3D6 Environmental Geofechnics Coib 2008 Dr I thusyanthan

d Th

Let 'h' be height of capillary rise in a tube of diamete d'.

weight of water column =  $\frac{\pi d^2 \times h \times \delta w}{4}$ Let surface tension of water be 'T'.  $T \pi d = \frac{\pi d^2 h}{4} \delta w$ 

h = 4 T

[20X.

b) From table 1, typical pore size of silt = D10 = 0.01 mm

$$h = \frac{4 \times 7.3 \times 10^{-5}}{10 \times 0.01 \times 10^{3}}$$

h = 2,92 m

[10.7.]

c) Unit weight of Soil

Y = (G+ESR) 800

(1+E)

Fol dry ase Sq = 0: 8 = Gran

For saturated Care Sn=1

$$8 \text{ Sand} = \frac{(2.65 + 0.62)}{(1+0.62)} \times 10 = \frac{20.19}{(1+0.62)} \times 10 = \frac{20.19}{(1+0.62)} \times 10 = \frac{1}{20.19} \times 10^{-3}$$

[20%]

Dorcy's slow V= 0.05 cm/s = 5x10 m/s

V= Kdh

5x10-4 = 2.5x10-2 dh

 $dh = \frac{5 \times 10^{-4}}{2.5 \times 10^{-2}} \times 50$ ds = 50 m - L

CIONT

· . h. - h = 1m

Since ABB art same elevation. h, -h = Im

.. hy = 2.5+1.5 = 4m

ha = 4-1 = 3m , worter level in B will

be 1.5m bélow the top of sitt layer.

[10x]

Assumptions y Flow is laminor in sand (A+B)

2) Pressure head drop is linear

3, Flow in sand by unisorm & steady starte.

y Flow is parallel to A -B

I sortworked = 19.42 kN/m3 } from

Sortworked = 20.19 kN/m3 } port (b)

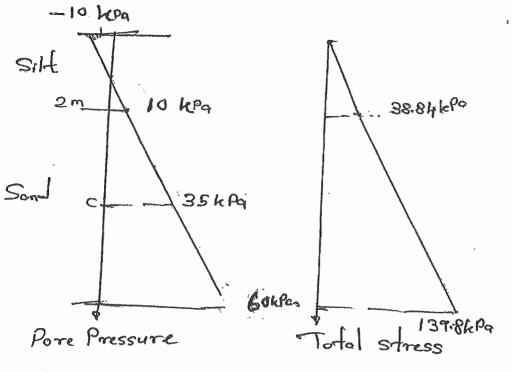
Sond Sortworked = 20.19 kN/m3

Total stress-based silf layer = 19.42x2 = 38.84 kPa Total stress - bose of sand layer= 38.84+20.19x5= 139.8 using AB as dotum.

 $5^{m}$ .B 5m. A Sand

h, = 4m, h, = 3m 1. he = 3.5 m

Since Mow is parallel to AB, xx is sand is a equiportential.



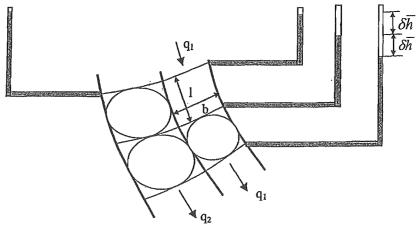
lokpa 28.84

Eddective Stress

Assume pore pressure variation linear in Silt loyer.

[30%]

2.a) Consider a set of flow lines and equi-potentials in the soil. From continuity, the volume flow rate within each flow tube must be constant.



Applying Darcy's law to the element of breadth b and length l:

$$v = K \cdot i_1 = K \frac{\delta \overline{h}}{l}$$

$$q_1 = A_1 \cdot v_1 = b \times 1 \times K \times \frac{\delta \overline{h}}{l}$$

$$= K \times \delta \overline{h}$$

For convenience a flow net of curvilinear squares is usually drawn with b=l, by adopting simple trail and error solutions. If the equi-potentials are drawn with equal drops in potential heads then  $\partial \bar{h} = \frac{\Delta \bar{h}}{N_h}$ , where  $\Delta \bar{h}$  is the total drop in the potential head along the flow tube from a source of water to a sink and  $N_h$  is the number of drops in potential. The flow rate per flow tube is:

$$q = K\delta \overline{h} = K \times \frac{\delta \overline{h}}{N_h}$$
 per tube.

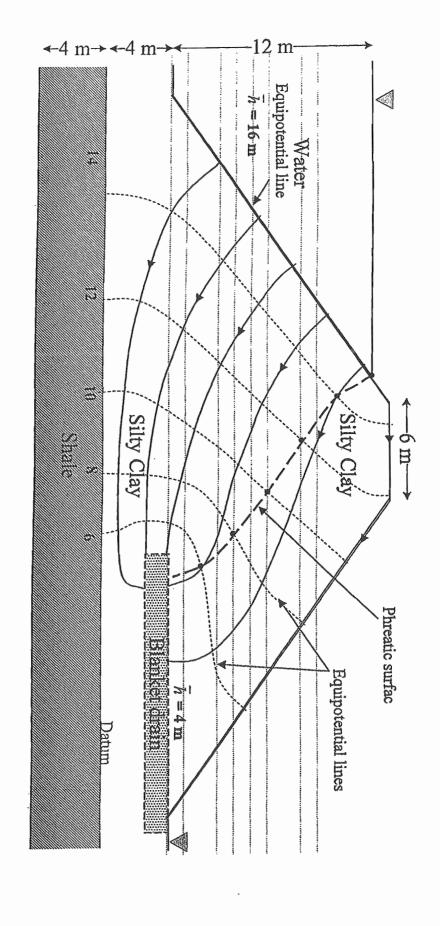
So a flow net of curvilinear squares will have constant potential differences and the same flow rate in each tube. Curvilinear squares have edges crossing at right angles, and an inscribing circle would just touch all four sides.

$$q = q_1 = q_2$$

If there are  $N_f$  flow tubes then the total flow quantity will be:

$$q = K\Delta \overline{h} \frac{N_f}{N_h}$$
 m<sup>3</sup>/s/m length

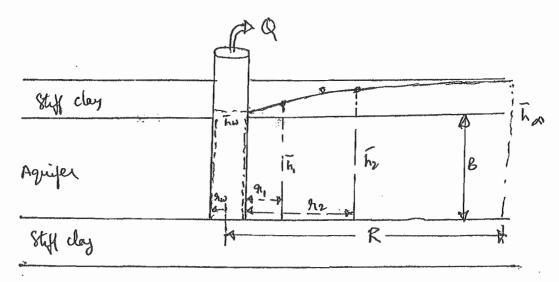
[20%]



2b) ii)  $9 = K \Delta h \frac{N_b}{N_h}$   $N_f = 6$   $N_h = 6$  from flownet.  $9 = 6.8 \times 10^{-6} \times 12 \times 6 = 8.16 \times 10^{-5} \, \text{m}^{3/s} / \text{m}$  $= 8.16 \, \text{m}^{3/s} / \text{m}$ . C

20) If the blanket drain is too long then the leakage rate through the down increases, decreasing its perform as an earthdam.

If the blanket drain is too short then the phreatic line exit through the downstream slope. If this hoppens then exotic of the downstream face can happen, eventually this may be to a celtostophic failure of the centh dawn. [2]



Rearranging 
$$d\bar{h} = \frac{Q}{2\pi b K} \frac{dx}{n}$$
  
Shigning  $h_{2} = \frac{Q}{2\pi b K} \frac{dx}{n}$   
 $h_{2} - h_{1} = \frac{Q}{2\pi b K} \ln \left(\frac{A_{2}}{9_{1}}\right)$ 

We have  $K = 5 \times 10^{-3} \text{ m/s}$   $9_1 = 20 \text{ m}$   $h_1 = 7 \text{ m}$  h = 6 m  $9_1 = 30 \text{ m}$   $h_2 = 7 \cdot 1 \text{ m}$ 

Q = 0.046488 m3/s ~ 46.5 lites/sec

130Y

b) Total draw down = ha-haeu

Potential head in the well Twell:  $Q = 0.0464 \text{ m}^3/\text{s}$   $9_{10} = 0.1 \text{ m}$ at  $9_1 = 20 \text{ m}$   $h_1 = 7 \text{ m}$ . b = 6 m.

$$7 - h_{\text{well}} = \frac{0.0464}{20.6 \times 5 \times 10^3} \times \ln \left[ \frac{20}{0.1} \right] = 1.304 \text{ m}$$

Radius of refluence R = 200m. The is the potential head at R. Q = 0.0464 m3/s R = 200 m at 8,=20m h=7m b=6m.  $h_{ch} - 7 = \frac{0.0464}{2\pi 6 \times 5 \times 10^{-3}} \times \ln \left[ \frac{200}{20} \right] = 0.568 \text{ m}$ ha = 7+0.568 = 7.568 m : Total draw down in the water table = 7.568 - 5.7 Dh = 1.868, m [204.] 30) Before the sheet pile wall is driven, the potential head at a distance of 10 m from the centre of the well.  $\overline{h}_{20} - \overline{h}_{10} = \frac{Q}{2\pi 6 \times 5 \times 10^{3}} \ln \left[ \frac{20}{10} \right] = \frac{0.0464}{2\pi 6 \times 5 \times 10^{3}} \ln 2$ 7- hio = 0.171 h10 = 6.83 m

Draw down at this point will

hos-his = 7.568 - 6.83

[Z Sheet pile would

Impermeable boundary

From Guage theory for wells,

on imaginary ab structure well present

of low from the sheef pile wall will model

well

Imaginary the unpermeable boundary andition

well

This will lead to dowship of the drawd

\[
\Delta = 2 \times 0.738 = 1.476. m

\]

The change in drawdown

[201]

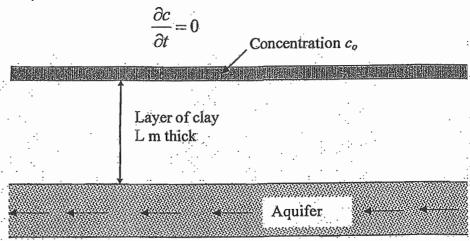
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= 0.738m

The governing equation is, as before:

$$\frac{\partial c}{\partial t} = D_l \frac{\partial^2 c}{\partial z^2} - v_f \frac{\partial c}{\partial z}$$

Consider an old landfill, leaking aqueous pollutant into the underlying clay layer. Pollutant has been leaking for a number of years an is assumed to have reached the steady state distribution  $t \rightarrow \infty$ , for which:



The advection-dispersion equation becomes:

$$D_{I} \frac{\partial^{2} c}{\partial z^{2}} = v_{f} \frac{\partial c}{\partial z}$$

and integrating once with respect z gives:

$$\frac{D_1}{v_f} \frac{\partial c}{\partial z} = c - P$$

where P is a constant, while integrating again gives:

$$\ln(c-P) = \frac{v_f z}{D_l} + \ln Q$$

where Q is also a constant. Rearranging gives:

$$c = P + Q \exp\left(\frac{v_f z}{D_l}\right)$$

which must satisfy the boundary conditions:

for 
$$z = 0$$
 
$$c = P + Q = c_o$$

for 
$$z = L$$
  $c = P + Q \exp\left(\frac{v_l L}{D_l}\right) = 0$   $\begin{bmatrix} c & \text{of } z = L \text{ con be} \\ \text{non 3 ero as well } \end{bmatrix}$ 

the solution of which gives:

$$P = \frac{-c_o \exp\left(\frac{v_f L}{D_l}\right)}{1 - \exp\left(\frac{v_f L}{D_l}\right)} \quad \text{and} \quad Q = \frac{c_o}{1 - \exp\left(\frac{v_f L}{D_l}\right)}$$

and therefore the steady state distribution is:

$$\frac{c}{c_o} = \frac{\exp\left(\frac{v_f z}{D_l}\right) - \exp\left(\frac{v_f L}{D_l}\right)}{1 - \exp\left(\frac{v_f L}{D_l}\right)}$$

If the mean linear water velocity is very small, then the exponentials can be approximated by power series:

$$\frac{c}{c_o} = \frac{\left(1 + \frac{v_f z}{D_l}\right) - \left(1 + \frac{v_f L}{D_l}\right)}{1 - \left(1 + \frac{v_f L}{D_l}\right)} = \frac{L - z}{L}$$

i.e. if advection is negligible and diffusion therefore dominates then the steady state distribution is linear from source to sink. This result could have also been reached by integrating the diffusion equation directly.

- (a) DNAPLS and LNAPLS are acronym for Dense Non-aqueous phase liquids and Light Non-aqueous phase liquids, respectively. They are liquid contaminants which were immiscible with water. Typical DNAPL contaminants are chlorinated solvents such as PCE and TCE. Typical LNAPL contaminants are petroleum products such as Benzene and Toluene. DNAPLs are denser than water, whereas LNAPLs are lighter than water. Due to their density differences, when they are spilled from the ground, LNAPL tends to float on top of the water table and DNAPL tends to penetrate deeper than the water table. Within DNAPLs, chlorinated solvents are less viscous than water. Therefore, the penetration front is unstable under gravity dominated flow and move inside the subsurface in a complex manner. Hence, it is very difficult to find them in the subsurface. The solubility values are low and they remain as a continuous contaminant source for very long time. Although small amount of solvents can only dissolve into water, the toxicity is high.
- (b) One person in one million people will get a cancer if one million people are exposed to this daily dose value of a chemical throughout their life time, which is usually 70 years. The maximum allowable concentration of this contaminant in water can be estimated by applying this daily dose to an amount of 2L of water, which is consumed daily.

[ISX]

(c)

(i) From Data sheet, the properties of benzene are

Henry's constant H = 5.55 atm/M

Molecular weight = 78.1

Gas concentration  $P = 2000 \text{ ppmV} = 2000 \text{ x } 10^{-6} \text{ atm} = 2 \text{ x } 10^{-3} \text{ atm.}$ 

Using Henry's law, the concentration in the soil moisture

$$C = P/H = 2 \times 10^{-3}/5.55 = 3.6 \times 10^{-4} M.$$

Convert this to mg/L.

$$3.6 \times 10^{-4}$$
 (M)=  $3.6 \times 10^{-4}$  (mol/L) x  $78.1$  (g/mol) x  $10^{3}$  (mg/g) =  $28.2$  mg/L.

(15% T

(ii) The octanol-water partition coefficient of toluene is logK<sub>ow</sub>=2.13 from Data sheet.

For aromatic compounds (see Data sheet),  $\log K_{oc} = 0.544$  (logKow) + 1.377 = 0.544 x 2.13 + 1.377 = 2.54

Hence,  $K_{oc} = 347 \text{ (L/kg)}$ 

The partitioning coefficient  $K_p$  is then estimated  $K_p = f_{oc}K_{oc} = 0.01 \times 347 = 3.47$ 

(L/kg)

Using the linear isotherm model,  $X = K_pC = 3.47 \times 28.2 = 97.9 \text{ mg/kg}$ .

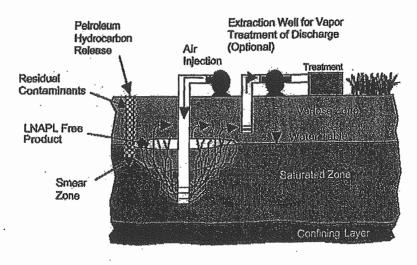
[15X]

(iii) Gas concentration  $P = 2000 \text{ ppmV} = 2000 \times 78.1/24.05 \text{ (mg/m}^3) \times 10^{-3} \text{ (m}^3/\text{L)} = 6.49 \text{ mg/L}.$ 

Mass of benzene inhaled = 6.49 (mg/L) x 2 (m<sup>3</sup>) x 10<sup>3</sup> (L/m<sup>3</sup>) = 12980 mg. Mass of benzene ingested = 97.9 (mg/kg) x 1800 (kg/m<sup>3</sup>) x 10 (cm<sup>3</sup>) x 10<sup>-6</sup> (m<sup>3</sup>/cm<sup>3</sup>) = 1.76 mg. Hence, Inhalation >> Ingestion.

## (iv) Soil vapour extraction and air sparging.

Air or oxygen is injected through a contaminated aquifer. Injected air traverses horizontally and vertically in channels through the soil, creating an underground stripper that removes volatile and semi-volatile organic contaminants by volatilization. The injected air helps to flush the contaminants into the unsaturated zone. Soil vapor extraction (SVE) usually is implemented in conjunction with air sparging to remove the generated vapor-phase contamination from the vadose zone. Oxygen present in the air added to the contaminated groundwater and vadose-zone soils also can enhance biodegradation of contaminants below and above the water table.



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