

1 a) Particle size distribution curve is a plot with the particle sizes on the abscissa and percentage finer (or % passing) on the ordinate. The percentage passing is obtained for larger sized particles like gravel, sand ~~and~~ by taking a known weight of soil and sieving them through standard sieves. The weight of the particles left on each sieve are ~~weighed~~ carefully obtained to calculate the percentage ~~pass~~ of particles passing each sized sieve. For finer particles such as fine silts and clays, a sedimentation analysis is conducted and rates of sediments are determined using Stokes' law. [10%]

b) It is dangerous to assume soil behaviour solely based on PSD curves. For example fine particles of silt are very different to rock flour that is generated by grinding action during weathering, although both have same particle sizes. The water absorbency can be different between the particles and this leads to different soil behaviour.

Index tests such as Liquid limit, plastic limit & shrinkage limits need to be conducted to establish the soil behaviour in addition to PSD's. The Plasticity Index (PI) = LL - PL is an important parameter that is linked to water absorbency and the strength of soil. [20%]

c) First establish the capillary rise:

$$h_c = \frac{4T}{\gamma_w D} \quad \text{where 'D' is representative pore size.}$$

In soils D_{10} size represents the average pore size while D_{20} is the average particle size. $D_{10} = 0.005 \text{ mm}$

$$\text{Capillary rise } h_c = \frac{4 \times 7 \times 10^{-5}}{9.81 \times 0.005 \times 10^{-3}} = 5.708 \text{ m}$$

This is greater than 5m i.e. $h_c > 5\text{m}$, therefore all the soil above the water table will remain saturated but in 'suction'.

c) Cont

$$\gamma_d = 24.6 \text{ kN/m}^3 \quad e = 0.78$$

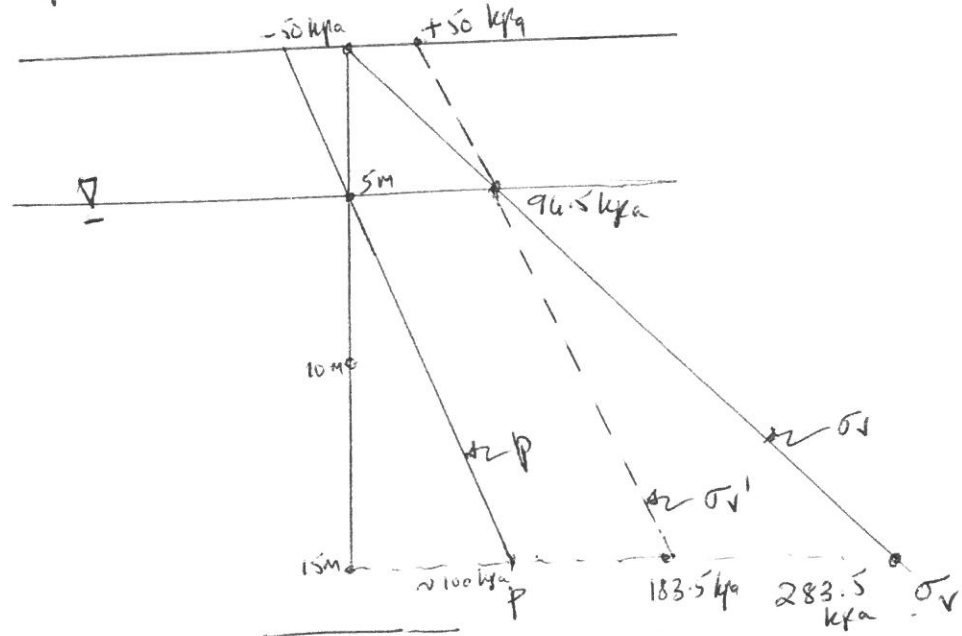
$$\gamma_d = \left(\frac{G_s + e S_r}{1+e} \right) \gamma_w = \frac{G_s \gamma_w}{1+e}$$

$$\therefore G_s = \frac{1.78 \times 14.6}{9.81} = 2.649 \approx 2.65$$

$$\gamma_{\text{sat}} = \frac{(2.65 + 0.78 \times 1) \times 9.81}{1 + 0.78} = 18.9 \text{ kN/m}^3$$

$$\sigma_v = 18.9 z$$

$$u = \gamma_w z \quad \text{for } z > 0 \Rightarrow \sigma_v' = \sigma_v - u$$



[20%]

1 d) i) see next page

$$\text{ii) } Q = K \times \Delta h \times N_b / N_u = 6.4 \times 10^{-7} \times 10 \times \frac{4}{10} = 2.56 \times 10^{-6} \text{ m}^3/\text{s}$$

$$L = 200 \text{ m} \quad Q = 2.56 \times 10^{-6} \times 200 \text{ m}^3/\text{s} \\ = 5.12 \times 10^{-4} \text{ m}^3/\text{s}$$

$$\text{or } 44236.8 \text{ litres per day}$$

$$\text{iii) Point A: } \bar{h}_A = 9.1 \text{ m} \quad y_A = 4.15 \text{ m} \Rightarrow h_A = 9.1 - 4.15 = 4.95 \text{ m} \\ p_A = 48.56 \text{ kPa}$$

$$\text{Point B: } \bar{h}_B = 5.1 \text{ m} \quad y_B = 1.96 \text{ m} \Rightarrow h_B = 3.14 \text{ m} \Rightarrow p_B = 30.8 \text{ kPa}$$

$$\text{Point C: } \bar{h}_C = 5.2 \text{ m} \quad y_C = 6 \text{ m} \Rightarrow h_C = 0.6 = p_C = -6 \text{ kPa}$$

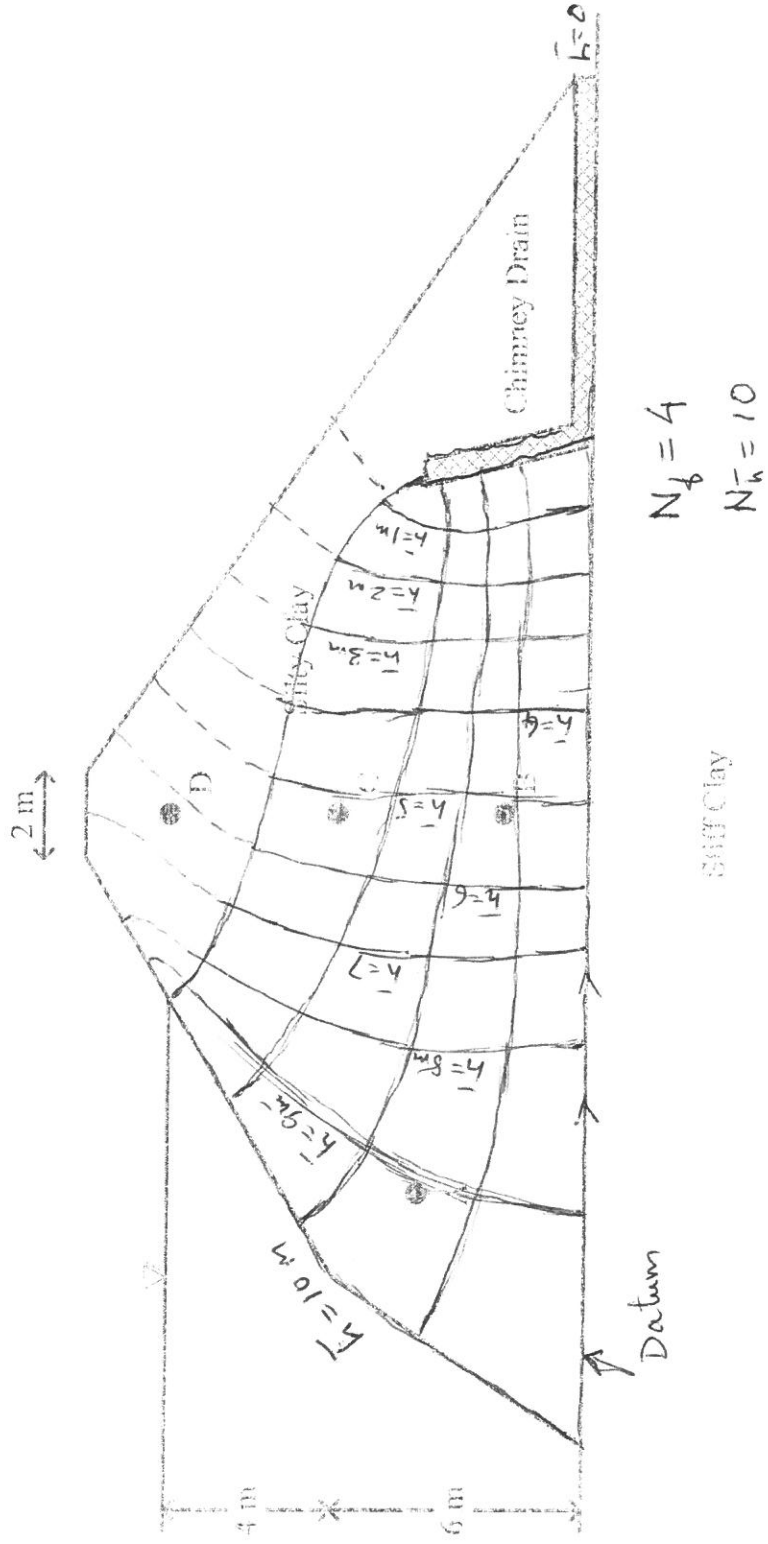
$$\text{Point D: } \bar{h}_D = 6.2 \text{ kPa} \quad y_D = 10 \text{ m} \Rightarrow h_D = 6.1 - 10 = -3.9 \text{ m}$$

$$\therefore p_D = -38.259 \text{ m} \approx -40 \text{ kPa}$$

[15%]

Candidate No:

DRAWN TO SCALE



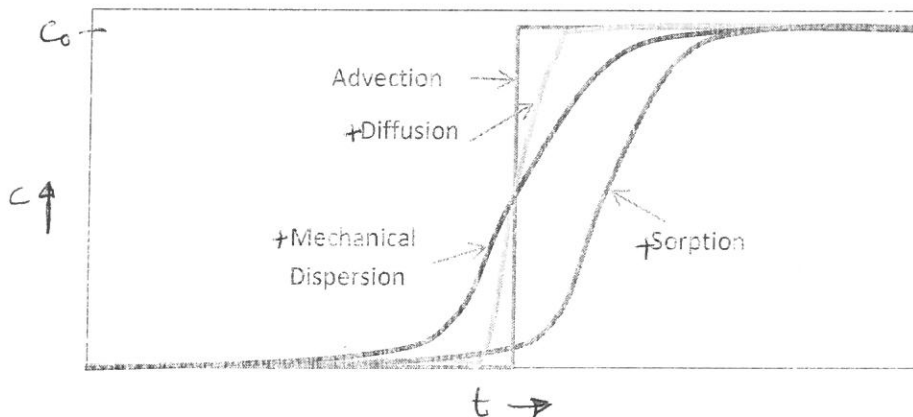
Extra copy of Fig. 1

3D8 Building Physics & Environmental Geotechnics

Q2) Cribbs

The contaminant transport mechanisms in ground water flow are: Advection, Diffusion, Mechanical dispersion and Sorption. Advection is the process by which the contaminant simply flows along with the ground water. Diffusion can occur with no ground water flow and is due to differences in concentrations and follows Fick's law. Mechanical Dispersion is transport due to mixing up of the contaminant as the ground water flows through soil and depends on the pore size, pore shape and the boundary layer formation at the interface between soil grains and the pore fluid. Sorption is when the contaminant either absorbs or adsorbs onto the soil grains.

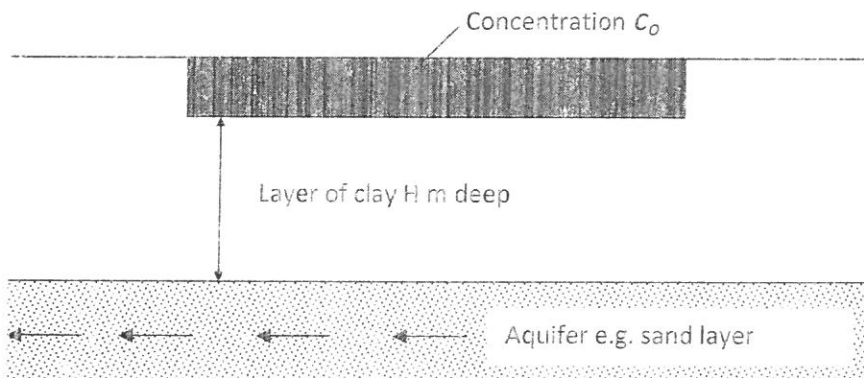
Advection will result in a step function or piston like flow causing a step change in concentration as the contaminant arrives at a given point (see Figure below). Diffusion will be more gradual change of concentration with time. Mechanical dispersion causes much more spread in concentration over time as shown below. Sorption has the effect of delaying/retarding the whole contaminant transport.



[20%]

2b) The advection dispersion equation is given as: $\frac{\partial c}{\partial t} = D_l \frac{\partial^2 c}{\partial z^2} - v_f \frac{\partial c}{\partial z}$

For steady state condition LHS = 0 i.e. $\frac{\partial c}{\partial t} = 0$.



The advection-dispersion equation becomes:

$$D_l \frac{\partial^2 c}{\partial z^2} = v_f \frac{\partial c}{\partial z}$$

and integrating once with respect z gives:

$$\frac{D_l}{v_f} \frac{\partial c}{\partial z} = c - P$$

where P is a constant, while integrating again gives:

$$\ln(c - P) = \frac{v_f z}{D_l} + \ln Q$$

where Q is also a constant. Rearranging gives:

$$c = P + Q \exp\left(\frac{v_f z}{D_l}\right)$$

which must satisfy the boundary conditions:

$$\text{for } z = 0 \quad c = P + Q = c_0$$

$$\text{for } z = L \quad c = P + Q \exp\left(\frac{v_f L}{D_l}\right) = 0$$

the solution of which gives:

$$P = \frac{-c_0 \exp\left(\frac{v_f L}{D_l}\right)}{1 - \exp\left(\frac{v_f L}{D_l}\right)} \quad \text{and} \quad Q = \frac{c_0}{1 - \exp\left(\frac{v_f L}{D_l}\right)}$$

and therefore the steady state distribution is:

$$\frac{c}{c_0} = \frac{\exp\left(\frac{v_f z}{D_l}\right) - \exp\left(\frac{v_f L}{D_l}\right)}{1 - \exp\left(\frac{v_f L}{D_l}\right)}$$

If the mean linear water velocity is very small, then the exponentials can be approximated by power series:

$$\frac{c}{c_0} = \frac{\left(1 + \frac{v_f z}{D_l}\right) - \left(1 + \frac{v_f L}{D_l}\right)}{1 - \left(1 + \frac{v_f L}{D_l}\right)} = \frac{L - z}{L}$$

i.e. if advection is negligible and diffusion therefore dominates then the steady state distribution is linear from source to sink. This result could have also been reached by integrating the diffusion equation directly.

[25%]

Q3) c) The relevant equation for GSHP is;

$$\frac{E}{2\pi B} \ln\left(\frac{r_2}{r_1}\right) = -\lambda (T_2 - T_1)$$

Substituting values and allowing for heat abstraction;

$$\frac{2.5 \times 10^3}{2\pi 50} \ln\left(\frac{2.4}{0.4}\right) = 2.6 (T_2 - 1)$$

Therefore at distance of 2m from the bore well wall, the temperature will be = 6.484 °C.

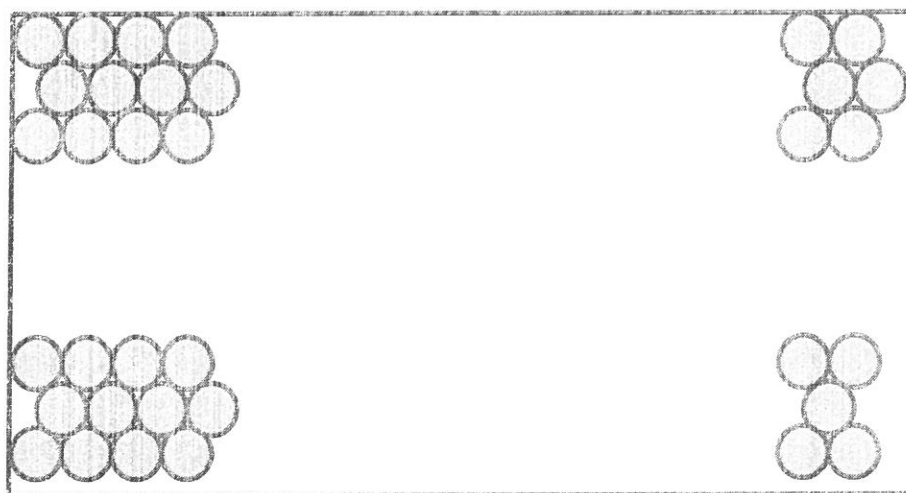
The radius of influence can be estimated as when the temperature T_2 approaches the ambient ground temperature of 10 °C.

$$\frac{2.5 \times 10^3}{2\pi 50} \ln\left(\frac{R}{0.4}\right) = 2.6 (10 - 1)$$

Therefore the radius of influence of the GSHP is $R = 7.57$ m.

[25%]

3) d) For maximum energy output we want to pack the GSHP's as closely as possible, but without the Radius of influence overlapping. We can fit 26 wells in the first row as shown below, which is the plan view of site 401.5m x 200m. Similarly we can fit 15 wells in each column.



So total number of wells we can have on this site = $26 \times 13 = 390$ wells.

Total energy output = $390 \times 2.5 \text{ kW} = 975 \text{ kW}$ (i.e. approximately 1 MW).

[30%]

7/11

(iii) (b) $\hat{T}_c(x, t) = \hat{T}(x) e^{2\pi i t / t_p}$ — (1)

$\hat{T}(x) = T_1 e^{-(1+i)x/d_p}$ — (2)

Insert (2) in (1)

(i) $\hat{T}_c(x, t) = T_1 e^{-x/d_p} \cdot e^{i(2\pi t/t_p - x/d_p)}$

(A) — $T(x, t) = T_1 e^{-x/d_p} \sin\left(\frac{2\pi t}{t_p} - \frac{x}{d_p}\right)$

(ii) $\hat{Q}(x) = \lambda A \frac{\partial \hat{T}}{\partial x}$ (heat conduction)

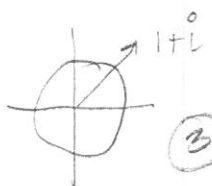
~~III~~

$\hat{Q}(x, t) = \lambda A \frac{\partial \hat{T}(x, t)}{\partial x}$

$\Rightarrow \lambda A \frac{\partial [T_1 e^{-(1+i)x/d_p} e^{2\pi i t/t_p}]}{\partial x}$

$\Rightarrow \frac{\lambda A}{d_p} T_1 \sqrt{2} e^{-x/d_p} e^{i[\pi/4 - x/d_p + 2\pi t/t_p]}$

$(1+i) = \sqrt{2} e^{i\pi/4}$ (B) $\Rightarrow \frac{\lambda A}{d_p} T_1 \sqrt{2} e^{-x/d_p} \sin\left(\frac{2\pi t}{t_p} - \frac{x}{d_p} + \frac{\pi}{4}\right)$



(iii) (3) From (A) Max T $\sim \frac{2\pi t}{t_p} - \frac{x}{d_p} = \frac{\pi}{2}$

(4) From (B) Max Q $\sim \frac{2\pi t}{t_p} - \frac{x}{d_p} + \frac{\pi}{4} = \frac{\pi}{2}$

III (b) (iii) ④ - ③

$$\frac{2\pi}{t_p} (t_r - t_a) - \frac{\pi}{4} = 0$$

$$t_r - t_a = \frac{t_p}{8}$$

III (a)

$$\text{diffusivity (thermal)} = \frac{\lambda}{\rho c}$$

$$a = \frac{\lambda}{\rho c} = \frac{3.2}{2 \times 10^6} = 1.6 \times 10^{-6} \text{ m}^2/\text{s}$$

- * ^{defines} rate at which heat flows thru a material
- * measure the material's ability to conduct heat relative to storing it.
- * characterizes 'unsteady' heat conduction

IV (c)

For 27°C dbT & 55% RH,

Dewpoint is at 17°C

From Psychrometric chart ← humidity at 17°C ~ 0.012 kg/kg

air is cooled to 15°C

from psychrometric chart ← humidity at 15°C ~ 0.0106 kg/kg

$$\begin{aligned} \text{Moisture condensed out} &: 0.012 - 0.0106 \\ &= 0.0014 \text{ kg/kg} \end{aligned}$$

IV (a) Geometry of the Room

$$\begin{aligned}
 l &= 6 \text{ m} \\
 w &= 4 \text{ m} \quad (\text{ext. wall}) \\
 h &= 3 \text{ m} \\
 \text{Window} &= 2.5 \times 2.2 \text{ m}
 \end{aligned}$$

Properties: $n = 0.5 \text{ ACH}$

$$\begin{aligned}
 U_{\text{extwall}} &= 0.6 \text{ W/m}^2\text{K} \\
 U_{\text{intwall}} &= 1.6 \text{ W/m}^2\text{K} \\
 U_{\text{window}} &= 2.8 \text{ W/m}^2\text{K}
 \end{aligned}$$

Environment:

$$T_o = -2^\circ\text{C} \quad T_{\text{ad}} = 19^\circ\text{C}$$

(i) Indoor Room Temperature

(a) heat Gains from internal walls

$$\begin{aligned}
 &U_{\text{int}} \times \text{Area}_{\text{int}} \times (T_{\text{ad}} - T_i) \\
 \Rightarrow &1.6 \times [2 \times (6 \times 4) + 2 \times (6 \times 3) + (4 \times 3)] \times \dots \\
 &\dots \times (19 - T_i) \\
 \Rightarrow &153.6 (19 - T_i) \quad \text{--- (1)}
 \end{aligned}$$

(b) heat losses:

$$\begin{aligned}
 &[U_{\text{win}} \times \text{Area}_{\text{win}} + U_{\text{extwall}} \times \text{Area}_{\text{extwall}}] \times (T_i + 2) + \dots \\
 &\dots + \left[\overset{\text{Fair}}{C_{\text{air}}} \times \frac{nV}{3600} \right] \times (T_i + 2)
 \end{aligned}$$

* Fair from data book

$$\Rightarrow [15.4 + 3.9 + 12] \times (T_i + 2) \quad \text{--- (2)}$$

Heat Balance: (1) = (2)

$$\begin{aligned}
 153.6 (19 - T_i) &= 31.3 (T_i + 2) \\
 \Rightarrow 4.9 (19 - T_i) &= T_i + 2 \\
 \Rightarrow &\boxed{15.45^\circ\text{C}}
 \end{aligned}$$

2

(ii) Heating Demand to maintain 23°C

$$\begin{cases} UA_{\text{int}} = 153.6 \text{ W/K} & (\text{from (a)}) \\ UA_{\text{ext}} = 31.3 \text{ W/K} \end{cases}$$

$$\begin{aligned} \text{heating demand} &\sim 153.6 (23 - 19) + 31.3 (23 + 2) \\ &\sim \boxed{1397 \text{ Watts}} \end{aligned}$$

(iii)

Area of Ceiling \sim area of radiator
 $\sim 6 \times 4 = 24 \text{ m}^2$

Area of all other surfaces = 84 m^2

$$\epsilon_1 = 0.9 \quad (\text{for all surfaces})$$

$$T_{\text{surface}} = 23^{\circ}\text{C} \quad (T_2)$$

$$T_{\text{ceiling}} = 34^{\circ}\text{C} \quad (T_1)$$

$$Q_{12} = hr A_1 \cdot (T_1 - T_2)$$

$$hr = \frac{4 \sigma T_{12}^3}{\frac{1 - \epsilon_1}{\epsilon_1} + \frac{1}{F_{12}} + \frac{1 - \epsilon_2}{\epsilon_2} \frac{A_1}{A_2}}$$

$$\sigma = 5.67 \times 10^{-8} \text{ W m}^{-2} \text{ K}^{-4} \quad (\text{data book})$$

$$T_{12} = \frac{T_1 + T_2}{2} \text{ K}; \quad F_{12} = 1 \quad (\text{view factor})$$

$$T_{12} = 301.65 \text{ K}$$

$$hr = 5.44 \text{ W/m}^2 \text{ K}$$

$$\begin{aligned} Q_{12} &= 5.44 \times 24 \times (34 - 23) \\ &= \boxed{1438 \text{ W}} \end{aligned}$$

Yes sufficient for (ii)

IV

(b) $\lambda_{\text{wall}} = 0.60 \text{ W/mK}$ $d_{\text{wall}} = 0.250 \text{ m}$
 $d_{\text{clay}} = 0.2 \text{ m}$
 $\lambda_{\text{clay}} = 0.09 \text{ W/mK}$ $R_{\text{so}} = 0.04$
 $\epsilon_{\text{clay}} = 25 \times 10^{-6}$ $R_{\text{si}} = 0.13$
 $U\text{-Value}_{\text{grd}} = 0.317 \text{ W/m}^2\text{K}$
 $R_{\text{ceiling}} = 2.5 \text{ m}^2\text{K/W}$

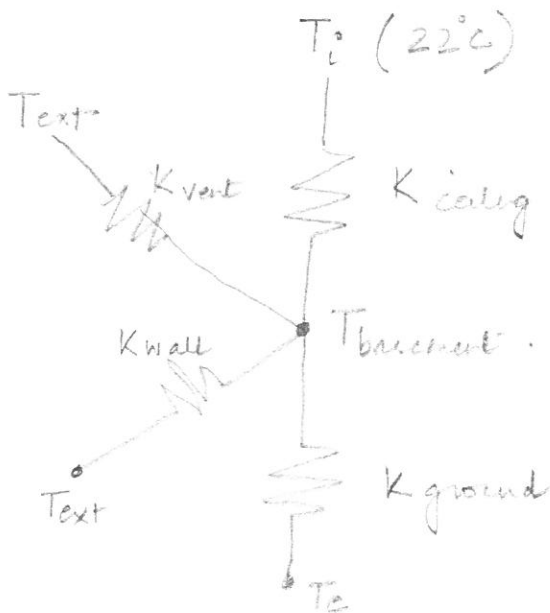
$n = 0.5 \text{ ACH}$

$T_{\text{ext}} = 3.5^\circ\text{C}$ $RH_{\text{ext}} = 80\%$

$T_{\text{int}} = 22^\circ\text{C}$ $RH_{\text{int}} = 48\%$

$\text{Area} = 10 \times 16 \text{ m}^2$

$\text{height} = 1 \text{ m}$



$\text{Area}_{\text{wall}} = 2(10 + 16) \times 1$
 $= 52 \text{ m}^2$

$\text{Area}_{\text{floor}} = 10 \times 16 = 160 \text{ m}^2$

$\text{Volume} = 10 \times 16 \times 1 = 160 \text{ m}^3$

$K_{\text{ceiling}} = \frac{1}{R_{\text{ceiling}}} \times \text{Area}_{\text{ceiling}} \Rightarrow 64 \text{ W/K}$

$K_{\text{out}} \sim K_{\text{ground}} + K_{\text{vent}} + K_{\text{wall}} \Rightarrow$

$U_{\text{ground}} \times \text{Area}_{\text{ground}} + \frac{nV}{3600} \text{ fair air} + U_{\text{wall}} \text{ Area}_{\text{wall}}$

=

①

$$R_{\text{wall}} = R_{\text{so}} + R_{\text{si}} + \frac{d_{\text{wall}}}{\lambda_{\text{wall}}}$$

$$= 0.13 + 0.04 + \frac{0.25}{0.60} = 0.59 \text{ m}^2\text{K/W}$$

$$U_{\text{wall}} = \frac{1}{R_{\text{wall}}} = 1.7 \text{ W/m}^2\text{K}$$

Inserting in ①

$$0.317 \times 160 + \frac{0.5 \times 160}{3600} \times 1.2 \times 10^3 + 1.7 \times 160$$

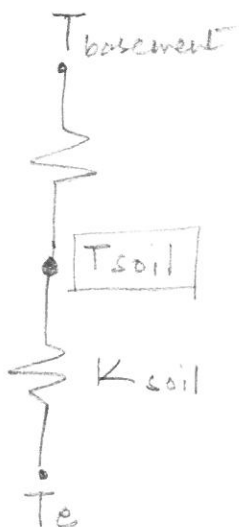
$$\Rightarrow 166.79 \text{ W/K}$$

$$T_{\text{basement}} = \frac{K_{\text{out}} T_{\text{ext}} + K_{\text{ceiling}} T_{\text{int}}}{K_{\text{out}} + K_{\text{ceiling}}}$$

$$\Rightarrow 12.26 \text{ }^\circ\text{C}$$

Moisture Calculation

Temperature at Soil Surface



$$R_{\text{clay}} = R_{\text{si}} + \frac{d_{\text{clay}}}{\lambda_{\text{clay}}}$$

$$= 0.13 + \frac{0.2}{0.09}$$

$$= 2.35 \text{ m}^2\text{W/K}$$

$$K_{\text{clay}} = \frac{1}{R_{\text{clay}}} = 0.426$$

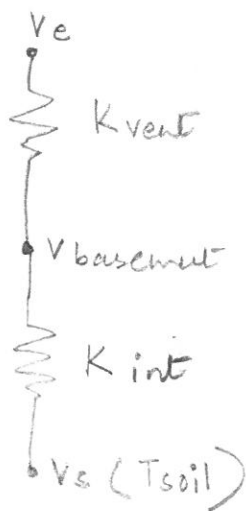
$$K_{\text{soil}} = \left[\frac{1}{U_{\text{soil}}} - \frac{0.20}{0.09} - 0.13 \right]^{-1}$$

$$= 1.25 \text{ W/K}$$

$$T_{soil} = \frac{K_{clay} T_{basement} + K_{soil} T_e}{K_{clay} + K_{soil}}$$

$$= 9.5^\circ\text{C}$$

$$V_s(T_{soil}) = 9.11 \text{ g/m}^3$$



$$K_{in} = \frac{\delta_{clay} \cdot \text{Area}}{d_{clay}} =$$

$$K_{vent} = \frac{n}{3600} \times \text{Volume}$$

$$V_{basement} = \frac{K_{in} V_s(T_{soil}) + K_{vent} V_s(T_e) RH}{K_{in} + K_{vent}}$$

$$= 7.91 \text{ g/m}^3$$

Relative Vapour Content

$$RH = \frac{7.91}{V_s(T_{basement})} \times 100$$

$$= \frac{7.91}{10.87} \times 100 = 73\%$$

i.e. no problem w/ moisture