

ENGINEERING TRIPOS PART IIB

---

Wednesday 6 May 2009 2.30 to 4

---

Module 4A8

ENVIRONMENTAL FLUID MECHANICS

*Answer not more than **three** questions.*

*All questions carry the same number of marks.*

*The **approximate** percentage of marks allocated to each part of a question is indicated in the right margin.*

*Attachments: Data sheets (5 pages).*

STATIONERY REQUIREMENTS

Single-sided script paper

SPECIAL REQUIREMENTS

Engineering Data Book

CUED approved calculator allowed

**You may not start to read the questions printed on the subsequent pages of this question paper until instructed that you may do so by the Invigilator**

1 The geostrophic flow is governed by the following equation

$$2\mathbf{\underline{\Omega}} \times \mathbf{\underline{u}} = \frac{-1}{\rho_0} \nabla P,$$

where the symbols have their usual meaning. Take the rotation rate vector  $\mathbf{\underline{\Omega}} = (0, 0, \Omega_z)$  as a constant.

(a) What is the physical interpretation of this equation? Is the equation valid for planetary boundary layers? [15%]

(b) Show that the vertical component of the vorticity,  $\underline{\omega} \equiv \nabla \times \underline{u}$ , is related to the Laplacian of the pressure. Also, show that, when the pressure field is continuous, the geostrophic velocity field satisfies  $\nabla \cdot \underline{u} = 0$ . [35%]

(c) The air density  $\rho$  can be expressed as  $\rho = \rho_0(1 - \alpha \theta)$ , where  $\alpha$  is the volumetric thermal expansion coefficient and  $\theta = T(z) - T(0)$ , with  $T(z)$  the temperature at height  $z$  and  $T(0)$  the ground temperature. A wind can result when the horizontal gradient of  $\theta$  is sufficiently large. This wind is called *thermal wind* and is governed by

$$2\Omega_z \frac{\partial v}{\partial z} = g\alpha \frac{\partial \theta}{\partial x} \quad \text{and} \quad 2\Omega_z \frac{\partial u}{\partial z} = -g\alpha \frac{\partial \theta}{\partial y},$$

where  $u$  and  $v$  are the horizontal components of the velocity vector  $\underline{u}$ . Obtain the above two equations using the hydrostatic balance equation  $\partial P / \partial z = -\rho g$  and the geostrophic equation given above. Determine the vertical variation of the thermal wind components  $u$  and  $v$  when the temperature increment varies as  $\theta = Ax^2 + By$ , where  $A$  and  $B$  are constants. Comment on your solutions. [50%]

2 Free convective flows in the environment can be approximated well by a flow between differentially heated parallel plates. Consider two horizontal infinitely long parallel plates separated by a vertical distance  $d$ . The bottom plate is at a temperature  $T_s$  and supplies a uniform heat flux of  $Q \text{ Wm}^{-2}$ . After an initial transient, a stationary turbulent flow with zero mean velocity is created. Assume that horizontal variations are negligible. The mean density of the fluid in the gap is  $\rho$  and the mean specific heat capacity at constant pressure is  $c_p$ .

(a) Using the mean temperature equation from the Data Card, show that the turbulent heat flux in the vertical direction is given by

$$\overline{u_3 \theta} \approx \frac{Q}{\rho c_p},$$

where the fluctuating velocity in the vertical direction is  $u_3$ , the temperature fluctuation is  $\theta$ , and the mean molecular heat flux can be neglected. [20%]

(b) Simplify the equations for the turbulent kinetic energy  $k$  and for the variance  $\sigma$  of the temperature fluctuations (given in the Data Card) for this problem. Taking the body force in the balance equation for  $k$  as  $g \overline{u_3 \theta} / \bar{T}$ , make an estimate for the turbulent kinetic energy per unit mass and its dissipation rate  $\varepsilon$ . The mean temperature is  $\bar{T}$  and the gravitational constant is  $g$ . [30%]

(c) By taking the dissipation rate of  $\sigma$  as  $c_d \sigma \varepsilon / k$ , where  $c_d$  is a constant, show that the mean temperature at  $d/2$  is

$$\frac{\bar{T}}{T_s} \approx (1 - \mathcal{A}d)^{3/4},$$

where  $\mathcal{A} = \frac{c_d}{3} \frac{\sigma}{T_s^{4/3}} \left( \frac{g}{d^2} \right)^{1/3} \left( \frac{\rho c_p}{Q} \right)^{2/3}$ . [50%]

(TURN OVER

3 (a) Discuss briefly three of the major pollutants usually found in urban areas in terms of their sources, chemistry, health impacts, and diurnal variation. [70%]

(b) A lake of volume  $V_0$  contains water contaminated by a pollutant at concentration  $\phi_0$  [units:  $\text{kg m}^{-3}$ ]. At time  $t = 0$ , a water stream begins to flow into the lake at a constant volume flow rate  $Q$  carrying the same pollutant at concentration  $2\phi_0$ . Show that, if there is no outflow from the lake, the subsequent evolution of the pollutant concentration  $\phi$  in the lake obeys

$$\frac{\phi}{\phi_0} = 2 - \left(1 + \frac{Qt}{V_0}\right)^{-1}.$$

[30%]

4 (a) Discuss briefly, using appropriate sketches, typical shapes of plumes from continuous sources in a uniform wind, including comments on the relevant atmospheric stability and inversions. [50%]

(b) Find the necessary relation between the dispersion coefficient  $\sigma$  and the diffusivity  $K$  for the one-dimensional Gaussian equation in the Data Card to be a solution to

$$U \frac{\partial \phi}{\partial x} = K \frac{\partial^2 \phi}{\partial y^2}$$

[50%]

**END OF PAPER**

## 4A8: Environmental Fluid Mechanics

### Part I: Turbulence and Fluid Mechanics

#### DATA CARD

##### Rotating Flows

##### Geostrophic Flow

$$-\frac{1}{\rho} \nabla p = 2\Omega \times \underline{u}$$

##### Ekman Layer Flow

$$-2\Omega_z v = -\frac{1}{\rho} \frac{\partial p}{\partial x} + \nu \frac{\partial^2 u}{\partial z^2}$$

$$2\Omega_z u = -\frac{1}{\rho} \frac{\partial p}{\partial y} + \nu \frac{\partial^2 v}{\partial z^2}$$

$$0 = -\frac{1}{\rho} \frac{\partial p}{\partial z}$$

OR

$$-2\Omega_z v = \nu \frac{\partial^2 u}{\partial z^2}$$

$$-2\Omega_z (u_g - u) = \nu \frac{\partial^2 v}{\partial z^2}$$

##### *GEOSTROPHIC VELOCITY*

Solution is

$$u = u_g \left[ 1 - e^{-z/\Delta} \cos \frac{z}{\Delta} \right]$$

$$v = u_g e^{-z/\Delta} \sin \frac{z}{\Delta}$$

$$\Delta = \left( \frac{\nu}{\Omega_z} \right)^{1/2}$$

## Turbulent Flows – Incompressible

Continuity Equation  $\nabla \cdot \underline{U} = \frac{\partial U_i}{\partial x_i} = 0$

Momentum Equation  $\rho \frac{DU_i}{Dt} = -\frac{\partial P}{\partial x_i} + \mu \frac{\partial^2 U_i}{\partial x_j^2} + F_i$

Enthalpy Equation  $\rho c_p \frac{DT}{Dt} = -k \frac{\partial^2 T}{\partial x_i^2}$

Reynolds Transformation  $U_i = \overline{U}_i + u_i$  etc

Reynolds Stress  $= -\overline{\rho u_i u_j}$ , Reynolds Heat Flux  $= -\overline{\rho c_p u_j \Theta}$

### Turbulent Kinetic Energy, $k$ , Equation

$$\frac{Dk}{Dt} = -\overline{u_i u_k} \frac{\partial \overline{U}_i}{\partial x_k} - \varepsilon + \frac{\overline{f_i u_i}}{\rho} + \text{transport of kinetic energy forms}$$

### Mean temperature equation

$$\rho c_p \frac{D\overline{T}}{Dt} = \frac{\partial}{\partial x_j} \left( \lambda \frac{\partial \overline{T}}{\partial x_j} - \overline{u_j \Theta} \rho c_p \right)$$

### Temperature variance, $\sigma$ , equation

$$\frac{D\sigma}{Dt} = -2\overline{u_j \Theta} \frac{\partial \overline{T}}{\partial x_j} - \varepsilon_\sigma + \text{molecular diffusion}$$

### In flows with thermally driven motion

$$\frac{f_i u_i}{\rho} = \frac{g}{T} \cdot \overline{\Theta u_i}, \quad i = \text{Vertical direction}$$

Dissipation of turbulent kinetic energy  $\varepsilon \approx \frac{u'^3}{\ell}$

Kolmogorov microscale  $\eta = \left( \frac{\nu^3}{\varepsilon} \right)^{1/4}$

Taylor microscale ( $\lambda$ )  $\varepsilon = 15\nu \frac{u'^2}{\lambda^2}$  ( $\nu$  is the kinematic viscosity)

## Density Influenced Flows

### Atmospheric Boundary Layer

$$\left. \frac{dT}{dz} \right|_{\text{NEUTRAL STABILITY}} = -\frac{g}{c_p} = \left. \frac{dT}{dz} \right|_{\text{DALR}}$$

$$R_i = \frac{g}{T} \frac{\left. \frac{dT}{dz} \right|_{\text{DALR}} - \left. \frac{dT}{dz} \right|_{\text{NEUTRAL STABILITY}}}{\left( \frac{dU}{dz} \right)^2} = \text{RICHARDSON NUMBER}$$

### Neutral Stability

$$U = \frac{u_*}{\kappa} \ln \frac{z}{z_0}; \quad \frac{dU}{dz} = \frac{u_*}{\kappa z}$$

$$u_* = \sqrt{\frac{\tau_w}{\rho}}; \quad \kappa = \text{Von Karman Constant} = 0.40$$

### Non-Neutral Stability

$$L = \text{Monin-Obukhov length} = -\frac{u_*^3}{\kappa \frac{g}{T} \frac{Q}{\rho c_p}}$$

Q = surface heat flux

$$\frac{dU}{dz} = \frac{u_*}{\kappa z} \left( 1 - 15 \frac{z}{L} \right)^{-1/4} \quad \text{Unstable}$$

$$= \frac{u_*}{\kappa z} \left( 1 + 4.7 \frac{z}{L} \right) \quad \text{Stable}$$

### Buoyant plume for a point source

$$\frac{d}{dz} \pi R^2 w = 2\pi R u_e \quad (\text{i})$$

$$\frac{d}{dz} \rho \pi R^2 w = \rho_a 2\pi R u_e \quad (\text{ii})$$

$$\frac{d}{dz} \rho \pi R^2 w^2 = g(\rho_a - \rho) \pi R^2 \quad (\text{iii})$$



(i) and (iii) give

$$\pi R^2 w \left( \frac{\rho_a - \rho}{\rho_a} \right) g = \text{constant} = F_0 \text{ (buoyancy flux)}$$

$$u_e = \alpha w$$

( $\alpha$  = Entrainment coefficient)

$$N^2 = -\frac{g}{\rho} \frac{d\rho}{dz} = \frac{g}{T} \frac{dT}{dz}$$

Actually  $\frac{g}{T} \left( \frac{dT}{dz} - \frac{dT}{dz} \Big|_{\text{DALR}} \right)$

N = Brunt – Vaisala Frequency or Buoyancy Frequency

## 4A8: Environmental Fluid Mechanics

### Part II: Dispersion of Pollution in the Atmospheric Environment

#### DATA CARD

Transport equation for the mean of the reactive scalar  $\phi$  :

$$\frac{\partial \bar{\phi}}{\partial t} + \bar{u}_j \frac{\partial \bar{\phi}}{\partial x_j} = \frac{\partial}{\partial x_j} \left( K \frac{\partial \bar{\phi}}{\partial x_j} \right) + \bar{w}$$

Transport equation for the variance of the reactive scalar  $\phi$  :

$$\frac{\partial g}{\partial t} + \bar{u}_j \frac{\partial g}{\partial x_j} = \frac{\partial}{\partial x_j} \left( K \frac{\partial g}{\partial x_j} \right) + 2K \left( \frac{\partial \bar{\phi}}{\partial x_j} \right)^2 - \frac{2}{T_{turb}} g + 2\overline{\phi'w'}$$

Mean concentration of pollutant after instantaneous release of  $Q$  kg at  $t=0$ :

$$\bar{\phi}(x, y, z, t) = \frac{Q}{8(\pi t)^{3/2} (K_x K_y K_z)^{1/2}} \exp \left[ -\frac{1}{4t} \left( \frac{(x-x_0)^2}{K_x} + \frac{(y-y_0)^2}{K_y} + \frac{(z-z_0)^2}{K_z} \right) \right]$$

Gaussian plume spreading in two dimensions from a source at  $(0,0,z_0)$  emitting  $Q$  kg/s:

$$\bar{\phi}(x, y, z) = \frac{Q}{2\pi U \sigma_y \sigma_z} \exp \left[ -\left( \frac{y^2}{2\sigma_y^2} + \frac{(z-z_0)^2}{2\sigma_z^2} \right) \right]$$

One-dimensional spreading from line source emitting  $Q/L$  kg/s/m :

$$\bar{\phi}(x, y) = \frac{Q}{UL} \frac{1}{\sqrt{2\pi}\sigma_y} \exp \left( -\frac{y^2}{2\sigma_y^2} \right)$$

Relationship between eddy diffusivity and dispersion coefficient:

$$\sigma^2 = 2 \frac{x}{U} K$$