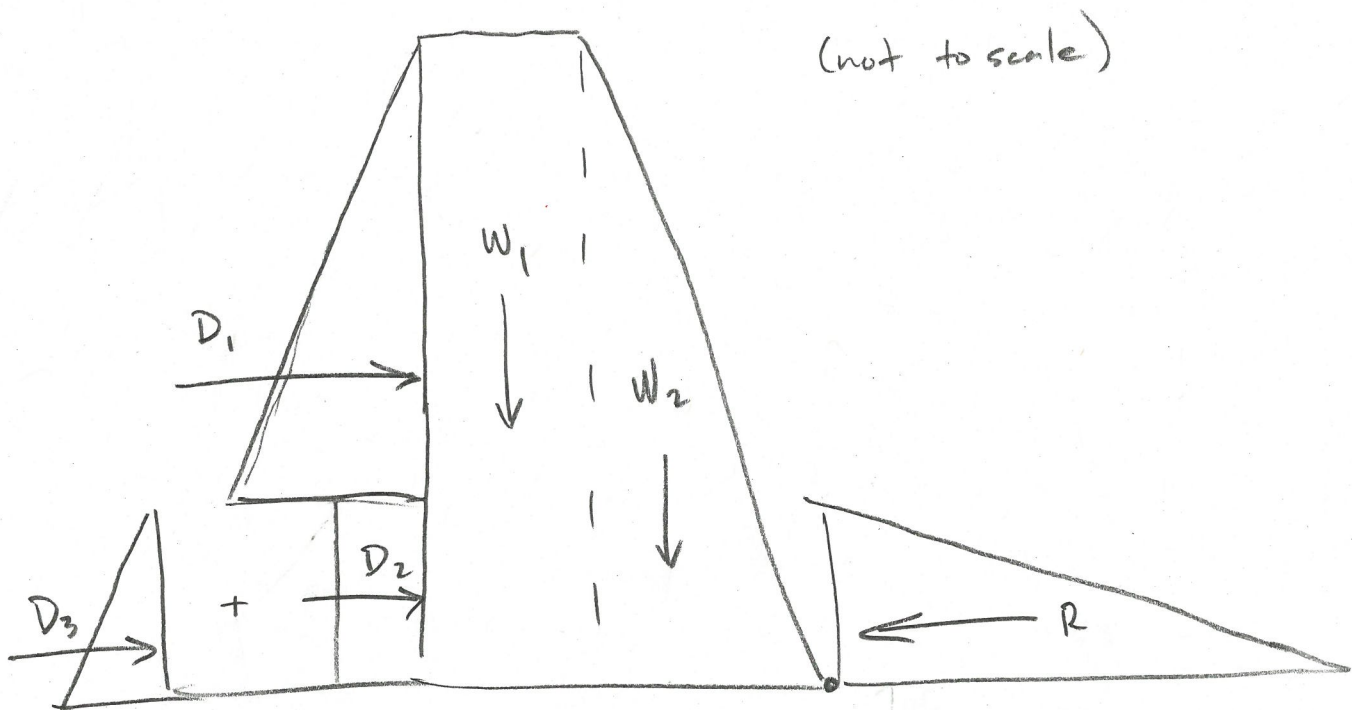
$$= 0.92$$



SF < 1 $\rightarrow$ FAIL

Part (d)

1. Assume rotation about toe
2. Ignore inclination again to evaluate pressure (passive) on front
3. Assume wall drains freely
4. Neglect buoyancy of submerged part of wall (small volume)



TOE

	moment arm (m)	force (kN)	moment (kN.m)
W_1	0.4	$(18)(0.4) = 7.2$ 20.1	29 8.1
W_2	$(2/3)(0.2) = 0.133$	$\frac{1}{2}(18)(0.2) = 1.8$ 5.0	0.2 0.67
D_1	$0.8 + \frac{1}{2}(2) = 1.47$	$\frac{1}{2}(2)(11.8) = 11.8$	-17
D_2	$\frac{1}{2}(0.8) = 0.4$	$(6.8)(5.22) = 4.2$	-1.7
D_3	$\frac{1}{3}(0.8) = 0.27$	$\frac{1}{2}(0.8)(15-5) = 3.9$	-1.0
R	$\frac{1}{3}(0.8) = 0.27$	$\frac{1}{2}(0.8)(45) = 18$	4.8

$$M_{\text{resist}} = \cancel{2.9}^{8.1} + \cancel{0.2}^{0.67} + 4.8 = \cancel{8}^{13.6} \text{ kN}\cdot\text{m}$$

$$M_{\text{driving}} = 17 + 1.7 + 1 = 20 \text{ kN}\cdot\text{m}$$

$$SF = \frac{M_{\text{resist}}}{M_{\text{driving}}} = \frac{\cancel{8}^{13.6} \text{ kN}\cdot\text{m}}{20 \text{ kN}\cdot\text{m}} = \cancel{0.4}^{0.68}$$

$$SF = \cancel{0.4}^{0.68} < 1 \Rightarrow \text{FAIL}$$

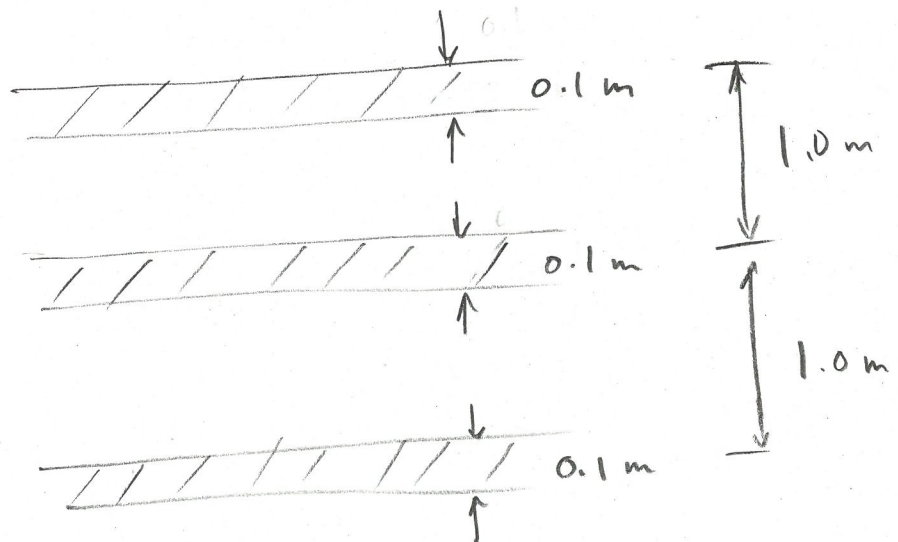
Part (e)

Overturning critical ; need $SF = 1$

$$\Rightarrow SF = 1 = \frac{\cancel{8}^{13.6} \text{ kN}\cdot\text{m} + (1.8 \text{ m}) F_{\text{anchor}}}{(20 \text{ kN}\cdot\text{m})}$$

$$F_{\text{anchor}} = \frac{20 - \cancel{8}^{13.6}}{1.8} = \cancel{6.7}^{3.5} \text{ kN/m}$$

From above :



$$F_{\text{anchor}}^* = F_{\text{anchor}} (1 \text{ m}) \dots \text{total force along } 1 \text{ m width}$$

$$F_{\text{anchor}}^* = 2 \tau_f b L^*$$



$$\tau_f = \sigma_v \tan \delta \dots \text{shear stress at failure}$$

$$b = 0.1 \text{ m} \dots \text{strip width}$$

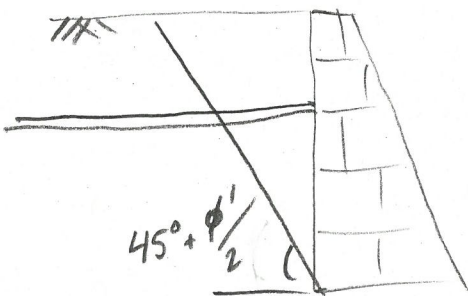
$$L^* \dots \text{required length}$$

$$\tau_f = \underbrace{(12 \text{ kN/m}^3)(1 \text{ m})}_{\sigma_v} \tan 20^\circ = 4.4 \text{ kPa}$$

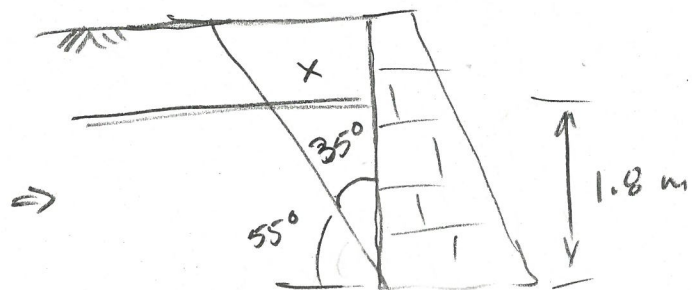
$$L^* = \frac{F_{\text{anchor}} (1 \text{ m})}{2 \tau_f b} = \frac{(\overset{3.5}{\cancel{6.7}} \text{ kN/m})(1 \text{ m})}{2 (4.4 \text{ kN/m}^2)(0.1 \text{ m})}$$

$$= \overset{4.1}{\cancel{7.6}} \text{ m} //$$

Need to consider active zone :



assume $\phi' = 20^\circ$

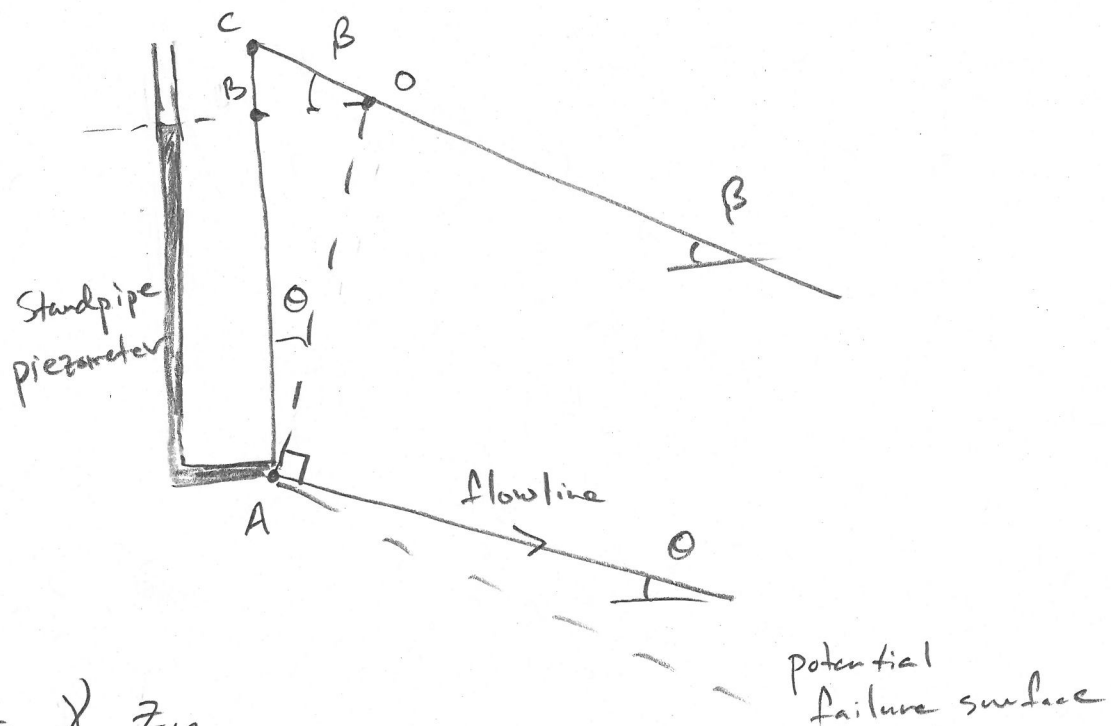


$$x = (1.8 \text{ m}) \tan 35^\circ$$

$$= 1.3 \text{ m}$$

$$\Rightarrow L = L^* + x = \overset{5.3}{\cancel{9}} \text{ m} //$$

3D2

Problem 4Part (a)

$$u_A = \gamma_w z_{AB}$$

z_{AB} ... height (head) measured from A to B

From triangle OAB : $\overline{OB} = \overline{AB} \tan \theta$

From triangle OBC : $\overline{BC} = \overline{OB} \tan \beta$

$$\overline{BC} = \overline{AB} \tan \theta \tan \beta$$

$AB + BC = z$... depth to potential failure surface

$$z - \overline{AB} = \overline{AB} \tan \theta \tan \beta$$

Solve: $\overline{AB} = \frac{z}{1 + \tan \theta \tan \beta}$

$$\overline{AB} = z_{AB} = \frac{u_A}{\gamma_w} \Rightarrow u = \frac{\gamma_w z}{1 + \tan \theta \tan \beta}$$

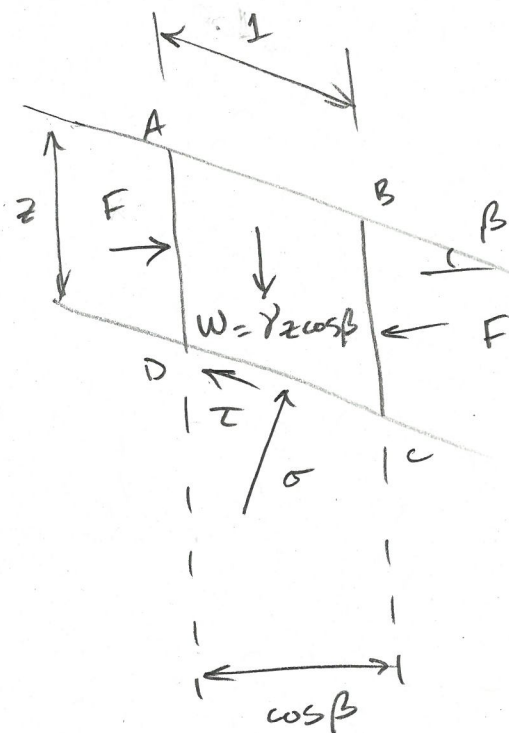
Drop "A" & "AB"
Since points could be anywhere

$$= \frac{\gamma_w z \cos \theta \cos \beta}{\cos \theta \cos \beta + \sin \theta \sin \beta}$$

$$= \frac{\gamma_w z \cos \theta \cos \beta}{\cos(\theta - \beta)}$$

$$= \frac{\gamma_w z \cos \theta \cos \beta}{\cos(\beta - \theta)}$$

Part (b)



$$\tau = W \sin \beta = \gamma_w z \cos \beta \sin \beta$$

$$\sigma = W \cos \beta = \gamma_w z \cos^2 \beta$$

$$\sigma' = \sigma - u$$

$$\frac{\tau}{\sigma'} = \tan \phi' = \frac{\gamma_w z \cos \beta \sin \beta}{\gamma_w z \cos^2 \beta - u} = \left(1 - \frac{u}{\gamma_w z \cos^2 \beta} \right) \quad (\#)$$

Substitute using result from (a)

$$\left\{ \begin{aligned} \frac{u}{\gamma z \cos^2 \beta} &= \frac{\gamma_w}{\gamma} \frac{\sec^2 \beta}{1 + \tan \theta \tan \beta} \\ \sec^2 \beta &= 1 + \tan^2 \beta \end{aligned} \right.$$

$$\rightarrow \frac{u}{\gamma z \cos^2 \beta} = \frac{\gamma_w}{\gamma} \frac{1 + \tan^2 \beta}{1 + \tan \theta \tan \beta}$$

Substitute into (#) :

$$\tan \phi' = \left[1 - \frac{\tan \beta}{\frac{\gamma_w}{\gamma} \frac{(1 + \tan^2 \beta)}{(1 + \tan \theta \tan \beta)}} \right] //$$

Part (c)

$$\theta = 90^\circ : \quad \tan \theta \rightarrow \infty \Rightarrow \tan \phi' = \tan \beta$$

$$\theta = 0 : \quad \tan \phi' = \frac{\tan \beta}{\left[1 - \frac{\gamma_w}{\gamma} (1 + \tan^2 \beta) \right]}$$

$\theta = 90^\circ$ is case of freely draining slope, for which $\beta = \phi'$ at failure

$\theta = 0$ is the case of horizontal flow, which may occur when downward flow is impeded.

$$\tan \phi' = \left[\frac{1}{1 - \frac{\gamma_w}{\gamma} (1 + \tan^2 \beta)} \right] \tan \beta$$

always greater than 1

$\Rightarrow$ slope destabilised compared with $\theta = 90^\circ$

Part (d)

Assume $\theta = 0$ since the lower boundary is impermeable (flow roughly horizontal).

This will give safer estimate.

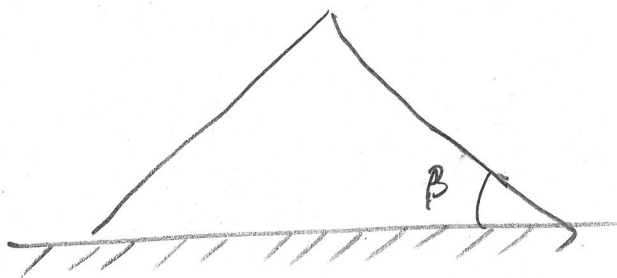
$$\tan 35^\circ = \frac{\tan \beta}{1 - \frac{9.81}{18} (1 + \tan^2 \beta)}$$

Solve : $\beta = 16^\circ$

Flow is in fact complex, and locally θ could take on a range of values $\rightarrow$ which should be checked.

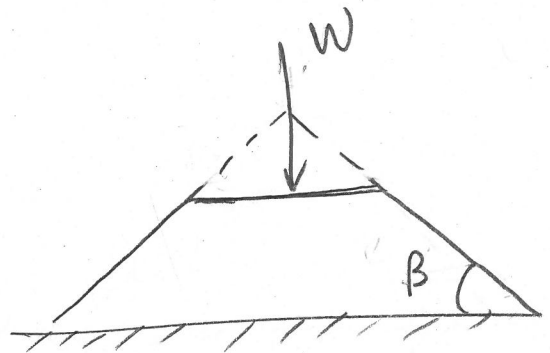
To be more rigorous, need to compute distribution of pore pressures (e.g., using flow net) and consider finite slope failure (e.g., using limit equilibrium or FE solver).

Part (e)

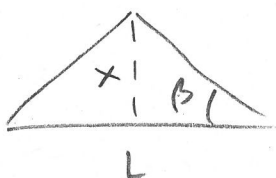


Stable

$\Rightarrow$



also stable



$$x = \frac{L}{2} \tan \beta$$

$$\begin{aligned} \Rightarrow W &= \frac{1}{2} L \left(\frac{L}{2} \tan \beta \right) \gamma \\ &= \frac{1}{4} \gamma L^2 \tan \beta \end{aligned}$$

Some distribution ^{of surcharge} $\checkmark$ that produces

$W = \frac{1}{4} \gamma L^2 \tan \beta$ will be stable, but

a uniform distribution is not necessarily stable.

Hence, $q = \frac{W}{L} = \frac{1}{4} \gamma L \tan \beta$ will

provide a dubious (potentially unsafe) estimate of the maximum surcharge that can be applied.

A safe estimate of q could be assessed using limit equilibrium, limit theorems, or finite element calculations,