

ENGINEERING TRIPOS PART IIA 2004

Solutions to Module 3A3

Fluid Mechanics II

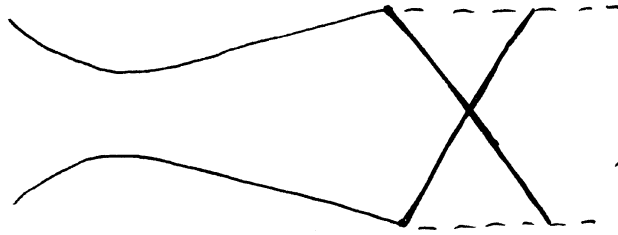
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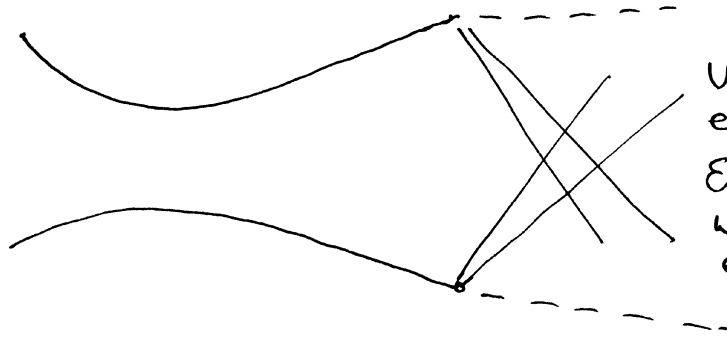
PAPER 3A3 - 2004

Q1

a)



Overexpanded shocks at exit



Under-expanded. Expansion waves at exit.

b)

$$\frac{P_2}{P_{01}} = \frac{1}{4.25} = 0.2353 \rightarrow M_{215} = 1.6$$

The exit Mach No is 1.6 if the flow is isentropic.

$$\text{This would have } \frac{A_2}{A^*} = \frac{1.281}{1.0246}$$

$$\rightarrow A_2 = 1.2502 A^*$$

So the exit area and exit pressure are both compatible with isentropic flow at $M_2 = 1.6$.

$$\begin{aligned} \text{Thrust} &= \dot{m} V_2 \text{ since exit pressure is ambient} \\ &= \frac{\dot{m} \sqrt{C_p T_0}}{A P_0} \times \frac{V}{\sqrt{C_p T_0}} \times A P_0 \end{aligned}$$

Taking A at throat, $P_0 = P_{01}$

Q
Cont

$$\begin{aligned} \text{Thrust} &= 1.281 \times 0.8229 \times \frac{\pi \times 3^2}{4} \times 10^{4.25} \text{ N} \\ &= \underline{\underline{31.66 \text{ kN}}} \end{aligned}$$

c)

For nozzle 1, $A/A^* = 1.555$.

If flow is isentropic within the nozzle

$$M_{\text{exit}} = 1.9.$$

$$\rightarrow \frac{P_e}{P_{01}} = 0.1492$$

This is lower than the actual exit pressure so there must be a shock at exit or within the nozzle. For a normal shock

$$\begin{aligned} \text{at exit } P_2/P_{01} &= \frac{P_2}{P_1} \times \frac{P_1}{P_{01}} = 4.025 \times 0.149 \text{ Tables.} \\ &= 0.599. \end{aligned}$$

The actual exit pressure is lower than this so there is an oblique shock at exit.

$$\text{Thrust} = (P_e A_e + \dot{m} V_e) - P_a A_e$$

$$= \frac{F}{\dot{m} \sqrt{C_p T_0}} \times \frac{\dot{m} \sqrt{C_p T_0}}{A_e P_0} \times A_e P_0 - P_a A_e$$

$$= A^* P_0 \left[1.097 \times 0.824 \times \frac{A_e}{A^*} - \frac{P_a}{P_0} \frac{A_e}{A^*} \right]$$

$$= \frac{\pi \cdot 3^2}{4} \times 4.25 \times 10^5 \left[1.097 \times 0.824 \times 1.555 - \frac{1}{4.25} \times 1.555 \right]$$

$$= \underline{\underline{31.235 \text{ kN}}}$$

Q6
cont'd
c)

For the second nozzle, $A/A^* = 1.066$

Isentropic flow $\rightarrow M_{exit} = 1.3$

$$\rightarrow \frac{P_e}{P_{o1}} = 0.3609$$

This is higher than the actual exit pressure so there must be expansion waves at exit - the nozzle is underexpanded.

$$\begin{aligned} \text{Thrust} &= \frac{F}{m\sqrt{c_p T_0}} \times \frac{m\sqrt{c_p T_0}}{A_e P_0} \times A_e P_0 - A_e P_a \\ &= 1.066 A^* \times P_0 \left[1.011 \times 1.201 - \frac{1}{4.25} \right] \\ &= \underline{\underline{31.349 \text{ kN}}} \end{aligned}$$

d)

$$T = mV_e + (P_e - P_a) A_e$$

$$\delta T = m \delta V_e + (P_e - P_a) \delta A_e + A_e \delta P_e$$

$$\text{Euler. } \delta V = -\frac{1}{\rho V} \delta P$$

$$\text{i.e. } \delta V_e = -\left(\frac{m}{A_e}\right)^{-1} \delta P_e$$

Substituting in eqn for δT

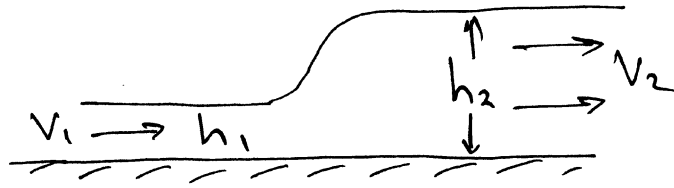
$$\rightarrow \delta T = (P_e - P_a) \delta A_e$$

which $\rightarrow 0$ when $P_e = P_a$

So $P_e = P_a$ gives the maximum thrust.

Q2

a)



$$V_1 h_1 = V_2 h_2 \quad \text{--- continuity}$$

$$V_1^2 h_1 + g \frac{h_1^2}{2} = V_2^2 h_2 + \frac{g h_2^2}{2} \quad \text{--- momentum}$$

$$\rightarrow V_1^2 h_1 + \frac{g h_1^2}{2} = V_1^2 \frac{h_1^2}{h_2} + \frac{g h_2^2}{2}$$

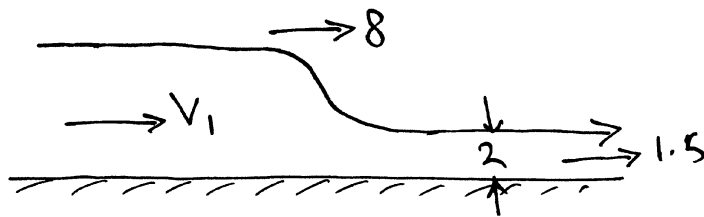
$$V_1^2 \left(h_1 - \frac{h_1^2}{h_2} \right) = \frac{g}{2} (h_2^2 - h_1^2)$$

$$\frac{V_1^2}{g h_1} \left(h_1^2 - \frac{h_1^3}{h_2} \right) = \frac{1}{2} (h_2^2 - h_1^2)$$

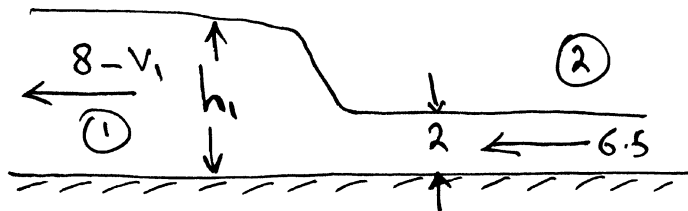
$$F_1^2 \frac{h_1^2}{h_2} (h_2 - h_1) = \frac{1}{2} (h_2 - h_1) (h_2 + h_1)$$

$$F_1^2 = \frac{1}{2} \left(\frac{h_2 + h_1}{h_1} \right) \frac{h_2}{h_1}$$

b)



Absolute frame



Relative frame

$$F_2 = \frac{6.5}{\sqrt{2g}} = 1.467, \quad h_2 = 2$$

$$\text{Let } \frac{h_1}{h_2} = x$$

$$1.467^2 = \frac{1}{2} x(1+x)$$

Q
cont'd

2

$$x^2 + x - 4.307 = 0$$

$$x = 1.6346$$

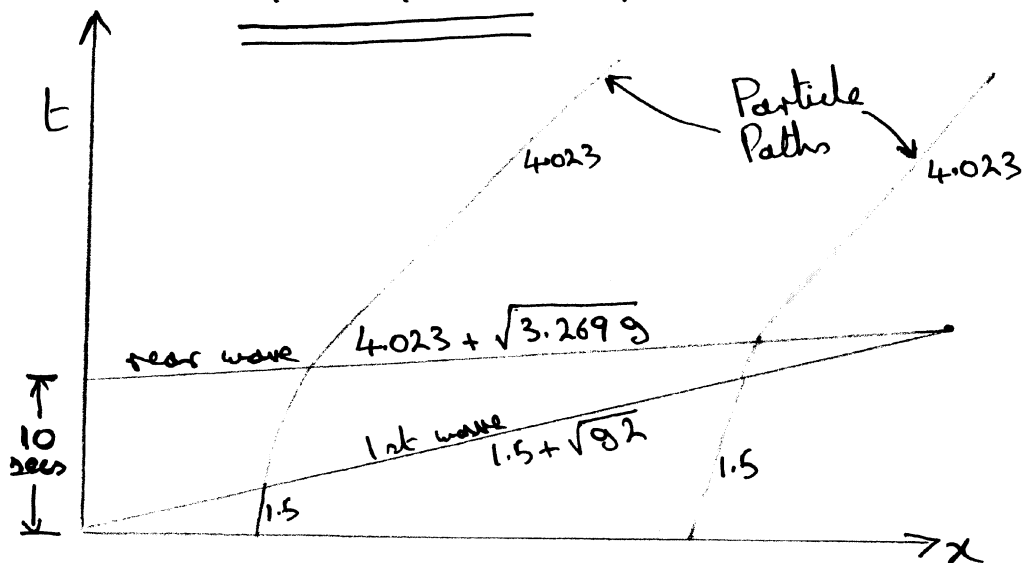
$$\rightarrow h_1 = 3.269 \text{ m}$$

$$v_1 h_1 = v_2 h_2 \rightarrow (8 - v_1) = \frac{6.5 \times 2}{3.269}$$

$$\rightarrow 8 - v_1 = 3.976$$

$$\underline{\underline{v_1 = 4.023 \text{ m/s}}}$$

(c)



First wave moves at $1.5 + \sqrt{2g} = 5.929 \text{ m/s}$

Rear wave moves at $4.023 + \sqrt{3.269g} = 9.686 \text{ m/s}$.

The waves coalesce when

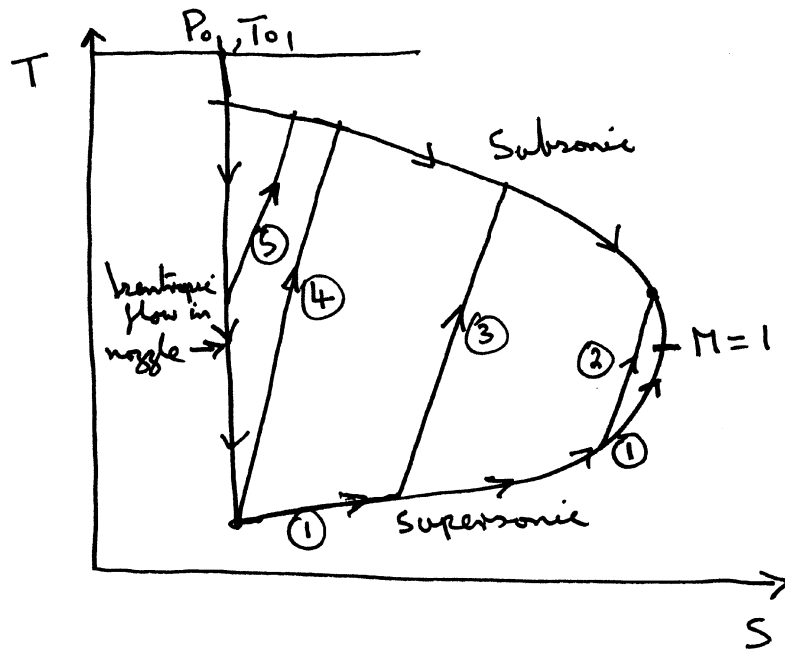
$$5.929 t = 9.686(t - 10)$$

$$t = 25.78 \text{ secs.}$$

$$\underline{\underline{x = 152.8 \text{ m}}}$$

Q3//

a)



- | | | |
|---|--|--|
| ① | | Low C_f |
| ② | | higher C_f
shock at exit |
| ③ | | higher C_f
Shock in pipe |
| ④ | | higher C_f
Shock at end of nozzle |
| ⑤ | | high C_f
Shock in nozzle. |

b)

At exit $\frac{m \sqrt{C_p T_0}}{A P} = 2.425$ and $P = 1 \text{ bar}$.

At exit of nozzle $\frac{m \sqrt{C_p T_0}}{A P_0} = 2.425 \times \frac{1}{2.425} = \underline{.890}$

Q3
cont'd

b)

Tables $\rightarrow M_2 = 1.8$ or 454

$$\rightarrow \frac{4fL_{\max}}{D} = 0.242 \text{ or } 1.5$$

Since the pipe is choked at exit $L_{\max} = 6.05 \text{ m}$.

$$\therefore f = \underline{\underline{.005}} \text{ or } \underline{\underline{0.031}}$$

c)

After shock $P = 1.49 \text{ bar}$.

$$\text{So } \frac{m \sqrt{C_p T_0}}{A P} = 2.425 \times \frac{1}{1.49} = 1.6275$$

$$\rightarrow M = 0.70 \text{ after shock}$$

$$\rightarrow M_s = 1.50 \text{ before shock.}$$

Downstream of shock $\frac{4fL}{D} = .208$

$$L = (6.05 - 2.03) = 4.02$$

$$\rightarrow \underline{\underline{f = .00647}}$$

Upstream of shock $\frac{4fL}{D} = 0.136$

At exit of nozzle $\frac{4fL}{D} = .242$.

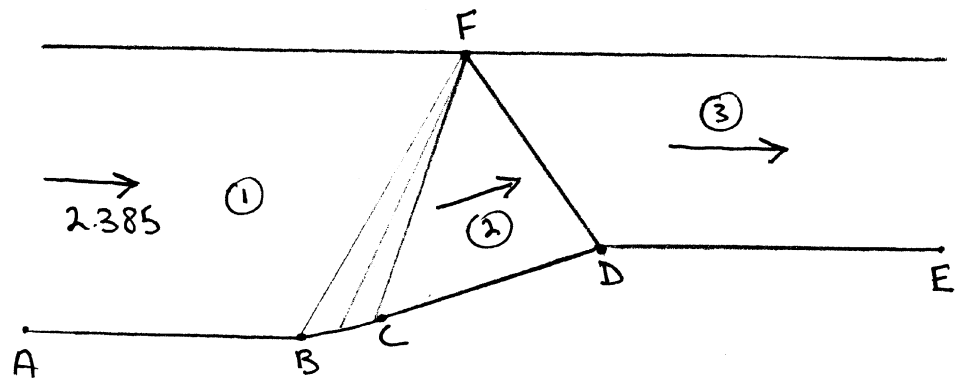
$$\frac{4f \Delta L}{D} = .242 - .136 = .106$$

$$\text{and } \Delta L = 2.03 \text{ m}$$

$$\rightarrow \underline{\underline{f = .00652}}$$

Values of f are effectively the same upstream and downstream of the shock.

Q4



a)

The compression waves from BC are weak and isentropic and turn the flow by 10°

$$v + \theta = \text{const}$$

$$\text{Tables} \rightarrow v_1 = 36.28^\circ$$

$$\therefore v_2 = 26.28^\circ \rightarrow M_2 = 2.0 \text{ \textit{v} closer}$$

Across the shock FD flow turns by 10° from $M_2 = 2.0$.

$$\text{Tables} \rightarrow \underline{M_3 = 1.6395} \quad \text{and} \quad \frac{\Delta S}{C_v} = .0062$$

$$\frac{w \sqrt{C_p T_0}}{A_3 P_3} = .9984 \quad \text{at} \quad M_3 = 1.6395$$

$$\frac{w \sqrt{C_p T_0}}{A_1 P_1} = .5404 \quad \text{at} \quad M_1 = 2.385.$$

$$\therefore \frac{A_3}{A_1} = \frac{P_1}{P_3} \times \frac{.5404}{.9984}$$

$$\Delta S = -R \ln \frac{P_3}{P_1} = .0062 C_v$$

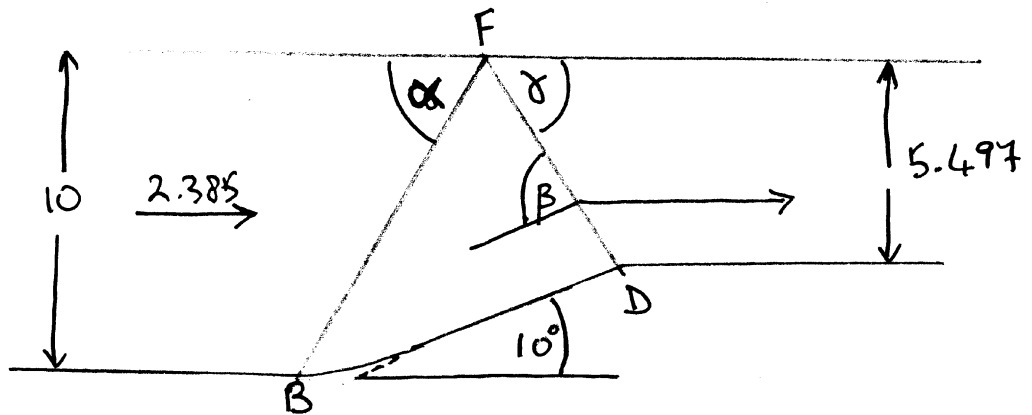
$$\rightarrow P_3 / P_1 = e^{-.0062 \left(\frac{1}{\gamma-1}\right)} = .9846$$

$$\rightarrow \underline{\underline{A_3 / A_1 = 0.5497}}$$

Q

b)

2



$$\text{Angle } \alpha = \sin^{-1} \frac{1}{M_1} = 24.81$$

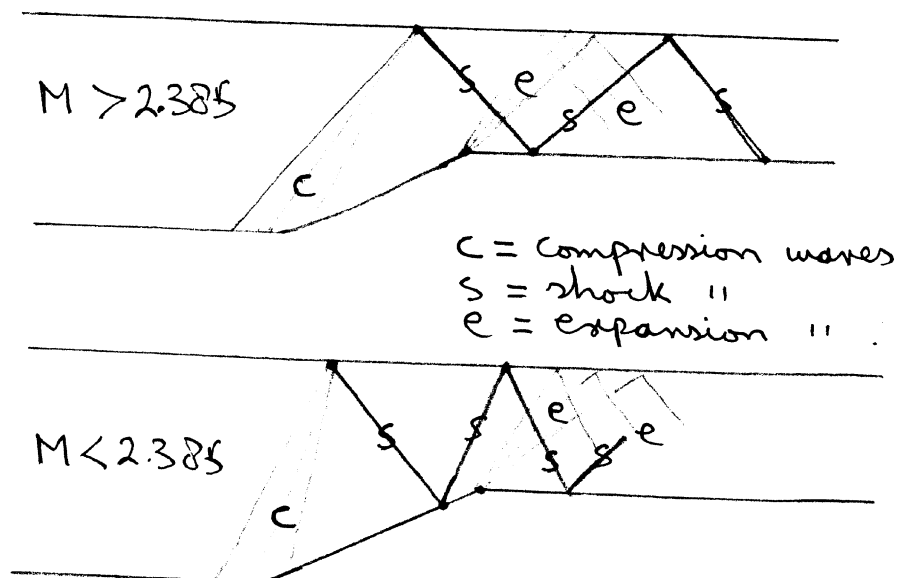
$$\text{Angle } \beta = 39.33^\circ \text{ (from Tables.)}$$

$$\therefore \text{Angle } \gamma = 29.33^\circ$$

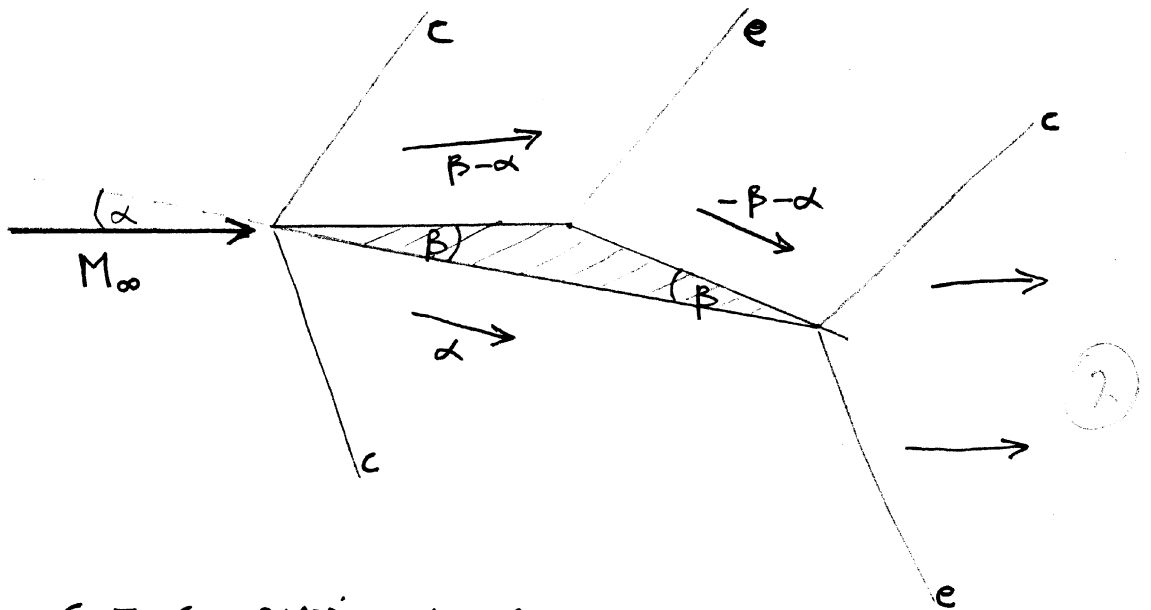
$$BF = \left(\frac{10}{\tan \alpha}, 10 \right) = (21.63, 10)$$

$$FD = \left(\frac{5.497}{\tan \gamma}, -5.497 \right) = (9.784, -5.497)$$

$$\therefore \underline{\underline{BD = (31.41, 4.503)}}$$



Q5



c = compression wave

e = expansion wave

$$C_p = \pm \frac{2\theta}{\sqrt{M_\infty^2 - 1}} \quad \begin{array}{l} + \text{ for compression} \\ - \text{ for expansion.} \end{array}$$

$$\text{On lower surface } C_p = \frac{+2\alpha}{\sqrt{M_\infty^2 - 1}}$$

$$\text{On front upper surface } C_p = +\frac{2(\beta - \alpha)}{\sqrt{M_\infty^2 - 1}}$$

$$\text{On rear upper surface } C_p = -\frac{2(\beta + \alpha)}{\sqrt{M_\infty^2 - 1}}$$

Resolving perp. to lower surface of aerofoil

$$\begin{aligned} F_n &= \frac{c}{\sqrt{M_\infty^2 - 1}} \left[2\alpha - (\beta - \alpha) + (\beta + \alpha) \right] \times \frac{1}{2} \rho_\infty V_\infty^2 \\ &= \frac{4\alpha c}{\sqrt{M_\infty^2 - 1}} \times \frac{1}{2} \rho_\infty V_\infty^2 \end{aligned}$$

Resolving parallel to the lower surface

$$F_D = 2 \frac{c}{\sqrt{M_\infty^2 - 1}} \tan \beta \left[(\beta - \alpha) + (\beta + \alpha) \right] \times \frac{1}{2} \rho_\infty V_\infty^2$$

Q
cont

$$\frac{F_D}{\frac{1}{2} \rho_{\infty} V_{\infty}^2} = \frac{2C\beta^2}{\sqrt{M_{\infty}^2 - 1}} \quad \text{for } \beta \text{ small.}$$

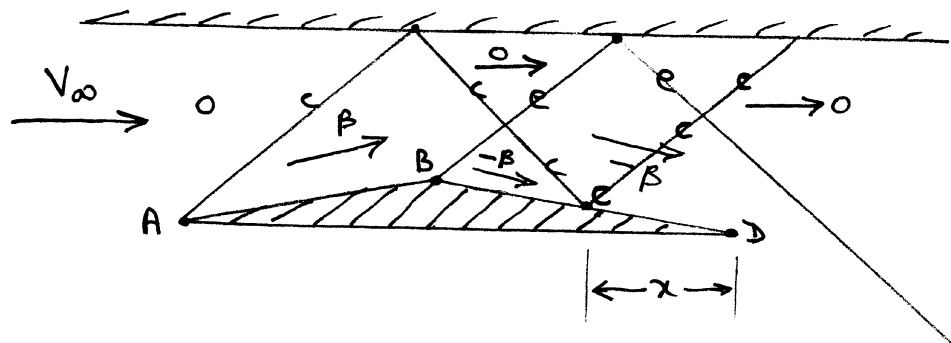
Resolving these parallel and perpendicular to the main stream

$$\frac{L}{\frac{1}{2} \rho_{\infty} V_{\infty}^2} = \frac{4\alpha C}{\sqrt{M_{\infty}^2 - 1}} \cos \alpha - \frac{2C\beta^2}{\sqrt{M_{\infty}^2 - 1}} \sin \alpha$$

$$\frac{D}{\frac{1}{2} \rho_{\infty} V_{\infty}^2} = \frac{2C\beta^2}{\sqrt{M_{\infty}^2 - 1}} \cos \alpha + \frac{4\alpha C}{\sqrt{M_{\infty}^2 - 1}} \sin \alpha$$

For small α

$$\underline{\underline{C_L = \frac{4\alpha}{\sqrt{M_{\infty}^2 - 1}}}}, \quad \underline{\underline{C_D = \frac{4\alpha^2 + 2\beta^2}{\sqrt{M_{\infty}^2 - 1}}}}$$



Along AB $C_p = \frac{+2\beta}{\sqrt{M_{\infty}^2 - 1}}$

Along BC $C_p = \frac{-2\beta}{\sqrt{M_{\infty}^2 - 1}}$

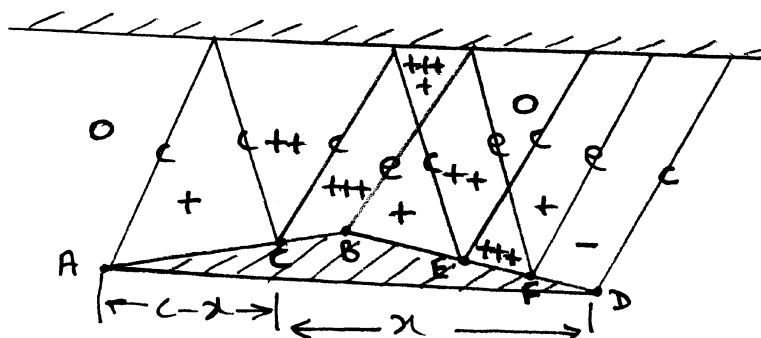
Along CD $C_p = \frac{+2\beta}{\sqrt{M_{\infty}^2 - 1}}$

$$\therefore C_D = \frac{(C/2 - x) 4\beta}{C \sqrt{M_{\infty}^2 - 1}} \tan \beta$$

Q
cont

For small β $C_D = \frac{1}{\sqrt{M_\infty^2 - 1}} \beta^2 \left(2 - \frac{4x}{c}\right)$

When $x > c/2$ the wave pattern becomes.



Pressure increases are denoted by + and decreases by - where each +/- represents one multiple of $\frac{2\beta}{\sqrt{M_\infty^2 - 1}}$ on C_p .

The 2 regions of +++ cancel out.

Length AC = $(c-x)$

Length BE = $2(c-x) - c/2 = (1.5c - 2x)$

Length ED = $\frac{c}{2} - (c-x) = (x - c/2)$

The drag is therefore proportional to

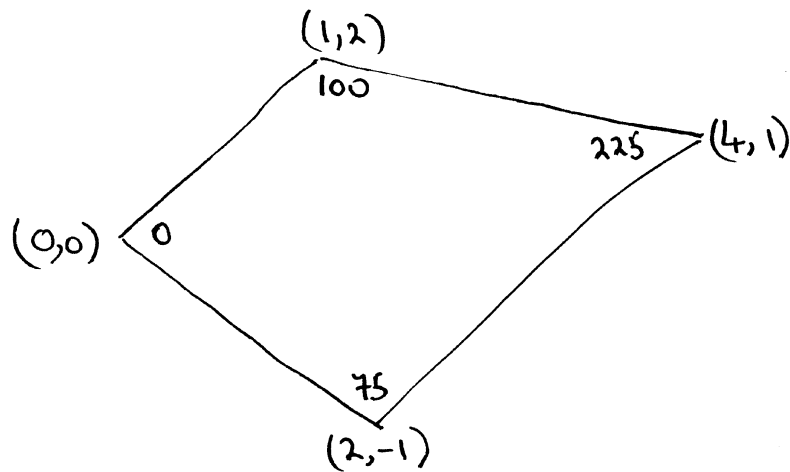
$$(c-x) - (1.5c - 2x) + (x - c/2)$$

$$= (-c + 2x)$$

So the drag increases again with x when $x > c/2$.

Q6

a)



Gauss $\frac{\partial \phi}{\partial x} = \frac{1}{A} \oint \phi dy$, $\frac{\partial \phi}{\partial y} = -\frac{1}{A} \oint \phi dx$ 2

$A = \text{area of cell} = \frac{1}{2} \times \text{vector product of diagonals}$

$$= \frac{1}{2} (4i + j) \times (\bar{3}i + 3j)$$

$$= \frac{1}{2} (12 + 1) = 6.5$$

Assuming a linear variation of ϕ between the corners of the cell,

$$\oint \phi dy = \frac{75}{2}(-1) + \frac{75+225}{2}(2) + \frac{225+100}{2}(1) + \frac{100+0}{2}(-2)$$

$$= -375 + 300 + 162.5 - 100$$

$$= +325.$$

$$\text{So } \frac{\partial \phi}{\partial x} = \frac{325}{6.5} = \underline{\underline{50 \text{ m/s.}}}$$

$$\oint \phi dx = \frac{75+0}{2}(2) + \frac{75+225}{2}(2) + \frac{225+100}{2}(-3) + \frac{100+0}{2}(-1)$$

$$= 75 + 300 - 487.5 - 50 = -162.5$$

$$\text{So } \frac{\partial \phi}{\partial y} = + \frac{162.5}{6.5} = \underline{\underline{25 \text{ m/s.}}}$$

Q

Assuming a change $\Delta\phi$ at the (4,1) grid point,

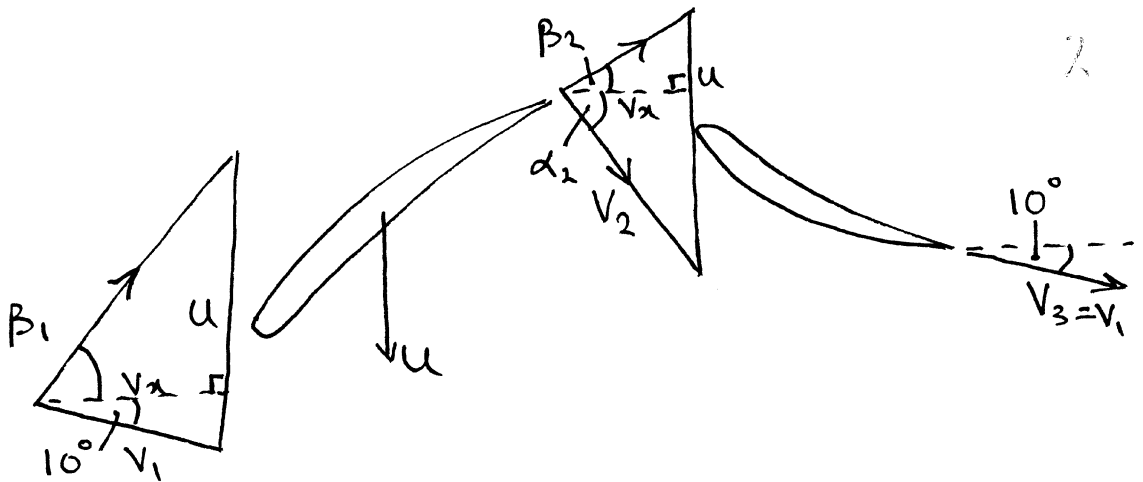
$$\text{change in } \oint \phi dy = \frac{\Delta\phi}{2} (2+1) = 1.5 \Delta\phi$$

$$\text{so change in } V_x = \frac{1.5}{6.5} \Delta\phi = \underline{\underline{.231 \Delta\phi}}$$

$$\text{change in } \oint \phi dx = \frac{\Delta\phi}{2} (2-3) = -0.5 \Delta\phi$$

$$\text{so change in } V_y = + \frac{0.5}{6.5} \Delta\phi = + \underline{\underline{.0769 \Delta\phi}}$$

b)



$$(i) \quad \tan \beta_1 = -\frac{u + V_x \tan 10^\circ}{V_x} = -\frac{320}{144} + \frac{144}{320} \tan 10^\circ$$

$$\rightarrow \underline{\underline{\beta_1 = -63.9^\circ}}$$

$$\therefore \underline{\underline{\beta_2 = -33.9^\circ}} \quad (\text{because } 30^\circ \text{ turning})$$

$$\tan \alpha_2 = \frac{u - V_x \tan \beta_2}{V_x} = \frac{320}{144} - \tan 33.9^\circ$$

$$\rightarrow \underline{\underline{\alpha_2 = +57.15^\circ}}$$

$$\Delta h_{\text{stage}} = u \Delta V_\theta$$

$$= 320 \times 144 (\tan 63.9^\circ - \tan 33.9^\circ)$$

$$= \underline{\underline{63.1 \text{ KJ/Kg}}}$$

Q

(ii)

$$\begin{aligned}\Delta h_{\text{stator}} &= \frac{1}{2}(V_2^2 - V_3^2) \\ &= \frac{1}{2} 144^2 (\tan^2 57.15^\circ - \tan^2 10^\circ) \\ &= 24.55 \text{ KJ/Kg.}\end{aligned}$$

$$\text{Reaction} = 1 - \frac{\Delta h_{\text{stat}}}{\Delta h_{\text{stage}}}$$

$$= 1 - \frac{24.55}{63.1} = \underline{\underline{61.1\%}}$$

Q7 a) Proof - see end of Q.
Radial equilibrium

$$\frac{dV}{dy} = -\frac{V}{r_c}$$

Approximate by $V_{i+1} = V_i - \frac{\Delta y V_i}{r_{ci}}$

$$\text{Taylor Series } V_{i+1} = V_i + \frac{\partial V}{\partial y} \Delta y + \frac{1}{2} \frac{\partial^2 V}{\partial y^2} \Delta y^2 + \frac{1}{6} \frac{\partial^3 V}{\partial y^3} \Delta y^3 + O(\Delta y)^4$$

$$\Rightarrow \frac{\partial V}{\partial y} = \frac{V_{i+1} - V_i}{\Delta y} - \frac{1}{2} \frac{\partial^2 V}{\partial y^2} \Delta y - \frac{1}{6} \frac{\partial^3 V}{\partial y^3} \Delta y^2 + O(\Delta y)^3$$

The approximation used is the first term on the RHS and so the largest term neglected is $O(\Delta y)$ - the method is 1st order accurate.

The truncation error is $\frac{1}{2} \frac{\partial^2 V}{\partial y^2} \Delta y$ which can be written as $-\frac{\partial V}{\partial y} \frac{1}{2r_c} = +\frac{V}{2r_c^2} \Delta y$ if r_c is constant.

b) Let $V_i = \bar{V}_i + V'_i$, where \bar{V}_i is the correct value

$$\rightarrow V_{i+1} = \bar{V}_i + V'_i - \frac{\bar{V}_i + V'_i}{r_{ci}} \Delta y$$

$$\rightarrow V_{i+1} = \left[\bar{V}_i - \frac{\bar{V}_i \Delta y}{r_{ci}} \right] + V'_i \left[1 - \frac{\Delta y}{r_{ci}} \right]$$

so an error $V'_i \rightarrow$ an error $V'_i \left[1 - \frac{\Delta y}{r_c} \right]$ at point $i+1$.

Q
cont

For stability the numerical value of the error at $i+1$ must be less than that at i , i.e. $\left|1 - \frac{\Delta y}{r_c}\right| < 1$ 2

$$\Rightarrow \underline{\underline{\frac{\Delta y}{r_c} < 2}} \quad \text{for stability} \quad 2$$

c)

Use $\frac{V_{i+1} - V_i}{\Delta y} = -\frac{(V_i + V_{i+1})}{2r_c}$ because $r_c = \text{const}$

$$V_{i+1} \left(1 + \frac{\Delta y}{2r_c}\right) = V_i \left(1 - \frac{\Delta y}{2r_c}\right)$$

$$\text{Let } \frac{\Delta y}{2r_c} = f$$

$$V_{i+1} = V_i \left(\frac{1-f}{1+f}\right)$$

$$= V_i (1-f)(1-f+f^2-f^3+\dots)$$

$$= V_i (1-f+f^2-f^3-f+f^2-f^3+\dots)$$

$$= V_i (1-2f+2f^2-2f^3+\dots) \quad 3$$

and $\frac{dV}{dy} = -\frac{V}{r_c} = -\frac{2fV}{\Delta y}$

$$\frac{d^2V}{dy^2} = +\frac{V}{r_c^2} = +\frac{4f^2}{\Delta y^2} \cdot V$$

$$\frac{d^3V}{dy^3} = -\frac{V}{r_c^3} = -\frac{8f^3}{\Delta y^3} \cdot V$$

Substituting for f, f^2, f^3, \dots in the above series

Q7
cont

$$V_{i+1} = V_i + \frac{dV}{dy} \Delta y + \frac{1}{2} \frac{d^2V}{dy^2} \Delta y^2 + \frac{1}{4} \frac{d^3V}{dy^3} \Delta y^3 + \dots$$

Compare this with the Taylor series - the 1st two terms are the same and the error in the $\frac{d^3V}{dy^3}$ term is

$$\left(\frac{1}{6} - \frac{1}{4}\right) \frac{d^3V}{dy^3} \Delta y^3$$

So the method is second order accurate and the truncation error is $-\frac{1}{12} \frac{d^3V}{dy^3} \Delta y^2$

Q7

1st part - prove $\frac{dV}{dy} = -\frac{V}{r_c}$

Radial equilibrium $\frac{1}{\rho} \frac{\partial P}{\partial y} = +\frac{V^2}{r_c}$

$$Tds = dh - \frac{1}{\rho} dP = dh_0 - v dv - \frac{1}{\rho} dP$$

$$S = \text{const}, h_0 = \text{const}$$

$$\rightarrow \frac{1}{\rho} dP = -v dv$$

$$\text{So R.E. eqn becomes } -v \frac{dv}{dy} = \frac{V^2}{r_c}$$

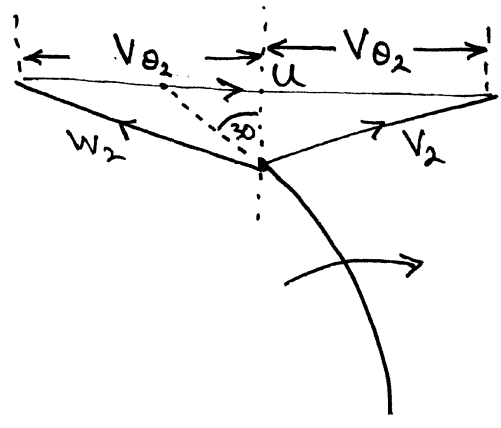
$$\text{or } \underline{\underline{\frac{dV}{dy} = -\frac{V}{r_c}}}$$

Note

It is not correct to just quote the Euler eqn $\therefore dP = -\rho v dv$ as this is along a streamline and we need the pressure gradient \perp to a streamline.

Q8

a)



(i)

$$\begin{aligned} V_{\theta 2, I} &= V_{r2} \tan 30^\circ + U_2 \\ &= -160 \tan 30^\circ + 380 \\ &= 287.6 \text{ m/s.} \end{aligned}$$

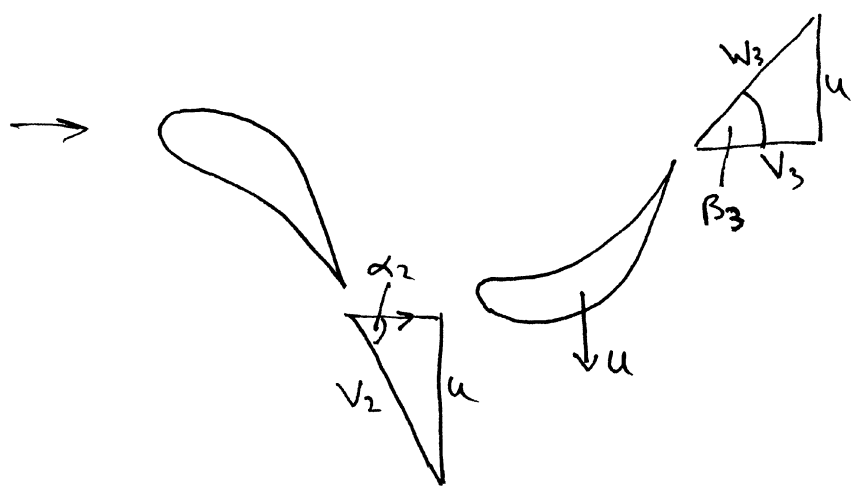
$$V_{\theta 2} = \sigma V_{\theta 2, I} = 0.88 \times 287.6 = \underline{\underline{253.1 \text{ m/sec.}}}$$

(ii)

$$\Delta h_o = U_2 V_{\theta 2}$$

$$\text{Power} = \dot{m} \Delta h_o = 2 \times 380 \times 253.1 = \underline{\underline{192.4 \text{ kW}}}$$

b)



(i)

$\dot{m} \Delta h_o = \text{same as compressor.}$

$$\begin{aligned} \rightarrow U_2 V_{\theta 2} &= 192.4 / 2 \times 10^3 & \left. \begin{array}{l} \text{For } M_2: \\ V_2 = \sqrt{V_{\theta 2}^2 + V_x^2} = 324.5 \text{ m/s} \end{array} \right\} \\ \rightarrow V_{\theta 2} &= \underline{\underline{310.3 \text{ m/sec}}} \\ \rightarrow \alpha_2 &= \tan^{-1} \frac{310.3}{95} = \underline{\underline{73^\circ}} & \left. \begin{array}{l} \frac{V_2}{\sqrt{c_p T_{02}}} = 0.3086 \\ \rightarrow \underline{\underline{M_2 = 0.5}} \end{array} \right\} \\ \Delta h_o / U^2 &= \frac{V_{\theta 2}}{U} = \underline{\underline{1.0}} \end{aligned}$$

Q8
cont

(ii)

$$T_{03} - T_{01} = \frac{\Delta h_0}{C_p} = \frac{192.4 \times 10^3}{2 \times 1005} = 95.72 \text{ K.}$$

$$\Delta T_{03,15} = \frac{1}{\eta_{\text{TT}}} \Delta T_0 = 112.61 \text{ K.}$$

$$T_{03,15} = 1100 - 112.61 = 987.38 \text{ K.}$$

$$\frac{P_{03}}{P_{01}} = \left(\frac{T_{03,15}}{T_{01}} \right)^{\frac{\gamma}{\gamma-1}} = 0.685$$

$$P_{01} = 4 \rightarrow P_{03} = \underline{\underline{2.741 \text{ bar.}}}$$

$$T_3 = T_{03} - \frac{1}{2} \times 95^2 / C_p = 999.79 \text{ K}$$

$$\frac{P_3}{P_{03}} = \left(\frac{T_3}{T_{03}} \right)^{\frac{\gamma}{\gamma-1}} = \left(\frac{999.79}{1004.28} \right)^{3.5} = 0.9844$$

$$\rightarrow P_3 = \underline{\underline{2.698 \text{ bar.}}}$$

(c)

See lecture notes.