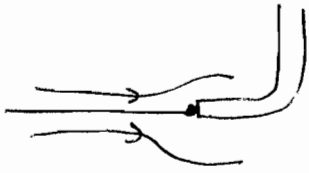


Model Solutions 3A3 2006  
Dr R J Miller

**PART IIA 2006**  
**3A3: Fluid mechanics II (double module)**  
*Principal Assessor: Dr R Miller*

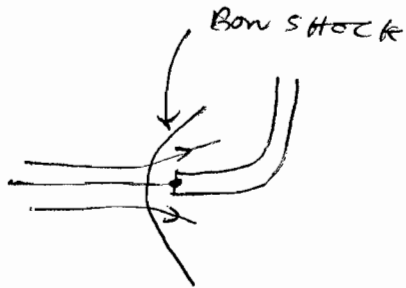
*Datasheet: Compressible Flow Data Book*

1a



SUBSONIC

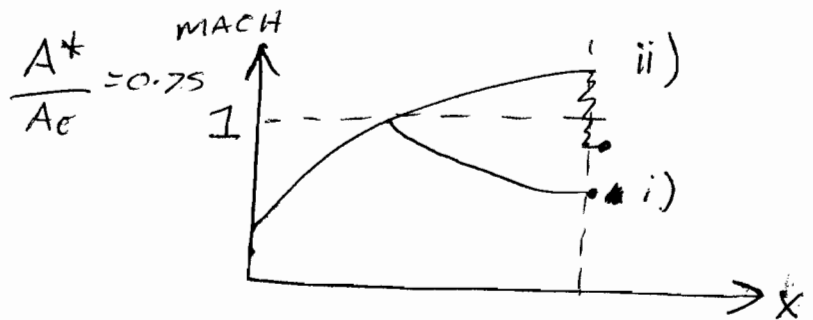
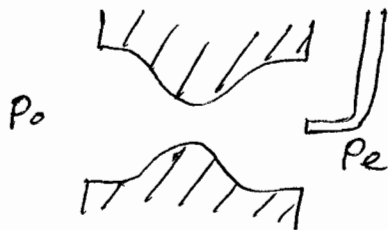
$P_0$  CONSTANT ALONG STREAMLINE



SUPERSONIC

$P_0$  DROP ACROSS SHOCK DEPENDANT ON UPSTREAM MACH NUMBER

B



i)  $M=1$  AT THROAT

$$\frac{m\sqrt{\rho T_0}}{A^* P_0} = 1.281$$

AT EXIT

$$\frac{m\sqrt{\rho T_0}}{A_e P_0} = 1.281 \times \frac{A^*}{A_e} = 0.9607$$

CUED MACH = 0.503

OR MACH = 1.696

MACH 0.503

MACH 1.696

WITHOUT SHOCK AT EXIT  $\frac{P_e}{P_0} = 0.2067$

NORMAL SHOCK  $\frac{P_s}{P} = 3.1655$

$$\frac{P_e}{P_0} = 0.2067 \times 3.1655 = 0.6543$$

$$\frac{P_{0s}}{P} = 0.8575 = \frac{P_{0PITOT}}{P_0}$$

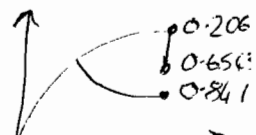
MACH 0.503

$$\frac{P_e}{P_0} = 0.841$$

$$\frac{P_{0PITOT}}{P_0} = 1$$

CASE ii) PITOT MEASURES 85.8% OF  $P_0$

CASE i) PITOT MEASURES 100% OF  $P_0$



①  $\frac{P_E}{P_0} = 0.75$



NEED TO CALCULATE  $\Delta P_0$  SHOCK  
SO NEED SHOCK STRENGTH

①  $\frac{P_{0s}}{P_0} = \frac{P_{0E}}{P_0} = \frac{\frac{m \sqrt{C_p T_0}}{A^* P_0} \times \frac{A_E P_{0E}}{m \sqrt{C_p T_0}} \times \frac{A}{A}}{A^* P_0}$

↑  
NEED TO  
KNOW  
MACH EXIT

NEED MACH No AT EXIT

$\frac{m \sqrt{C_p T_0}}{A_E P_E} = \frac{m \sqrt{C_p T_0}}{A^* P_0} \times \frac{A^*}{A_E} \times \frac{P_0}{P_E}$

$= 1.281 \times 0.75 \times \frac{1}{0.75} = 1.281$

CUED MACH EXIT = 0.562

CUED  $\frac{A_E P_{0E}}{m \sqrt{C_p T_0}} = 1.034$

FROM ①  $\frac{P_{0s}}{P_0} = 1.281 \times \frac{1}{1.034} \times 0.75 = 0.93$

FLOW SUBSONIC AT EXIT SO  $\frac{P_{0TOT}}{P_0} = 0.93$

② FROM  $\frac{P_E}{P_0} = 1 \rightarrow 0.84$

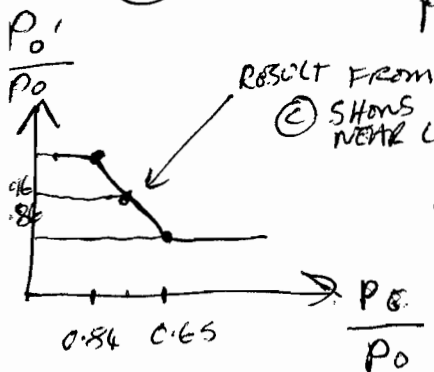
EXIT SUBSONIC SO

$\frac{P_{0TOT}}{P_0} = 1$

$\frac{P_E}{P_0} = 0.84 \rightarrow 0.65$

$\frac{P_{0TOT}}{P_0}$  DROPS TO 0.86

THEN  $P_{0TOT}$  FROZEN BECAUSE UPSTREAM MACH CONSTANT



2a

$$\frac{P_o}{P_E} = 1.25$$

$$\frac{P_E}{P_o} = 0.8$$

$$M_1 = 0.572 \text{ CUED}$$

①



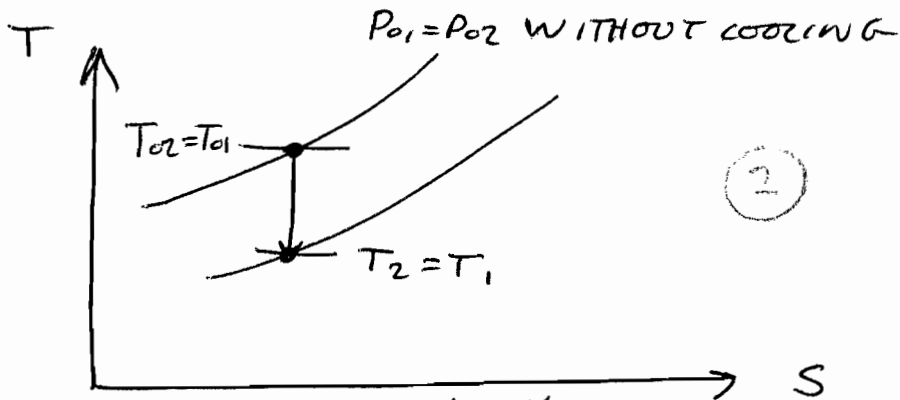
$$M_2 < M_1$$

SUBSONIC FLOW COOLED  
DROPS IN MACH NO.  
SO COOLING OF PIPE  
DROPS MACH NUMBER.

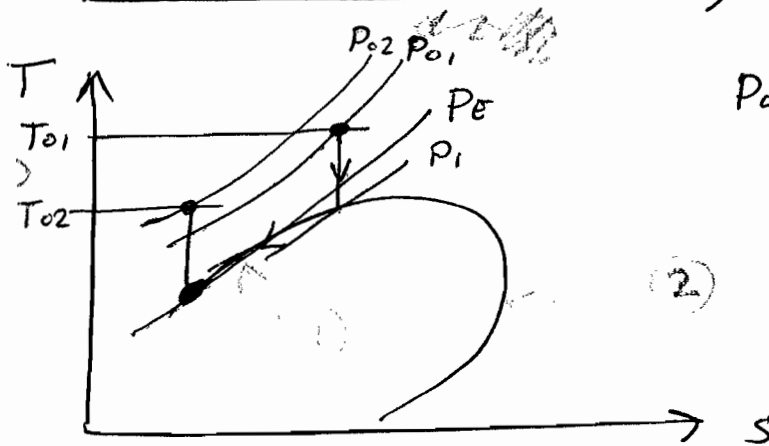
②

③

b



②

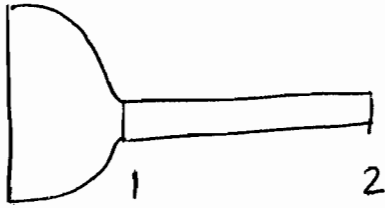


P0 RISES WITH COOLING

②

⑥

20



$$\frac{T_{02}}{T_{01}} = 0.85$$

$$M_2 = 0.572$$

AT ②  $\frac{F}{\dot{m} \sqrt{T_{02} C_p}} = 1.11$

F CONSTANT BECAUSE NO FRICTION

$$\frac{F}{\dot{m} \sqrt{T_{01} C_p}} = 1.11 \times \sqrt{\frac{T_{02}}{T_{01}}} = 1.11 \times \sqrt{0.85} = 1.023$$

$$M_1 = \underline{\underline{0.74}}$$

$$\frac{\dot{m} \sqrt{C_p T_{01}}}{A P_{01}} = 1.199$$

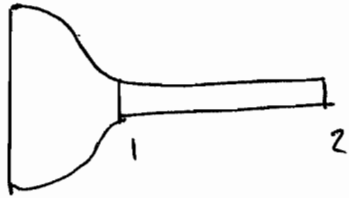
$$\frac{\dot{m} \sqrt{C_p T_{02}}}{A P_{02}} = 1.023$$

$$\Pi m_1 = \Pi m_2 \times \frac{P_{02}}{P_{01}} \times \sqrt{\frac{T_{01}}{T_{02}}}$$

$$\frac{P_{01}}{P_{02}} = \frac{\Pi m_2}{\Pi m_1} \times \sqrt{\frac{T_{01}}{T_{02}}} = \frac{1.023}{1.199} \times \sqrt{0.85} = 1.176$$

$$\underline{\underline{P_{01} = 1.17 \times P_{ATMOS}}}$$

(2) (d)



$$M_2 = 0.572$$

$$\frac{\dot{m} \sqrt{C_p T_{02}}}{A P_2} = 1.30$$

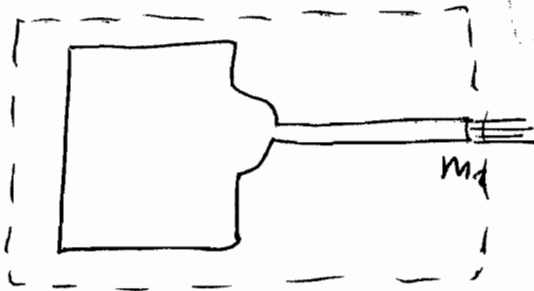
$T_0$  CHANGES WITH COOLING

~~$$\frac{\dot{m} \sqrt{C_p T_{02}}}{A P_2} = 1.30$$~~

$$(\dot{m} \sqrt{T_{02}})_{\text{COOLED}} = (\dot{m} \sqrt{T_{02}})_{\text{UNCOOLED}}$$

$$\frac{\dot{m}_{\text{UNCOOLED}}}{\dot{m}_{\text{COOLED}}} = \sqrt{\frac{T_{02 \text{ COOLED}}}{T_{02 \text{ UNCOOLED}}}} = \sqrt{\frac{T_{02}}{T_{01}}}$$

8.5% CHANGE = 0.9220 (3)



$$\text{THRUST} = F - A P_a$$

$$F = \frac{\dot{m} \sqrt{C_p T_{02}}}{M_2}$$

$$\dot{m} \sqrt{T_{02}} = \text{CONSTANT WHEN COOLED} \quad (2)$$

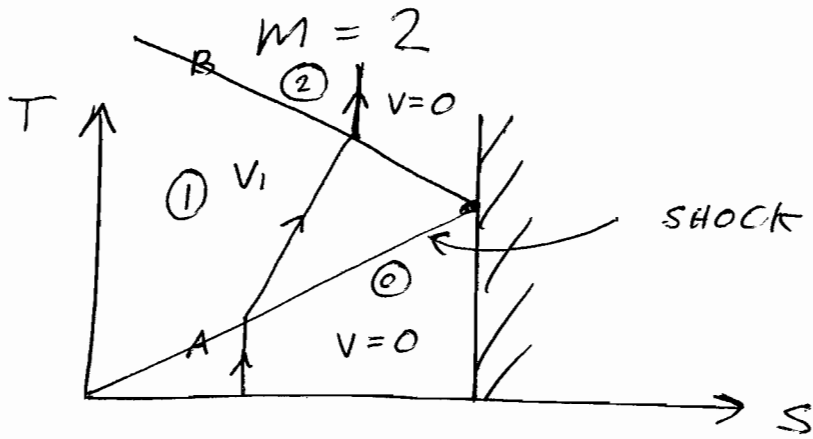
SO  $F_2$  CONSTANT WHEN COOLED

SO THRUST SAME FOR BOTH CASES.

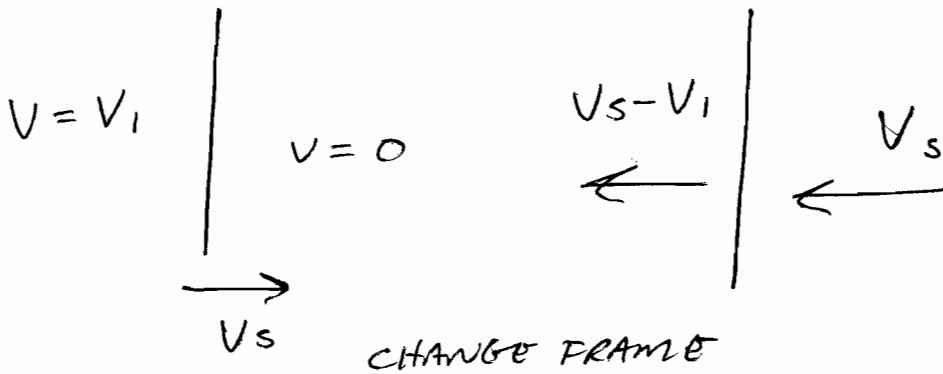
(5)

3A

$$\frac{P_s}{P} = 4.5 \quad \text{CUBED}$$



B



$$\rho_0 V_s = (V_s - V_1) \rho_1 \quad \text{CONTINUITY}$$

$$\frac{\rho_0}{\rho_1} = \frac{V_s - V_1}{V_s} = \frac{\rho_0 T_1}{\rho_1 T_0} = \frac{1}{4.5} \times 1.6875 = 0.375$$

$$\therefore V_s - V_1 = 0.375 V_s$$

$$V_1 = V_s - 0.375 V_s \quad \text{①}$$

MACH 2  $V_s = 2 a_0$

SUB INTO ①

$$V_1 = (1 - 0.375) \times 2 a_0 = \underline{1.25 a_0}$$

CUBED  $M=2$   $\frac{T_s}{T} = 1.6875$   $a_1 = a_0 \times \sqrt{1.6875}$   
 $a_1 = 1.299 a_0$

3c

$$\frac{\rho}{\rho_s} = \frac{2}{\gamma+1} \times \frac{1}{M_1^2} + \frac{\gamma-1}{\gamma+1}$$

FLOW STOPS AFTER SHOCK



CHANGE FRAME

$$\rho_s V_{SB} = \rho (V_1 + V_{SB})$$

$$\frac{\rho}{\rho_s} = \frac{V_{SB}}{V_1 + V_{SB}} = \left(\frac{2}{\gamma+1}\right) \frac{1}{M_{SB}^2} + \left(\frac{\gamma-1}{\gamma+1}\right)$$

$M_{SB}$  ~~is the Mach number of the shock~~ ~~is the Mach number of the shock~~ IS MACH RELATIVE UPSTREAM TO THE REFLECTED SHOCK

$$\frac{M_{SB} - V_1/a_0}{M_{SB}} = \left(\frac{2}{\gamma+1}\right) \frac{1}{M_{SB}^2} + \left(\frac{\gamma-1}{\gamma+1}\right)$$

$$\frac{2}{\gamma+1} M_{SB}^2 - \frac{V_1}{a_0} M_{SB} - \frac{2}{\gamma+1} = 0$$

$$M_{SB} = \left( \frac{V_1}{a_0} \pm \sqrt{\frac{V_1^2}{a_0^2} + \frac{16}{(\gamma+1)^2}} \right) / \frac{4}{\gamma+1}$$

FROM (b)

$$\frac{V_1}{a_0} = 0.9623$$

$$= 0.9623 \pm \sqrt{(0.9623)^2 + \frac{16}{(2.4)^2}}$$

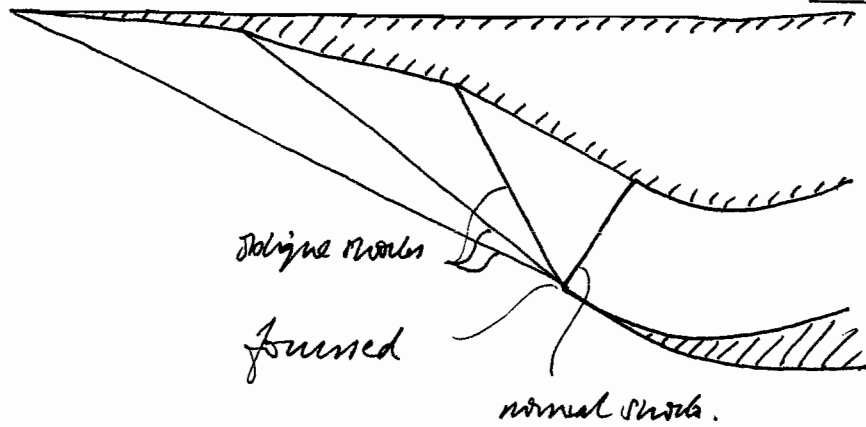
$$M_{SB} = \frac{4}{\gamma+1} = 1.73$$

SHOCK STRENGTH = 1.73



4)

a)



From Tables:

b)

	$\theta$	$\beta$	$M_2$	$P_0/P$
1	$\theta$	33.8	1.90	0.990
2	$\theta$	39.3	1.62	0.993
3	$\theta$	47.3	1.34	0.994
4			0.77	0.972

Mach no. downstream of normal shock = 0.77

c)

Relate oblique shock strength to equivalent normal shock

with upstream Mach no =  $M \sin \beta$

and relate to  $P_{0\infty}$  via  $P_0 = P \left[ 1 + \frac{1}{2}(\gamma-1)M^2 \right]^{\frac{\gamma}{\gamma-1}}$

to give values in table above:

$$\therefore \frac{P_{07}}{P_{0\infty}} = 0.990 \times 0.993 \times 0.994 \times 0.972 = 0.95$$

d)

Remove final oblique & normal & replace with a normal with

upstream  $M = 1.62$

$$\therefore \frac{P_{07}}{P_{0\infty}} = 0.990 \times 0.993 \times 0.889 = 0.87$$

(4e)

$$M_\infty = 2$$

SAS - 2D COMPRESSIBLE

Flow - 2005 - 2006

J.P. JARRETT

From tables

	$\delta$	$\beta$	$M_2$	$P_0/P_\infty$
1	$\delta$	37.2	1.71	0.993
2	$\delta$	44.2	1.44	0.990
3				0.947

$$\Rightarrow \frac{P_3}{P_{0,2}} = 0.993 \times 0.990 \times 0.947 = 0.93$$

The significant loss in pressure recovery resulting from simplifying the intake design is almost entirely regained by a relatively modest reduction in flight speed.

5) Flow is irrotational

$$V = (u, v)$$

SAB-20 COMPRESSIBLE  
FLOW 2005-2006  
J. P. JARRETT

$$\text{Mass: } \nabla \cdot (\rho V) = 0 \Rightarrow \nabla \cdot V + \frac{1}{\rho} V \cdot \nabla \rho = 0$$

$$\text{Energy: } \text{const} = h_0 = c_p T + \frac{1}{2} (u^2 + v^2) = \frac{a^2}{\gamma - 1} + \frac{1}{2} (u^2 + v^2)$$

$$\text{Flow is isentropic: } p = k \rho^\gamma \Rightarrow dp = \gamma k \rho^{\gamma-1} d\rho \Rightarrow \nabla p = a^2 \nabla \rho$$

$$\text{Consider Euler (momentum): } -\frac{1}{\rho} \nabla p = V \cdot \nabla V$$

$$\text{Eliminate } \nabla p \text{ \& } \Delta \rho \Rightarrow V \cdot V = -\frac{1}{\rho} V \cdot \nabla \rho = -\frac{1}{\rho a^2} V \cdot \nabla p = \frac{1}{a^2} V \cdot (V \cdot \nabla V)$$

$$\text{Rearranging gives } a^2 \nabla \cdot V - V \cdot (V \cdot \nabla V) = 0.$$

In terms of components  $V = (u, v)$  in  $x$  &  $y$  dir'n.

$$a^2 \left( \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} \right) - [u \underline{e}_x + v \underline{e}_y] \cdot \left[ \left( u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} \right) \underline{e}_x + \left( u \frac{\partial v}{\partial x} + v \frac{\partial v}{\partial y} \right) \underline{e}_y \right] = 0$$

$$a^2 \left( \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} \right) - u \left( u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} \right) - v \left( u \frac{\partial v}{\partial x} + v \frac{\partial v}{\partial y} \right) = 0$$

$$(a^2 - u) \frac{\partial u}{\partial x} - uv \frac{\partial u}{\partial y} - vu \frac{\partial v}{\partial x} + (a^2 - v^2) \frac{\partial v}{\partial y} = 0$$

$$\text{Flow is irrotational } \therefore \nabla \times V = 0 \Rightarrow \frac{\partial u}{\partial y} = \frac{\partial v}{\partial x}$$

$$\therefore (a^2 - u^2) \frac{\partial u}{\partial x} - 2uv \frac{\partial u}{\partial y} + (a^2 - v^2) \frac{\partial v}{\partial y} = 0$$

2 cont

3/13-23 COMPRESSIBLE

FEB 2005-2006

J.P. JACKETT

$$\text{Ans: } V = \left( u_\infty + \frac{\partial \phi}{\partial x}, \frac{\partial \phi}{\partial y} \right)$$

$$\left[ a^2 - \left( u_\infty + \frac{\partial \phi}{\partial x} \right)^2 \right] \frac{\partial^2 \phi}{\partial x^2} - 2 \left[ u_\infty + \frac{\partial \phi}{\partial x} \right] \frac{\partial \phi}{\partial y} \frac{\partial^2 \phi}{\partial x \partial y} + \left[ a^2 - \left( \frac{\partial \phi}{\partial y} \right)^2 \right] \frac{\partial^2 \phi}{\partial y^2} = 0$$

$$\frac{\partial \phi}{\partial x}, \frac{\partial \phi}{\partial y} \ll u_\infty$$

$$\therefore \text{Simplify to } \left[ a_\infty^2 - u_\infty^2 \right] \frac{\partial^2 \phi}{\partial x^2} + a_\infty^2 \left( \frac{\partial^2 \phi}{\partial y^2} \right) = 0$$

$$\Rightarrow \beta^2 \frac{\partial^2 \phi}{\partial x^2} + \frac{\partial^2 \phi}{\partial y^2} = 0$$

$$\text{where } \beta = \sqrt{1 - M_\infty^2}$$

This is the term which enables compressible  $C_p$ ,  $C_v$  &  $C_m$  to be evaluated from the incompressible equivalents via the Prandtl-Glauert compressibility correction.

Num 6(a) Hyperbolic equations are 'wave-like' and solution information travels along specific directions with characteristic speeds. Upwind differences are used for spatial derivatives and use values at the current position and upstream (in the characteristic direction). When combined with forward time differencing, they preserve this information property - i.e. that information can only travel in the downstream characteristic direction.

$$(b) \quad u_i^{n+1} = u_i^n + \Delta t \frac{\partial u}{\partial t} + \frac{\Delta t^2}{2!} \frac{\partial^2 u}{\partial t^2} + O(\Delta t^3)$$

[All denios evaluated at  $i, n$ ]

$$u_{i-1}^n = u_i^n - \Delta x \frac{\partial u}{\partial x} + \frac{\Delta x^2}{2!} \frac{\partial^2 u}{\partial x^2} + O(\Delta x^3)$$

Substituting into (1)

$$\Rightarrow u_i^{n+1} = u_i^n + \Delta t \frac{\partial u}{\partial t} + \frac{\Delta t^2}{2!} \frac{\partial^2 u}{\partial t^2} + O(\Delta t^3)$$

$$= u_i^n - c \left( u_i^n - u_{i-1}^n + \Delta x \frac{\partial u}{\partial x} - \frac{\Delta x^2}{2!} \frac{\partial^2 u}{\partial x^2} + O(\Delta x^3) \right)$$

$$\Rightarrow \frac{\partial u}{\partial t} = -\frac{\Delta t}{2} \frac{\partial^2 u}{\partial t^2} + O(\Delta t^2) - \frac{A}{\Delta x} \left[ \Delta x \frac{\partial u}{\partial x} - \frac{\Delta x^2}{2} \frac{\partial^2 u}{\partial x^2} + O(\Delta x^3) \right]$$

$$\Rightarrow \frac{\partial u}{\partial t} + A \frac{\partial u}{\partial x} = -\frac{\Delta t}{2} \frac{\partial^2 u}{\partial t^2} + \frac{A \Delta x}{2} \frac{\partial^2 u}{\partial x^2} + O(\Delta t^2, \Delta x^2)$$

$$= -\frac{A^2 \Delta t}{2} \frac{\partial^2 u}{\partial x^2} + \frac{A \Delta x}{2} \frac{\partial^2 u}{\partial x^2} + O(\Delta t^2, \Delta x^2)$$

using hint.

$$= \frac{A \Delta x}{2} [1 - c] \frac{\partial^2 u}{\partial x^2} + O(\Delta t^2, \Delta x^2)$$

i.e.  $\alpha = \frac{A \Delta x}{2} (1 - c)$  & scheme is 1st order  
unless  $c=1$  when 2nd order

⑥ (c) (iii) Scheme is unstable if perturbation at  $n+1$  is bigger (in magnitude) than at  $n$ .

For a perturbation of the form  $u_i^n = (-1)^i \epsilon$  ( $\Rightarrow u_{i-1}^n = -u_i^n$ )

$$u_i^{n+1} = \epsilon(-1)^i - c \epsilon(-1)^i [1+1]$$

$$\therefore \left| \frac{u_i^{n+1}}{\epsilon} \right| = |1-2c|$$

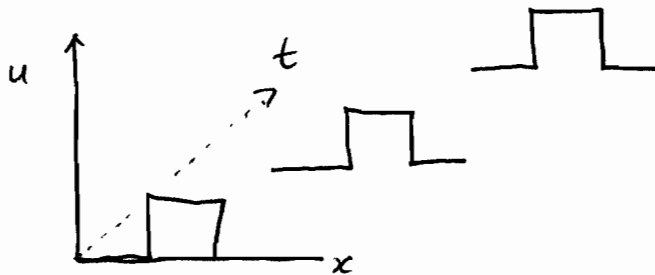
Stable only if  $|1-2c| \leq 1$  i.e.  $-1 \leq 1-2c \leq 1$

$$\Rightarrow \underline{0 \leq c \leq 1}$$

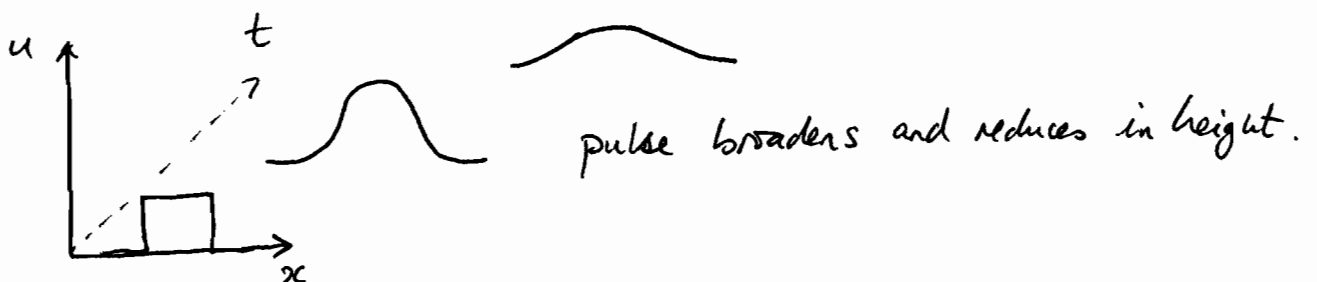
~~(c)~~ (i)  $c=1$   $\propto \frac{\partial^2 u}{\partial x^2}$  is a diffusion term

and  $\alpha=0$  for  $c=1$

$\therefore$  Very little spread/reduction [in fact difference scheme is exact]



(ii)  $c=1/2$  Dominant error is diffusion



pulse broadens and reduces in height.

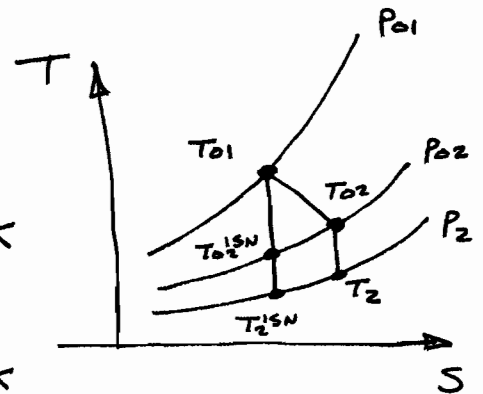
7

HALF QUESTION

(a) POWER =  $\dot{m} \Delta h_o$

$$\Rightarrow \Delta T_o = \frac{\text{POWER}}{\dot{m} c_p} = \frac{15 \times 10^6}{50 \times 1005} = 298.5 \text{ K}$$

$$T_{o2} = T_{o1} - \Delta T_o = 900 - 298.5 = \underline{601.5 \text{ K}}$$



$$P_{o2} = P_2 \left(1 + \frac{\gamma-1}{2} M_2^2\right)^{\frac{\gamma}{\gamma-1}} = 1.0 \left(1 + 0.2 \cdot 0.7^2\right)^{3.5} = \underline{1.387 \text{ bar}}$$

TOTAL - TOTAL

$$\eta_{tt} = \frac{T_{o1} - T_{o2}}{T_{o1} - T_{o2}^{ISN}}$$

$$T_{o2}^{ISN} = T_{o1} \left(\frac{P_{o2}}{P_{o1}}\right)^{\frac{\gamma-1}{\gamma}} = 900 \left(\frac{1.387}{8.0}\right)^{1/3.5} = 545.5 \text{ K}$$

$$\eta_{tt} = \frac{900 - 601.5}{900 - 545.5} = 0.842 \quad \eta_{tt} = \underline{\underline{84.2\%}}$$

TOTAL - STATIC

$$\eta_{ts} = \frac{T_{o1} - T_{o2}}{T_{o1} - T_2^{ISN}}$$

$$T_2^{ISN} = T_{o1} \left(\frac{P_2}{P_{o1}}\right)^{\frac{\gamma-1}{\gamma}} = 900 \left(\frac{1.0}{8.0}\right)^{1/3.5} = 496.8 \text{ K}$$

$$\eta_{ts} = \frac{900 - 601.5}{900 - 496.8} = 0.740 \quad \eta_{ts} = \underline{\underline{74.0\%}}$$

(b)  $\eta_{tt}$  - ASSUMES EXIT KE USEFUL

$\eta_{ts}$  - REFLECTS CASE WHEN EXIT KE IS WASTED.

IMPROVE BY DROPPING  $M_2$  - SAY EXIT DIFFUSER.

7 ~~Hom 22~~ (b)

(i) Conservation form is

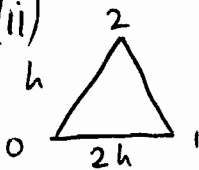
$$\frac{\partial U}{\partial t} + \frac{\partial F_x}{\partial x} + \frac{\partial F_y}{\partial y} + \frac{\partial F_z}{\partial z} = 0$$

where  $\underline{U} = \begin{pmatrix} \rho v_x \\ \rho v_y \\ \vdots \end{pmatrix}$  and  $F_x, F_y, F_z$  represent the flux of a quantity.

It is called conservation form, because, when integrated over a control volume, the rate of change of stuff in the control volume is related directly to the flux across the surrounding surface.

Numerical schemes based on this formulation will conserve mass, momentum and energy for steady solutions, achieve the correct strength of any shocks, etc.

(ii)



$$\text{Area} \frac{d\rho_{cell}}{dt} = - \oint_C \rho \underline{V} \cdot \underline{n} \, dl \quad \text{using Gauss' theorem}$$

$$\int_A \frac{\partial \rho}{\partial t} dA = - \int_A \nabla \cdot (\rho \underline{V}) dA = - \oint_C (\rho v_x) dy + \oint_C \rho v_y dx$$

Using the trapezium rule

$$\begin{aligned} \text{Area} = \frac{1}{2} \times 2h \times h & \quad \frac{h^2}{dt} \frac{d\rho_{cell}}{dt} = - \left( \frac{(\rho v_x)_1 + (\rho v_x)_0}{2} \times (0) - \frac{(\rho v_x)_2 + (\rho v_x)_1}{2} (-h) \right. \\ & \quad \left. - \frac{(\rho v_x)_0 + (\rho v_x)_2}{2} (-h) \right. \\ & \quad \left. + \frac{(\rho v_y)_1 + (\rho v_y)_0}{2} (2h) + \frac{(\rho v_y)_2 + (\rho v_y)_1}{2} (h) \right. \\ & \quad \left. + \frac{(\rho v_y)_0 + (\rho v_y)_2}{2} (-h) \right) \\ & = -h \left\{ \frac{(\rho v_x)_1 - (\rho v_x)_0}{2} + (\rho v_y)_2 - \frac{(\rho v_y)_1 + (\rho v_y)_0}{2} \right\} \end{aligned}$$



(a)  $U = r\omega = 0.3 \cdot \frac{2\pi \cdot 6500}{60} = \underline{204.2 \text{ m/s}}$

$u_1 = \phi \cdot U = 0.5 \times 204.2 = \underline{102.1 \text{ m/s}}$

$T_1 = T_{01} - u_1^2 / 2c_p = 288 - 102.1^2 / (2 \times 1005) = \underline{282.8 \text{ K}}$

$P_1 = P_{01} (T_1 / T_{01})^{3.5} = 1.0 \left( \frac{282.8}{288} \right)^{3.5} = \underline{0.9382 \text{ bar}}$

$\rho_1 = P_1 / RT_1 = \frac{0.9382 \times 10^5}{287 \times 282.8} = \underline{1.1560 \text{ kg/m}^3}$

$A_1 = \frac{\dot{m}}{\rho_1 u_1} = \frac{25}{1.156 \times 102.1} = \underline{0.2118 \text{ m}^2}$

$\Delta r = \frac{A_1}{2\pi r} = \frac{0.2118}{2\pi \cdot 0.3} = \underline{0.112 \text{ m}}$  (BLADE HEIGHT = ~~112~~ 112 mm)

(b)  $|\underline{u}_1^{REL}| = \sqrt{u_1^2 + U^2} = \sqrt{102.1^2 + 204.2^2} = \underline{228.3 \text{ m/s}}$



$T_{01}^{REL} = T_1 + |\underline{u}_1^{REL}|^2 / 2c_p = 282.8 + 228.3^2 / (2 \times 1005) = \underline{308.7 \text{ K}}$

$P_{01}^{REL} = P_1 \left( \frac{T_{01}^{REL}}{T_1} \right)^{3.5} = 0.9382 \left( \frac{308.7}{282.8} \right)^{3.5} = \underline{1.275 \text{ bar}}$

$\alpha_1^{rel} = \tan^{-1} \left( \tan \alpha_1 - \frac{1}{\phi} \right) = \tan^{-1} \left( 0 - \frac{1}{0.5} \right) = \underline{-63.4^\circ}$

(c)  $Y_p = \frac{P_{01}^{REL} - P_{02}^{REL}}{P_{01}^{REL} - P_1}$  (N.B. REL. QUANTITIES & FLOW AT FIXED RADIUS  $T_{02}^{REL} = T_{01}^{REL}$ )

$P_{02}^{REL} = P_{01}^{REL} - Y_p (P_{01}^{REL} - P_1) = 1.275 - 0.05 (1.275 - 0.9382)$

$\underline{P_{02}^{REL} = 1.258 \text{ bar}}$

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2/2

(C cont.)  $\frac{\dot{m} \sqrt{C_p T_{03}^{rel}}}{A \cos \alpha_{rel} P_{01}^{rel}} = f_n(M_{rel}) \quad A_2 = A_1$

$$\frac{\dot{m} \sqrt{C_p T_{02}^{rel}}}{A_2 \cos \alpha_2 P_{02}^{rel}} = \frac{25 \sqrt{1005 \cdot 308.7}}{0.2118 (\cos 50^\circ) 1.258 \times 10^5} = 0.8131$$

TABLES ( $\gamma = 1.4$ )  $M_2^{rel} = \underline{\underline{0.405}}$

$$P_2 = P_{02}^{rel} / \left(1 + \frac{\gamma-1}{2} M_2^{rel 2}\right)^{\gamma/\gamma-1} = \frac{1.258}{(1 + 0.2 \times 0.405^2)^{3.5}} = \underline{\underline{1.124 \text{ bar}}}$$

(d)  $V_2^{rel} = M_2^{rel} \sqrt{\gamma R T_2}$

$$T_2 = T_{02}^{rel} / \left(1 + \frac{\gamma-1}{2} M_2^{rel 2}\right) = \frac{308.7}{(1 + 0.2 \times 0.405^2)} = \underline{\underline{298.9 \text{ K}}}$$

$$V_2^{rel} = 0.405 \sqrt{1.4 \cdot 287 \cdot 298.9} = 140.4 \text{ m/s}$$

$$u_{\theta 2}^{rel} = V_2^{rel} \sin \alpha_2^{rel} = 140.4 \sin(-50^\circ) = \underline{\underline{-107.6 \text{ m/s}}}$$

$$u_{\theta 2} = u_{\theta 2}^{rel} + U = -107.6 + 204.2 = \underline{\underline{96.6 \text{ m/s}}}$$

$$\frac{\Delta h_0}{U^2} = \frac{U_2 u_{\theta 2} - U_1 u_{\theta 1}}{U^2} = \frac{u_{\theta 2}}{U} = \frac{96.6}{204.2} = \underline{\underline{0.473}}$$

WOULD NORMALLY EXPECT  $\Delta h_0/U^2 \sim 0.4$  to  $0.45$  SO THIS IS A CHALLENGING AERODYNAMIC DESIGN.

(e) CONSTANT BLADE HEIGHT MEANS  $U_x$  DECREASES SO SWIRL ANGLES BECOME HIGHER. BETTER TO DECREASE BLADE HEIGHT TO MAINTAIN CONSTANT AXIAL VELOCITY.

Answers to 3A3 2006

1. (b) (i) 0.84, 1, (ii) 0.65, 0.86.  
(c) 0.93.
2. (a) 0.572.  
(c) 0.74, 1.17.  
(d) 0.992.
3. (a) 2.  
(b)  $1.25a_0$ ,  $1.30a_0$ .  
(c) 1.73.
4. (b) 0.77.  
(c) 0.95.  
(d) 0.87.  
(e) 0.93.
7. (a) 1.39 bar, 84.2%, 74.0%.
8. (a) 0.112m.  
(b) 308.7k, 1.275bar,  $-63.4^\circ$   
(c) 1.258 bar, 1,124bar.  
(d) 0.473.